

Heat Transfer Enhancement in Pipe Using Al₂O₃/Water Nanofluid

Abdulhafid M A Elfaghi^{1,*}, Alhadi A Abosbaia², Munir F A Alkbir³, Abdoulhdi A B Omran⁴

¹ Faculty of Mechanical and Manufacturing Engineering, Universiti Tun Hussein Onn Malaysia, Malaysia

² Faculty of Engineering, University of Zawia, Libya

³ Advanced Facilities Engineering Technology Research Cluster, Malaysian Institute of Industrial Technology (MITEC), University Kuala Lumpur, Malaysia

⁴ Department of Mechanical and Mechatronic Engineering, Faculty of Engineering, Sohar University, Sohar, P C-311, Oman

| ARTICLE INFO | ABSTRACT |
|--|---|
| Article history: Received 29 May 2022 Received in revised form 3 August 2022 Accepted 26 August 2022 Available online 30 September 2022 | Convection heat transfer is widely used in many industrial heat and cooling systems. The heat convection can be enhanced passively by adding metal nanoparticles in the water that have been adequately consumed. Small solid metals or nanoparticles of metal oxides floating in the base liquid increase the efficiency of thermal transmission in the system. Commercial CFD code FLUENT is used to simulate water-based nanofluids and is considered to be a single-phase fluid. The effects of various parameters such as Nusselt number and friction factor are studied as a function of Reynolds number and particle volume fraction. The volume fraction of 0.5, 1.0, and |
| <i>Keywords:</i> Heat transfer; Forced convection; Nano- particles; CFD | 2.0 percent of the Al2O3 nanoparticles was investigated, with Reynolds numbers between 6000 and 12,000. The numerical results show that nanofluids have a higher efficiency in convection heat than basic fluid and an improved thermal transfer efficiency with Reynolds numbers and volume concentrations. |

1. Introduction

Many researchers have demonstrated the properties of thermal transmission in nanofluid thermal pipes [1–3]. Choi and Eastman [4] first proposed the concept of nanofluid. That is, adding nano-scale metals and metal oxide particles to liquids in a specific way and proportion form a new type of working fluid for heat transfer and cooling [5,6].

In order to estimate the thermal conductivity of nanofluids, theoretical and experimental research was carried out. Some experimental studies have shown that the thermal conductivity of nanofluids measured is larger than the theoretical predictions of classical theory [7]. Other experimental studies [8,9] have shown that thermal conductivity does not exhibit abnormal improvement, and the results are well consistent for low volume [7,10]. Efforts are being made to formulate effective theoretical models for predicting effective thermal conductivity, but this topic remains seriously incomplete. Keblinski *et al.*, [11] carried out an interesting review of the properties and future challenges of nanofluids. Aluminum oxide nanoparticles (Al₂O₃) are widely used in

* Corresponding author.

https://doi.org/10.37934/cfdl.14.9.118124

E-mail address: abdulhafid@uthm.edu.my (Abdulhafid M A Elfaghi)

experiments and numerical studies [12,13]. Wen and Ding [12] developed a series of experiments using Al₂O₃-water nanofluids in a circular tube. Anoop *et al.*, [13] conducted experiments using Al₂O₃-water to calculate the heat transfer coefficient considering the influence of particle size. Experimental results showed an increase in the thermal transfer coefficient of 25% at particle sizes of 45nm. In this study, a numerical heat transfer enhancement of nanofluids (water-Al₂O₃) in a two-dimensional horizontal pipe has been investigated. Numerical analysis is performed with the finite-volume method using FLUENT software.

2. Mathematical Formulation

2.1 Geometry Configuration

Figure 1 shows a schematic of physical problems and boundary conditions. The nano fluid enters a pipe of radius 0.06 m at a constant velocity of 0.001 m/s. The fluid has a density of 1000 kg/m³, a thermal conductivity of 0.6 W/m-K, a specific heat of 4180 J/kg-K, and a viscosity of 1.002×10^{-5} kg/m-s. The first 5.76 m of the pipe is isothermal, held at 300 K. The remaining 2.88 m of the pipe have a constant heat flux of 10Kw/m² added at the wall.

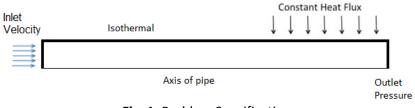


Fig. 1. Problem Specification

2.2 Governing Equations and Boundary Conditions

Nanofluids are composed of very small particles, so nanoparticles and base liquids are considered to be thermally balanced and flow at the same speed. In energy equations, compression work and viscosity dissipation are considered to be insignificant. Based on these hypotheses, the general equation of the rule is as follows. [14-17]:

Continuity equation:

$$\nabla \left(\rho_{nf} V \right) = 0 \tag{1}$$

Momentum equation:

$$\nabla . (\rho_{nf} VV) = -\nabla P + \nabla . \tau$$
(2)

Energy equation:

$$\nabla . \left(\rho_{nf} V C_{p,nf} \right) = - \nabla . \left(k_{nf} \nabla T - C_{p,nf} \rho_{nf} \overline{vt} \right)$$
(3)

2.3 Nanofluid Thermo-Physical Properties

The thermophysical properties of nanofluids are mainly the function of particle volume and temperature. Since there are no experimental data, the density and specific heat of nanofluids are defined as the following fractional functions [2,3,18,19]:

Nanoparticle volume fraction in nanofluid:

$$\phi = \frac{V_{np}}{V_{bf} + V_{np}} \tag{4}$$

Density of nanofluid:

$$\rho_{nf} = (1 - \emptyset)\rho_{bf} + \emptyset\rho_{np} \tag{5}$$

Specific heat of nanofluid:

$$C_{p,nf} = \frac{(1-\emptyset)\rho_{bf}C_{p,bf} + \emptyset\rho_{np}C_{p,np}}{\rho_{nf}}$$
(6)

Thermal conductivity of nanofluid:

Tabla 1

$$\frac{k_{nf}}{k_{bf}} = \frac{(k_{np} + 2k_{bf}) - 2\phi(k_{bf} - k_{np})}{(k_{np} + 2k_{bf}) + \phi(k_{bf} - k_{np})}$$
(7)

Viscosity of nanofluid:

$$\mu_{nf} = \mu_{bf} \frac{1}{(1-\phi)^{2.5}} \tag{8}$$

Based on the equations above, the volume fraction of nanoparticle is \emptyset , V_{bf} is base fluid volume, V_{np} as the volume of nanoparticle. Other than that, ρ_{np} (kg/m³) is the nanoparticle's density while ρ_{bf} (kg/m³) is the base fluid's density. The specific heat is $C_{p,nf}$ (J/kg.K) for nanofluid while $C_{p,bf}$ (J/kg.K) is for base fluid, k_{nf} (W/m.K) represents the nanofluid thermal conductivity while k_{bf} (W/m.K) is the base fluid's thermal conductivity, k_{np} (W/m.K) is nanoparticle's thermal conductivity. Lastly, μ_{nf} (Pa.s) and μ_{bf} (Pa.s) are viscosity of nanofluid and base fluid respectively.

Table 1 shows the water and Al_2O_3 characteristics, and the proposed nanoparticles, Al_2O_3 . The thermophysical characteristics formulas are shown in the section below.

| Thermophysical properties of Al ₂ O ₃ nanofluid | | | |
|---|-------|--------------------------------|--|
| Property | Water | Al ₂ O ₃ | |
| Density (kg/m ³) | 998.2 | 3970 | |
| Specific heat (J/kg.K) | 4182 | 765 | |
| Thermal conductivity (W/m.K) | 0.6 | 40 | |
| Viscosity (Pa.s) | 0.001 | - | |

3. Results

Figure 2 shows the temperature contours along the pipe. The temperature is constant along the isothermal part of the pipe and is varying along the heat flux region. The temperature is high at the pipe wall and is gradually decreasing towards the centreline.

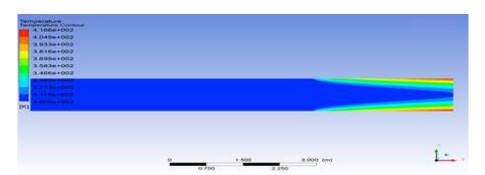


Fig. 2. Temperature Contour along the pipe

Figure 3 shows that heat transfer coefficient grows linearly with Reynolds number. The heat transfer coefficient of the Al_2O_3 nanofluid is superior to that of water due to the improved thermophysical characteristics of the nanofluids due to the dispersion in water. The addition of solid nanoparticles to water has improved thermal conductivity resulting in an increase in the heat transfer coefficient.

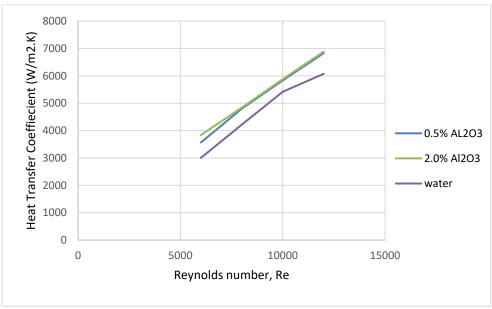


Fig. 3. Effect of nanoparticle concentration on convective heat transfer coefficient

Based on the results in Figure 4, Nusselt number increases as the Reynolds number increases. This is also influenced by the volume fraction increase where Nusselt number is higher when the volume fraction of the Al_2O_3 nanofluid increases.

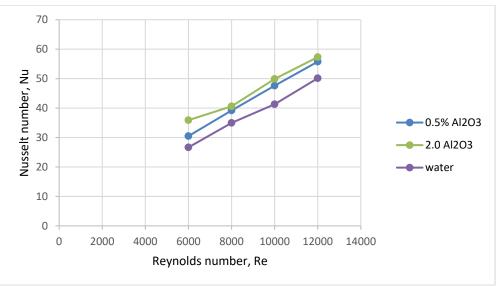


Fig. 4. Effect of nanoparticle concentration on Nusselt number

Figure 5 shows the impact of volume fractions and Reynolds numbers on water friction factors and Al2O3 nanofluids.

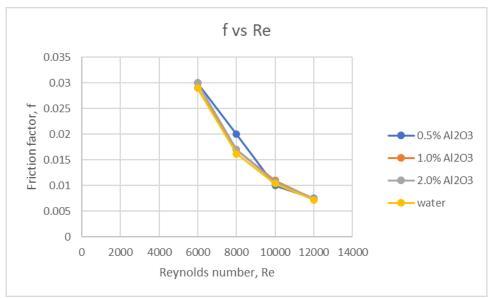


Fig. 5. Comparison of friction factor between present study and water

The friction factor of Al_2O_3 nanofluids is higher than that of water, and as the volume increases, the friction factor increases. This is due to the fact that nanofluids have a viscosity higher than water and increase in volume fraction. Al_2O_3 nanofluid density is higher than water density, so nanofluid velocity is lower. Among Al_2O_3 and water, the 2.0% nanofluid had the greatest friction factor. As Reynolds increased from 6000 to 20,000, nanofluid friction factors increased by 0.1%.

4. Conclusions

A numerical CFD simulation for a forced convection heat transfer in a horizontal pipe is carried out using the commercial CFD ANSYS Fluent code. The simulation is carried out for pure water and water with nanoparticles as a cooling fluid. Ansys fluent software was used to study the effect of suspension of nano particles of Al_2O_3 into water as a base fluid and to determine to what extent 2D modelling is sufficient to display the behaviour of thermohydraulic characteristics of the convective heat transfer flow through pipes. According to the numerical results, adding nanoparticles to the fluid improved heat transfer and the Nusselt number in the flow.

Acknowledgement

The corresponding author acknowledge the Research Management Centre, (RMC), Universiti Tun Hussein Onn Malaysia for the financial support under the RMC Research Fund (H768).

References

- Sureshkumar, R., S. Tharves Mohideen, and N. Nethaji. "Heat transfer characteristics of nanofluids in heat pipes: a review." *Renewable and Sustainable Energy Reviews* 20 (2013): 397-410. https://doi.org/10.1016/j.rser.2012.11.044
- [2] Elfaghi, Abdulhafid M A, and Muhammad Syahmi Mohammad Hisyammudden. "Computational Simulation of Heat Transfer Enhancement in Heat Exchanger Using TiO₂ Nanofluid". *Journal of Complex Flow* 3, no. 2 (2021): 1-6.
- [3] Elfaghi, Abdulhafid M A, and Musfirah Mustaffa. "Numerical Simulation of Forced Convection Heat Transfer in Pipe Using Different Nanoparticles". *Journal of Complex Flow* 3, no. 2 (2021): 33-37.
- [4] Choi, S. US, and Jeffrey A. Eastman. *Enhancing thermal conductivity of fluids with nanoparticles*. No. ANL/MSD/CP-84938; CONF-951135-29. Argonne National Lab. (ANL), Argonne, IL (United States), 1995.
- [5] Yoo, Dae-Hwang, K. S. Hong, and Ho-Soon Yang. "Study of thermal conductivity of nanofluids for the application of heat transfer fluids." *Thermochimica Acta* 455, no. 1-2 (2007): 66-69. <u>https://doi.org/10.1016/j.tca.2006.12.006</u>
- [6] Hamilton, R. L^Ĥ, and O. K. Crosser. "Thermal conductivity of heterogeneous two-component systems." *Industrial & Engineering chemistry fundamentals* 1, no. 3 (1962): 187-191. <u>https://doi.org/10.1021/i160003a005</u>
- [7] Putnam, Shawn A., David G. Cahill, Paul V. Braun, Zhenbin Ge, and Robert G. Shimmin. "Thermal conductivity of nanoparticle suspensions." *Journal of applied physics* 99, no. 8 (2006): 084308. <u>https://doi.org/10.1063/1.2189933</u>
- [8] Zhang, Xing, Hua Gu, and Motoo Fujii. "Effective thermal conductivity and thermal diffusivity of nanofluids containing spherical and cylindrical nanoparticles." *Experimental Thermal and Fluid Science* 31, no. 6 (2007): 593-599. <u>https://doi.org/10.1016/j.expthermflusci.2006.06.009</u>
- [9] Yamada, Etsuro, and Terukazu Ota. "Effective thermal conductivity of dispersed materials." *Wärme-und Stoffübertragung* 13, no. 1 (1980): 27-37. <u>https://doi.org/10.1007/BF00997630</u>
- [10] Choi, S. U. S., Z. George Zhang, WLockwoodFE Yu, F. E. Lockwood, and E. A. Grulke. "Anomalous thermal conductivity enhancement in nanotube suspensions." *Applied physics letters* 79, no. 14 (2001): 2252-2254. <u>https://doi.org/10.1063/1.1408272</u>
- [11] Keblinski, Pawel, Jeffrey A. Eastman, and David G. Cahill. "Nanofluids for thermal transport." *Materials today* 8, no. 6 (2005): 36-44. <u>https://doi.org/10.1016/S1369-7021(05)70936-6</u>
- [12] Wen, Dongsheng, and Yulong Ding. "Experimental Investigation into Convective Heat Transfer of Nanofluids at the Entrance Region under Laminar Flow Conditions." *International Journal of Heat and Mass Transfer* 47, no. 24 (2004): 5181–88. <u>https://doi.org/10.1016/j.ijheatmasstransfer.2004.07.012</u>
- [13] Anoop, K. B., T. Sundararajan, and Sarit K. Das. 2009. "Effect of Particle Size on the Convective Heat Transfer in Nanofluid in the Developing Region." *International Journal of Heat and Mass Transfer* 52, no. 9–10 (2009): 2189– 95. <u>https://doi.org/10.1016/j.ijheatmasstransfer.2007.11.063</u>
- [14] Abobaker, Mostafa, Sogair Addeep, and Abdulhafid M. Elfaghi. "Numerical Study of Wind-Tunnel Wall Effects on Lift and Drag Characteristics of NACA 0012 Airfoil." CFD Letters 12, no. 11 (2020): 72–82. <u>https://doi.org/10.37934/cfdl.12.11.7282</u>
- [15] Elfaghi, A. M., W. Asrar, and A. A. Omar. "A High Order Compact-Flowfield Dependent Variation (Hoc-FDV) Method for Inviscid Flows." *International Journal for Computational Methods in Engineering Science and Mechanics* 11, no. 5 (2010): 258–63. <u>https://doi.org/10.1080/15502287.2010.501322</u>
- [16] Elfaghi, Abdulhafid M., Waqar Asrar, and Ashraf A. Omar. "Higher Order Compact-Flowfield Dependent Variation (HOC-FDV) Solution of One-Dimensional Problems." *Engineering Applications of Computational Fluid Mechanics* 4, no. 3 (2010): 434–40. <u>https://doi.org/10.1080/19942060.2010.11015330</u>
- [17] Elfaghi, Abdulhafid, Ashraf Ali Omar, and Waqar Asrar. "Higher-Order Compact-Flow Field-Dependent Variation (Hoc-FDV) Method for Solving Two-Dimensional Navier-Stokes Equations." International Journal for Computational Methods in Engineering Science and Mechanics 16, no. 4 (2015): 256–63. <u>https://doi.org/10.1080/15502287.2015.1048386</u>

- [18] Elhadi Kh. Abugnah, Wan Saiful-Islam Wan Salim, Abdulhafid M. Elfaghi, and Zamani Ngali. "Comparison of 2D and 3D Modelling Applied to Single Phase Flow of Nanofluid through Corrugated Channels." CFD Letters 14, no. 1 (2022): 128–139. <u>https://doi.org/10.37934/cfdl.14.1.128139</u>
- [19] Dittus, F. W., and L. M. K. Boelter. "Heat transfer in automobile radiators of the tubular type." International communications in heat and mass transfer 12, no. 1 (1985): 3-22. <u>https://doi.org/10.1016/0735-1933(85)90003-X</u>