

Time-Dependent MHD Free Convective Heat Circulation of Hybrid Nano Liquid over a Vertical Porous Plate Due to Temperature Oscillation with Thermal Radiation and Viscous Dissipation

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ARTICLE INFO	ABSTRACT
Article history: Received 6 August 2023 Received in revised form 27 October 2023 Accepted 9 November 2023 Available online 30 November 2023 Keywords: Free convection; MHD; hybrid nano	In the current numerical simulation, the thermal transfer of viscous incompressible time dependent MHD free convective flow of hybrid nanofluid (Cu-TiO ₂ -H ₂ O) over a vertical porous plate with viscous dissipation and thermal radiation is examined. The system of partial differential equations which controls the fluid flow are transmuted into dimensionless equations and are solved using numerical simulation namely Galerkin Finite Element Method. The momentum and thermal consequences, coefficient of heat transfer and skin friction with Gr, M, Ec, N, t, ωt , δ_2 , λ – parameters for both nanofluid (Cu-H ₂ O) and hybrid nanofluid (Cu-TiO ₂ -H ₂ O) flows are exposed through graphs and tables. It is revealed that heat transfer coefficient of Cu-TiO ₂ -H ₂ O is more effective when compared with Cu-H ₂ O flows varying with aforementioned parameters. The current numerical computation is in good agreement with the analytical solution of the problem.
liquid; temperature oscillation; viscous dissipation; thermal radiation	This study is used in several engineering fields such as electronic cooling, heat exchangers, nanomaterial processing, environmental engineering, chemical industry.

1. Introduction

Transient MHD thermal convective circulations together with temperature oscillation in porous media is paramount in designing of natural and fluid engineering problems. Applications of MHD unsteady thermal convective circulations in nature and fluid engineering problems are of great technical importance in the areas such as geothermal energy extraction, MHD generators, elevation of thermal transfer in gas cooling systems, blood flow, accelerators, salinity difference in sea, cooling of nuclear power plants, electrical and electronic equipment etc. In view of aforesaid applications Vempati and Laxmi-Narayana-Gari [1] explored numerical simulation of natural convection and mass transmission on time dependent viscous liquid flow over an erect plane in presence of magnetism. Rashidi *et al.*, [2] analytically demonstrated mass and heat transformations on two-dimensional

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hydromagnetic laminar flow with radiation over a porous surface. The buoyancy and heat transmission influence on hydromagnetic motion over a permeable surface is numerically examined by Daniel et al., [3]. Singh et al., [4] numerically described the heat transfer of free convective fluid flow past an infinite erect permeable surface with hydromagnetic influence. In view of aforesaid applications many scholars investigated MHD heat transformation fluid flow with various geometrical parameters [5-15]. The heat and mass transfer of MHD nanofluid flow with hall effects over different geometries is described by Singh et al., [16,17]. The numerical study on MHD effects with viscous dissipation and chemical reaction of first order of heat and mass transfer over an upright stretching surface is investigated by Sharma and Gandhi [18]. Sharma et al., [19] studied an incompressible fluid flow over an erect stretching surface to analyze heat and mass transfer impacts with ohmic heating, thermal and exponential heat source. Kumar et al., [20] developed the sensitivity analysis of hybrid nano liquid over an up straight stretching surface with viscous dissipation, Joule heating impacts. Sharma et al., [21] explored the influence of entropy generation, heat transmission, and mass transfer on the flow of Jeffrey fluid with solar radiation effect in the presence of copper nanoparticles and gyrotactic microorganisms. A numerical simulation to blood flow past a penetrable artery with an aneurysm under the electric and magnetic effect of hybrid nano liquid is scrutinized by Gandhi et al., [22]. Reddy et al., [23] numerically examined the impact the heat generation/absorption over a porous stretching cylinder on MHD thermal transfer flow of fluid.

Hybrid nano liquids are the next generation of nano liquids, which are acquired by scattering a homogeneous/non-homogeneous solution of composite nano powder of varied nanomaterials in a mixture of one or more base liquids. Hybridization of nanoparticles results a pristine physical and chemical bond which really make hybrid nano liquids to extend finer heat transfer performance than the conventional heat transmission and nano liquids with single nanoparticles. Hybrid nano liquids expanded their applications in every field like microelectronics, nuclear cooling, transportation, defence, naval structures, medical, drug delivery, pasteurization, solar energy conversion system, acoustics, liquid propulsion, heat transmission, manufacturing and so on. Vemula et al., [24] explained numerical model of transient natural convection nano liquid flow of heat transmission past an erect surface. A comparative numerical flow and heat transfer analysis of nano liquid and Hybrid nano liquid over an enlarging sheet was performed by Devi and Devi [25,26]. The process of activation energy in thermo bioconvection nanofluid motion in a square cavity with gyrotactic microorganisms past a permeable surface is demonstrated by Bodduna et al., [27]. Asogwa et al., [28] numerically studied the heat generation with activation energy on hydrodynamic nanofluid flow over a stretching sheet. The usage of Hybrid nanofluids past a movable up right surface to amplify the free convective transmission of heat is numerically demonstrated by Rajesh et al., [29]. Sharma et al., [30] explored the effects of chemical reaction and thermal radiation of hybrid nanofluid flow over rotating disk. Mallesh et al., [31] numerically scrutinized the heat generation and radiation effects on unsteady convective hybrid nanofluid flow over an upright oscillating plane.

Viscous dissipation is an irreversible phenomenon in which shear forces convert into heat due to the friction on flow between adjacent layers as a consequence mechanical energy is transmuted into heat energy. Viscous dissipation in Hybrid nano liquids acts an essential role in geophysical flows, aerodynamics and polymer processing. Reddy [32] numerically analyzed unsteady free convection flow on an upright sheet with viscous dissipation effect and magnetism. Zainal *et al.*, [33] demonstrated viscous dissipation impact on MHD stagnation flow over an expanding sheet in different nano liquids.

Thermal radiation has a major impact on thermal expansion in the boundary layer flow of a liquid at ambient temperature and is crucial in many technological applications including space technology, integrated circuit cooling, turbines, plasmas, missiles, satellites, design of space vehicles and aviation equipment. Bestman and Adjepong [34] analytically explored three-dimensional natural convection flow over a porous plane in a rotating motion. Makinde and Ogulu [35] numerically developed the influence of temperature-dependent viscosity with magnetism on natural convective laminar liquid flow over an up straight plane. Pal and Mondal [36] numerically scrutinized the radiation impact over a vertical sheet immersed in combined convective flows of optically thick viscous liquid. Jat and Chaudhary [37] numerically explored two-dimensional steady viscous fluid flow over a stretching sheet under the influence of Lorentz force and thermal radiation. Sandeep *et al.*, [38] and Chaudhary and Chaudhary [39] numerically demonstrated hydromagnetic and heat exchange properties on the different liquid flows over an exponentially stretching plane. Recently, numerical simulation of unsteady free convective CNT's nano liquid motion over an up straight plane with thermal variation is investigated by Kavitha *et al.*, [40].

Convective heat transfer in fluid-saturated porous media has received much attention since a decade due to its importance in various applications like nuclear waste repository, geothermal sciences, engineering, agriculture, combustion systems, heat pipes, enhanced oil reservoir recovery, thermal insulation engineering, hydro flow in geothermal reservoirs etc. Recently, numerous researchers have focused on radiative heat transfer and multiphase transport in porous medium, with and without phase change. Several researchers scrutinized heat transmission challenges in porous media on varied geometries [41-45]. Chaudhary *et al.*, [46] developed a numerical model on transient viscous liquid over a stretching surface using magnetic field and heat generation/absorption. Mixed convection two-dimensional steady flow pattern along permeable up right sheet with a hybrid nano liquid is numerically presented by Waini *et al.*, [47]. Sharma *et al.*, [48] studied the ternary hybrid nanofluid with blood as a host fluid for homogeneous and heterogeneous chemical reaction, thermal radiation, viscous dissipation effects over curved surfaces.

The heat transmission of incompressible time dependent MHD natural convective flow of hybrid nano liquid past a vertical permeable surface with thermal radiation and viscous dissipation and novel term temperature oscillation is described in this numerical simulation. The flow controlling equations of hybrid nanofluid in the form of partial differential equations are transformed into dimensionless equations employing similarity variables and are solved using a numerical approach namely Galerkin Finite Element Method. The graphical and tabular explanation is presented on momentum, thermal, heat transfer and skin friction coefficient with pertinent parameters of both Cu-H₂O and Cu-TiO₂-H₂O fluids. This numerical computation is in good agreement with the analytical solution of the problem. The current work has novel characteristics which are used in engineering fields such as nuclear coolants, heat exchangers, thermal image processing etc. The future scope of the present study is to explore the mixed convective flows over different geometries.

2. Flow Analysis and Solution

A laminar, incompressible time dependent MHD Cu-TiO₂-H₂O hybrid nano liquid flow over a vertical plate with viscous dissipation and thermal radiation effects are considered. We assumed a cartesian coordinate system (x^*, y^*) such that x^* - axis is taken vertically upwards along with the plate and y^* - axis is normal to the plate, which is presented in Figure 1. Initially, both the plate and fluid are kept steady and retained at free stream temperature $\theta^* = \theta^*_{\infty}$ for all $t' \le 0$. When t' > 0, vertical plate commences being in motion with velocity $u_1^* = u_{1_0}^*$ and plate temperature is enhanced to $\theta^* = \theta^*_{\omega} + (\theta^*_{\omega} - \theta^*_{\infty}) \cos \omega^* t'$ and maintained uniform.

In the current study, Cu and TiO₂ nano particles with H₂O as base fluid is considered. Cu-H₂O is formed by scattering Cu nanoparticles of 0.1 volume fraction (δ_1 = 0.1, is fixed throughout the

simulation). To improve Cu-TiO₂-H₂O, titania nanoparticles with various volume fraction are dispersed in Cu-H₂O nanofluid. In the present scenario, Tiwari and Das [49] nano liquid model with Boussinesq approximation is considered [50]. The main assumption of Boussinesq approximation is that the density variations in the fluid can be neglected except in the buoyancy term of the Navier-stokes equations. The above assumptions are used to study the heat transfer characteristics of hybrid nano fluid flow in several engineering and bio-medical applications such as heat exchangers, polymer industries, drug delivery for chemo therapy processing etc. In view of these applications the frontier flow control equations of hybrid nano liquid are



$$\frac{\partial u_2^*}{\partial y^*} = 0 \tag{1}$$

$$\rho_{hnf}\left[\frac{\partial u_1^*}{\partial t'} + u_2^*\frac{\partial u_1^*}{\partial y^*}\right] = \mu_{hnf}\frac{\partial^2 u_1^*}{\partial y^{*^2}} + (\rho\beta)_{hnf}g\left(\theta^* - \theta_\infty^*\right) - \sigma_{hnf}B_0^2 u_1^*$$
⁽²⁾

$$\left(\rho C_{p}\right)_{hnf}\left[\frac{\partial\theta^{*}}{\partial t} + u_{2}^{*}\frac{\partial\theta^{*}}{\partial y^{*}}\right] = \kappa_{hnf}\frac{\partial^{2}\theta^{*}}{\partial y^{*^{2}}} - \frac{\partial q_{R}^{*}}{\partial y^{*}} + \mu_{hnf}\left(\frac{\partial u_{1}^{*}}{\partial y^{*}}\right)^{2}$$
(3)

Where,

$$q_R^*$$
 (radiative flux) = $-\frac{4\sigma_s}{3k_e}\frac{\partial\theta^{*^4}}{\partial y^*}$ (4)

Here σ_s represents absorption coefficient and K_e represents Stefan Boltzmann constant. The present study is assumed to optically thick nano liquids with Rosseland approximation. If temperature variations with in the stream are considered, then θ^{*4} can be represented as temperature lineal function using Taylor's series for θ^{*4} about $\theta^*_{\ \alpha}$, and ignoring components of highest order we get,

$$\theta^{*^4} \cong 4\theta^{*^3}_{\infty}\theta^* - 3\theta^{*^4}_{\infty} \tag{5}$$

Eq. (4) on differentiating, we obtain

$$\frac{\partial q_R^*}{\partial y^*} = -\frac{16\sigma_s \left(\theta_{\infty}^*\right)^3}{3k_e} \frac{\partial^2 \theta^*}{\partial y^{*^2}}$$
(6)

Taken into consideration of Eq. (4), Eq. (5) and Eq. (6), Eq. (3) is simplified as,

$$\left(\rho C_{p}\right)_{hnf}\left[\frac{\partial\theta^{*}}{\partial t^{'}}+u_{2}^{*}\frac{\partial\theta^{*}}{\partial y^{*}}\right]=\kappa_{hnf}\frac{\partial^{2}\theta^{*}}{\partial y^{*^{2}}}+\frac{16\sigma_{s}\left(\theta_{\infty}^{*}\right)^{3}}{3k_{e}}\frac{\partial^{2}\theta^{*}}{\partial y^{*^{2}}}+\mu_{hnf}\left(\frac{\partial u_{1}^{*}}{\partial y^{*}}\right)^{2}$$
(7)

The ancillary constraints are

$$t' \leq 0, \quad u_{1}^{*} = 0, \quad \theta^{*} = \theta_{\infty}^{*} \qquad \text{for all} \qquad y^{*}$$

$$t' > 0, \quad u_{1}^{*} = u_{1_{0}}^{*}, \quad \theta^{*} = \theta_{w}^{*} + (\theta_{w}^{*} - \theta_{\infty}^{*}) \cos \omega^{*} t' \quad \text{at} \qquad y^{*} = 0$$

$$u_{1}^{*} \rightarrow 0, \quad \theta^{*} \rightarrow \theta_{\infty}^{*} \qquad \text{as} \qquad y \rightarrow \infty$$
(8)

Eq. (1) gives $u_2^* = -u_{2_0}^* \left(u_{2_0}^* > 0 \right)$

Here, $u_{2_0}^*$ = constant suction velocity, and is towards the plate. Table 1 exhibits the Thermal features of water and nanoparticles. The necessary thermal parameters of Hybrid nano liquid ρ_{hnf} , μ_{hnf} , $\left(\rho C_p\right)_{hnf}$, $\left(\rho\beta\right)_{hnf}$, K_{hnf} are displayed in Table 2.

Table 1

|--|

	$\rho(kg/m^3)$	$C_p(J/kgK)$	$\kappa (W/mK)$	$\sigma(s/m)$	$\beta(1/K)$
H ₂ O	997.1	4179	0.613	5.5x10 ⁻⁶	21x10 ⁻⁵
Cu	8933	385	401	59.6x10 ⁶	1.67x10 ⁻⁵
TiO ₂	4250	686.2	8.9528	2.6x10 ⁶	0.9x10⁻⁵

Table 2

Thermo phys	ical attributes of nano liquid and hybric	d nano liquid
Properties	Nano liquid $Cu - H_2O$	Hybrid Nano liquid $Cu - TiO_2 - H_2O$
Density	$\rho_{nf} = \delta_1 \rho_s + (1 - \delta_1) \rho_f$	$\rho_{hnf} = \left\{ \left(1 - \delta_2\right) \left[\left(1 - \delta_1\right) \rho_f + \delta_1 \rho_{s1} \right] \right\} + \delta_2 \rho_{s2}$
Heat Capacity	$\left(\rho C_{p}\right)_{nf} = \delta_{1}\left(\rho C_{p}\right)_{s} + \left(1 - \delta_{1}\right)\left(\rho C_{p}\right)_{f}$	$\left(\rho C_{p}\right)_{hnf} = \left\{ \left(1 - \delta_{2}\right) \left[\left(1 - \delta_{1}\right) \left(\rho C_{p}\right)_{f} + \delta_{1} \left(\rho C_{p}\right)_{s1} \right] \right\}$
		$+ \delta_2 \left(ho C_p ight)_{s2}$
Viscosity	$\mu_{nf}=rac{\mu_f}{\left(1-\delta_1 ight)^{2.5}}$	$\mu_{hnf} = \frac{\mu_f}{\left(1 - \delta_1\right)^{2.5} \left(1 - \delta_2\right)^{2.5}}$
Thermal Conductivity	$\frac{\kappa_{nf}}{\kappa_f} = \frac{\kappa_s(n-1)\kappa_f - (n-1)\delta_1(\kappa_f - \kappa_s)}{\kappa_s + (n-1)\kappa_f + \delta_1(\kappa_f - \kappa_s)}$	$\kappa_{hnf} = \kappa_{bf} \left[\frac{\kappa_{s2} + (n_1 - 1)\kappa_{bf} - (n_1 - 1)\delta_2(\kappa_{bf} - \kappa_{s2})}{\kappa_{s2} + (n_1 - 1)\kappa_{bf} + \delta_2(\kappa_{bf} - \kappa_{s2})} \right]$
		Where
		$\kappa_{bf} = \kappa_f \left[\frac{\kappa_{s1} + (n_1 - 1)\kappa_f - (n_1 - 1)\delta_1(\kappa_f - \kappa_{s1})}{\kappa_{s1} + (n_1 - 1)\kappa_f + \delta_1(\kappa_f - \kappa_{s1})} \right]$
Thermal Expansion	$(\rho\beta)_{nf} = (1-\delta_1)(\rho\beta)_f + \delta_1(\rho\beta)_s$	$(\rho\beta)_{hnf} = (1-\delta_2) \left\{ (1-\delta_1)(\rho\beta)_f + \delta_1(\rho\beta)_{s_1} \right\} + \delta_2(\rho\beta)_{s_2}$
Electrical Conductivity	$\sigma_{nf} = \sigma_f \left[\frac{\sigma_s (1 + 2\delta_1) + 2\sigma_f (1 - \delta_1)}{\sigma_s (1 - \delta_1) + \sigma_f (2 + \delta_1)} \right]$	$\sigma_{hnf} = \sigma_{bf} \left[\frac{\sigma_{s_2}(1+2\delta_2) + 2\sigma_{bf}(1-\delta_2)}{\sigma_{s_2}(1-\delta_2) + \sigma_{bf}(2+\delta_2)} \right],$
		Where
		$\sigma_{bf} = \sigma_f \left[\frac{\sigma_{s_1}(1+2\delta_1) + 2\sigma_f(1-\delta_1)}{\sigma_{s_1}(1-\delta_1) + \sigma_f(2+\delta_1)} \right]$

Utilizing the relations,

$$u_{1} = \frac{u_{1}^{*}}{u_{l_{0}}^{*}}, \ t = \frac{t'u_{l_{0}}^{*}}{v_{f}}, \ y = \frac{y^{*}u_{l_{0}}^{*}}{v_{f}} = \frac{y^{*}}{L_{ref}}, \ \theta = \frac{\theta^{*} - \theta_{\infty}^{*}}{\theta_{w}^{*} - \theta_{\infty}^{*}}$$
(9)

After non-dimensioning, the flow controlling equations are

$$\frac{\partial u_2}{\partial y} = 0 \tag{10}$$

$$\frac{\partial u_1}{\partial t} - \lambda \frac{\partial u_1}{\partial y} = \frac{G_2}{G_1} \frac{\partial^2 u_1}{\partial y^2} + \frac{G_3}{G_1} Gr\theta - \frac{G_4}{G_1} M u_1$$
(11)

$$\frac{\partial\theta}{\partial t} - \lambda \frac{\partial\theta}{\partial y} = \left(G_6 + \frac{4}{3N}\right) \frac{1}{G_5 P_r} \frac{\partial^2 \theta}{\partial y^2} + \frac{G_2 Ec}{G_5} \left(\frac{\partial u_1}{\partial y}\right)^2$$
(12)

The analogous ancillary relations:

$$t \le 0, \quad u_1 = 0, \quad \theta = 0 \quad \text{for all } y$$

$$t > 0, \quad u_1 = 1, \quad \theta = 1 + \cos \omega t \quad \text{at} \quad y = 0 \quad (13)$$

$$u_1 \to 0, \quad \theta \to 0 \quad \text{as} \quad y \to \infty$$

Here,

$$P_{r} = \frac{v_{f}}{\alpha_{f}} = \frac{\left(\mu C_{p}\right)_{f}}{k_{f}}, \quad \lambda = -\frac{u_{2}^{*}}{u_{1_{0}}^{*}}, \quad Gr = \frac{g\beta_{f}v_{f}\left(\theta_{w}^{*} - \theta_{w}^{*}\right)}{\left(u_{1_{0}}^{*}\right)^{3}},$$
$$M = \frac{\sigma_{f}B_{0}^{2}v_{f}}{\rho_{f}u_{1_{0}}^{2}}, \quad N = \frac{k_{f}k_{e}}{4\sigma_{s}\theta_{w}^{*^{3}}}, \quad Ec = \frac{u_{1_{0}}^{*^{2}}}{\left(C_{p}\right)_{f}\left(\theta_{w}^{*} - \theta_{w}^{*}\right)}.$$
(14)

where,

$$\begin{aligned} G_{1} &= \left[\left(1 - \delta_{2} \right) \left\{ \left(1 - \delta_{1} \right) + \delta_{1} \frac{\rho_{s_{1}}}{\rho_{f}} \right\} \right] + \delta_{2} \frac{\rho_{s_{2}}}{\rho_{f}}, \\ G_{2} &= \frac{1}{\left(1 - \delta_{1} \right)^{2.5} \left(1 - \delta_{2} \right)^{2.5}}, \\ G_{3} &= \left[\left(1 - \delta_{2} \right) \left\{ \left(1 - \delta_{1} \right) + \delta_{1} \frac{\left(\rho \beta \right)_{s_{1}}}{\left(\rho \beta \right)_{f}} \right\} \right] + \delta_{2} \frac{\left(\rho \beta \right)_{s_{2}}}{\left(\rho \beta \right)_{f}}, \\ G_{4} &= \frac{\sigma_{bf}}{\sigma_{f}} \left[\frac{\sigma_{s_{2}} \left(1 + 2\delta_{2} \right) + 2\sigma_{bf} \left(1 - \delta_{2} \right)}{\sigma_{s_{2}} \left(1 - \delta_{2} \right) + \sigma_{bf} \left(2 + \delta_{2} \right)} \right], \\ G_{5} &= \left[\left(1 - \delta_{2} \right) \left\{ \left(1 - \delta_{1} \right) + \delta_{1} \frac{\left(\rho C_{p} \right)_{s_{1}}}{\left(\rho C_{p} \right)_{f}} \right\} \right] + \delta_{2} \frac{\left(\rho C_{p} \right)_{s_{2}}}{\left(\rho C_{p} \right)_{f}}, \\ G_{6} &= \frac{\kappa_{bf}}{\kappa_{f}} \frac{\left[\kappa_{s_{2}} + \left(n_{1} - 1 \right) \kappa_{bf} - \left(n_{1} - 1 \right) \delta_{2} \left(\kappa_{bf} - \kappa_{s_{2}} \right) \right]}{\left[\kappa_{s_{2}} + \left(n_{1} - 1 \right) \kappa_{bf} + \delta_{2} \left(\kappa_{bf} - \kappa_{s_{2}} \right) \right]}. \end{aligned}$$

$$\tag{15}$$

The analytical solution of Eq. (12) without the convective and viscous dissipation terms subject to frontier constraints (13) when $\left(\omega t = \frac{\pi}{2}\right)$, using Laplace transform technique is obtained as:

$$\theta = erfc \left(\frac{y\sqrt{pr}}{2\sqrt{\left(G_6 + \frac{4}{3N}\right)\frac{t}{G_5}}} \right)$$
(16)

3. Surface Engineering Properties

In this work, two dispensable parameters of engineering relevance, namely Coefficient of skin friction (C_f) and the heat transfer (Nu), are computed numerically and given as

$$C_{f} = \frac{\tau_{w}}{\rho_{f} u_{l_{0}}^{*^{2}}}, \quad Nu = \frac{q_{w} L_{ref}}{\kappa_{f} (\theta_{w}^{*} - \theta_{\infty}^{*})}$$
(17)

Here τ_w designates Skin-friction or shear stress and q_w designates rate of heat transmission as

$$\tau_{w} = \mu_{hnf} \left(\frac{\partial u_{1}^{*}}{\partial y^{*}} \right)_{y^{*}=0}, \quad q_{w} = -\kappa_{hnf} \left(\frac{\partial \theta^{*}}{\partial y^{*}} \right)_{y^{*}=0}$$
(18)

Utilizing dimensionless components in (10), we attain

$$C_{f} = \frac{1}{\left(1 - \delta_{1}\right)^{2.5} \left(1 - \delta_{2}\right)^{2.5}} \left(\frac{\partial u_{1}}{\partial y}\right)_{y=0} , \quad Nu = -\frac{\kappa_{hnf}}{\kappa_{f}} \left(\frac{\partial \theta}{\partial y}\right)_{y=0}$$
(19)

4. Solution Procedure

A robust Galerkin finite element approach, as shown in Figure 2, has decoded the PDE's (11) and (12) with inclusive pertinent conditions (13). The fundamental steps involved in this method are outlined by Rajesh and Chamkha [52], Reddy [53], and Bathe [54]. The analogous finite element equations on employing the Galerkin finite element procedure for Eq. (11) and Eq. (12) on the component (e) $(y_i \le y \le y_k)$ gives



Fig. 2. Flow chart – Galerkin Finite Element Method [8]

$$\int_{y_j}^{y_k} N^{*(e)^{\theta}} \left(\frac{G_2}{G_1} \frac{\partial^2 u_1^{(e)}}{\partial y^2} + \lambda \frac{\partial u_1^{(e)}}{\partial y} - \frac{\partial u_1^{(e)}}{\partial t} + \frac{G_3}{G_1} Gr\theta - \frac{G_4}{G_1} Mu_1 \right) dy = 0$$

$$\tag{20}$$

$$\int_{y_j}^{y_k} N^{*(e)^{\theta}} \left(\left[G_6 + \frac{4}{3N} \right] \frac{1}{P_r G_5} \frac{\partial^2 \theta^{(e)}}{\partial y^2} + \lambda \frac{\partial \theta^{(e)}}{\partial y} - \frac{\partial \theta^{(e)}}{\partial t} + \frac{G_2 E_c}{G_5} \left(\frac{\partial u_1}{\partial y} \right)^2 \right) dy = 0$$
(21)

On integrating Eq. (20) on both sides with respect to y, we get

$$\left(\frac{G_2}{G_1}\right)_{y_j}^{y_k} N^{*(e)^{\theta}} \frac{\partial^2 u_1^{(e)}}{\partial y^2} dy + \lambda \int_{y_j}^{y_k} N^{*(e)^{\theta}} \frac{\partial u_1^{(e)}}{\partial y} dy - \int_{y_j}^{y_k} N^{*(e)^{\theta}} \frac{\partial u_1^{(e)}}{\partial t} dy + \left(\frac{G_3}{G_1}\right) Gr \theta \int_{y_j}^{y_k} N^{*(e)^{\theta}} dy - \left(\frac{G_4}{G_1}\right) M \int_{y_j}^{y_k} N^{*(e)^{\theta}} u_1 dy = 0$$
(22)

Applying Integration by parts to Eq. (22),

$$\left(\frac{G_2}{G_1}\right)\left[N^{*(e)^{\theta}}\frac{\partial u_1^{(e)}}{\partial y}\right]_{y_j}^{y_k} - \left(\frac{G_2}{G_1}\right)\int_{y_j}^{y_k}\frac{\partial \left(N^{*(e)^{\theta}}\right)}{\partial y}\frac{\partial u_1^{(e)}}{\partial y}dy + \lambda\int_{y_j}^{y_k}N^{*(e)^{\theta}}\frac{\partial u_1^{(e)}}{\partial y}dy - \int_{y_j}^{y_k}N^{*(e)^{\theta}}\frac{\partial u_1^{(e)}}{\partial t}dy = -\left(\frac{G_3}{G_1}\right)Gr\theta\int_{y_j}^{y_k}N^{*(e)^{\theta}}dy + \left(\frac{G_4}{G_1}\right)M\int_{y_j}^{y_k}N^{*(e)^{\theta}}u_1dy$$
(23)

Neglect the first term and multiply Eq. (23) by (-1) the simplified equation is

$$\left(\frac{G_2}{G_1}\right)_{y_j}^{y_k} \frac{\partial \left(N^{*(e)^{\theta}}\right)}{\partial y} \frac{\partial u_1^{(e)}}{\partial y} dy - \lambda \int_{y_j}^{y_k} N^{*(e)^{\theta}} \frac{\partial u_1^{(e)}}{\partial y} dy + \int_{y_j}^{y_k} N^{*(e)^{\theta}} \frac{\partial u_1^{(e)}}{\partial t} dy = \left(\frac{G_3}{G_1}\right) Gr \theta \int_{y_j}^{y_k} N^{*(e)^{\theta}} dy - \left(\frac{G_4}{G_1}\right) M \int_{y_j}^{y_k} N^{*(e)^{\theta}} u_1 dy$$

$$(24)$$

Consider the lineal piecewise approximation solution be

$$u_1^{(e)} = N_j^*(y)u_{1_j}(t) + N_k^*(y)u_{1_k}(t) = N_j^*u_{1_j} + N_k^*u_{1_k}$$
(25)

$$\theta^{(e)} = N_j^*(y)\theta_j(t) + N_k^*(y)\theta_k(t) = N_j^*\theta_j + N_k^*\theta_k$$
(26)

Where

$$N_{j}^{*} = \frac{y_{k} - y}{y_{k} - y_{j}}, \ N_{k}^{*} = \frac{y - y_{j}}{y_{k} - y_{j}}, \ N^{*(e)'} = \left[N_{j}^{*} \ N_{k}^{*}\right]' = \left[N_{j}^{*} \ N_{k}^{*}\right] \text{ are base functions.}$$
(27)

On simplifying, we get

$$\left(\frac{G_{2}}{G_{1}}\right) \int_{y_{j}}^{y_{k}} \left[N_{j}^{*'}N_{j}^{*'} - N_{k}^{*'}N_{k}^{*'}\right] \left[u_{1_{j}}\right] dy - \lambda \int_{y_{j}}^{y_{k}} \left[N_{j}^{*(e)}N_{j}^{*(e)'} - N_{j}^{*(e)}N_{k}^{*(e)'}\right] \left[u_{1_{k}}\right] dy + \int_{y_{j}}^{y_{k}} \left[N_{j}^{*(e)}N_{j}^{*(e)} - N_{j}^{*(e)}N_{k}^{*(e)}\right] \left[u_{1_{k}}\right] dy + \int_{y_{j}}^{y_{k}} \left[N_{k}^{*(e)}N_{j}^{*(e)} - N_{k}^{*(e)}N_{k}^{*(e)}\right] \left[u_{1_{k}}\right] dy + \int_{y_{j}}^{y_{k}} \left[N_{k}^{*(e)}N_{j}^{*(e)} - N_{k}^{*(e)}N_{k}^{*(e)}\right] \left[u_{1_{k}}\right] dy = \left(\frac{G_{3}}{G_{1}}\right) Gr \theta \int_{y_{j}}^{y_{k}} \left[N_{j}^{*(e)}\right] dy - \left(\frac{G_{4}}{G_{1}}\right) M \int_{y_{j}}^{y_{k}} \left[N_{k}^{*(e)}N_{j}^{*(e)} - N_{k}^{*(e)}N_{k}^{*(e)}\right] \left[u_{1_{k}}\right] dy$$

$$Since, u_{1}^{(e)} = N^{*(e)} \psi^{*(e)} \text{ then } \frac{\partial u_{1}^{(e)}}{\partial y} = \frac{\partial N^{*(e)}}{\partial y} \psi^{*(e)} \text{ and } \frac{\partial u_{1}^{(e)}}{\partial t} = N^{*(e)} \frac{\partial \psi^{*(e)}}{\partial y},$$

Cy Cy

 $y_k - y_j = l_e$ (Length of the element)

$$\begin{pmatrix} \underline{G}_{2} \\ \overline{G}_{1}l_{e} \end{pmatrix} \begin{bmatrix} 1 & -1 \\ -1 & 1 \end{bmatrix} \begin{bmatrix} u_{1_{j}} \\ u_{1_{k}} \end{bmatrix} - \begin{pmatrix} \underline{\lambda} \\ 2 \end{pmatrix} \begin{bmatrix} -1 & 1 \\ -1 & 1 \end{bmatrix} \begin{bmatrix} u_{1_{j}} \\ u_{1_{k}} \end{bmatrix} + \begin{pmatrix} \underline{l}_{e} \\ \overline{6} \end{pmatrix} \begin{bmatrix} 2 & 1 \\ 1 & 2 \end{bmatrix} \begin{bmatrix} \cdot \\ u_{1_{j}} \\ \cdot \\ u_{1_{k}} \end{bmatrix} =$$

$$\begin{pmatrix} \underline{l}_{e}G_{3} \\ 2G_{1} \end{pmatrix} Gr\theta \begin{bmatrix} 1 \\ 1 \end{bmatrix} - \begin{pmatrix} \underline{l}_{e}G_{4} \\ \overline{6G_{1}} \end{pmatrix} M \begin{bmatrix} 2 & 1 \\ 1 & 2 \end{bmatrix} \begin{bmatrix} u_{1_{j}} \\ u_{1_{k}} \end{bmatrix}$$

$$(30)$$

where a dot denotes differentiation with respect to time. Assembling the element equations for two consecutive elements $y_{i-1} \le y \le y_i$ and $y_i \le y \le y_{i+1}$, we derive

$$\left(\frac{G_2}{G_1 l_e^2}\right) \begin{bmatrix} 1 & -1 & 0\\ -1 & 2 & -1\\ 0 & -1 & 1 \end{bmatrix} \begin{bmatrix} u_{1_{i-1}}\\ u_{1_i}\\ u_{1_{i+1}} \end{bmatrix} - \left(\frac{\lambda}{2}\right) \begin{bmatrix} 1 & -1 & 0\\ -1 & 0 & -1\\ 0 & -1 & 1 \end{bmatrix} \begin{bmatrix} u_{1_{i-1}}\\ u_{1_i}\\ u_{1_{i+1}} \end{bmatrix} + \left(\frac{1}{6}\right) \begin{bmatrix} 2 & 1 & 0\\ 1 & 4 & 1\\ 0 & 1 & 2 \end{bmatrix} \begin{bmatrix} \bullet\\ \bullet\\ u_{1_{i+1}}\\ \bullet\\ u_{1_{i+1}} \end{bmatrix} =$$

$$\left(\frac{G_3}{2G_1}\right) Gr\theta \begin{bmatrix} 1\\ 2\\ 1 \end{bmatrix} - \left(\frac{G_4}{2G_1}\right) M \begin{bmatrix} 2 & 1 & 0\\ 1 & 4 & 1\\ 0 & 1 & 2 \end{bmatrix} \begin{bmatrix} u_{1_{i-1}}\\ u_{1_i}\\ u_{1_{i+1}} \end{bmatrix}$$

$$(31)$$

Then putting the members of the row, corresponding to the node equal to zero, we obtain from Eq. (31) where $l_e=h$

$$\left(\frac{G_2}{G_1 h^2}\right) \left[-u_{1_{i-1}} + 2u_{1_i} - u_{1_{i+1}}\right] - \left(\frac{\lambda}{2h}\right) \left[-u_{1_{i-1}} + u_{1_{i+1}}\right] + \left(\frac{1}{6}\right) \left(\underbrace{\bullet}_{u_{1_{i-1}}} + 4\underbrace{u_{1_i}}_{u_{1_i}} + u_{1_{i+1}}\right) = \frac{G_3 Gr\theta}{G_1} - \frac{G_4 M}{6G_1} \left(u_{1_{i-1}} + 4u_{1_i} + u_{1_{i+1}}\right)$$
(32)

$$\mathbf{\dot{u}}_{1_{i-1}} + 4\mathbf{\dot{u}}_{1_{i}} + \mathbf{\dot{u}}_{1_{i+1}} = u_{1_{i-1}} \left[-\frac{G_{4}M}{G_{1}} - \frac{3\lambda}{h} + \frac{6G_{2}}{G_{1}h^{2}} \right] + u_{1_{i}} \left[-\frac{4G_{4}M}{G_{1}} - \frac{12G_{2}}{G_{1}h^{2}} \right] + u_{1_{i+1}} \left[-\frac{G_{4}M}{G_{1}} + \frac{3\lambda}{h} + \frac{6G_{2}}{G_{1}h^{2}} \right] + \frac{6G_{3}Gr\theta}{G_{1}}$$
(33)

Using α -family of time marching schemes (Trapezoidal rule), we have

Using Eq. (34) at stations j and j+1 in Eq. (35), we get

$$u_{l_{i-1}}^{j+1} \left[\frac{6G_2}{G_1h^2} - \frac{3\lambda}{h} - \frac{G_4M}{G_1} - \frac{2}{k} \right] + u_{l_i}^{j+1} \left[-\frac{12G_2}{G_1h^2} - \frac{4G_4M}{G_1} - \frac{8}{k} \right] + u_{l_{i+1}}^{j+1} \left[\frac{6G_2}{G_1h^2} + \frac{3\lambda}{h} - \frac{G_4M}{G_1} - \frac{2}{k} \right] =$$

$$u_{l_{i-1}}^j \left[-\frac{6G_2}{G_1h^2} + \frac{G_4M}{G_1} + \frac{3\lambda}{h} - \frac{2}{k} \right] + u_{l_i}^j \left[\frac{12G_2}{G_1h^2} + \frac{4G_4M}{G_1} - \frac{8}{k} \right] + u_{l_{i+1}}^j \left[-\frac{6G_2}{G_1h^2} - \frac{3\lambda}{h} + \frac{G_4M}{G_1} - \frac{2}{k} \right] - \frac{6G_3Gr\theta}{G_1} \left[T_i^j + T_i^{j+1} \right]$$

$$(35)$$

By Crank Nicolson Method, we have $T_i^{j} + T_i^{j+1} = T_i^{j}$.

The given system of Eq. (35) is converted into Matrix Tridiagonal form AX=B. Aloft equations are scrutinized for the numerical solutions of velocity and temperature stencils via Thomas algorithm [55]. The time and spatial step sizes $\Delta t = 0.01$, $\Delta y = 0.2$ along t and y directions are selected to give accurate results. A ' δ ' mesh sensitivity analysis with slightly revised values of the mesh distance in the t – and y – directions, i.e. k and h, has been operated through MATLAB program to define an optimal mesh system for u_1 , θ . Also, we performed grid independent analysis for various grid sizes 81x151, 161x301, 321x601 which is pointed in Figure 3 and confirmed to be in excellent agreement. Hence, we achieved mesh independence for solutions with excellent stability and convergence. To confirm the exactitude of the ciphered data, the temperature stencils of the current work in the absence of convective, and viscous dissipation terms when $\delta_2 = 0$ are compared with the analytical relation given by Eq. (15) in Figure 4. This authorizes the present ciphered technique is apt for the current simulation.



5. Result Analysis

The pronouncement of this segment is to examine the corollary of numerous ambient flow parameters such as Gr, M, N, Ec, ωt , t, δ_2 , λ , Nu, C_f, and these are presented through tables and pictorial representation. In current scrutiny, consider P_r = 6.2, M=5, Ec=0.09, N = 2, Gr = 10, $\lambda = 0.2$, t = 0.5, $\omega t = \pi/3$, $\delta_1 = 0.05$, $\delta_2 = 0.05$, and n₁ = 3 (spherical shaped nanoparticles) unless otherwise defined. From a chemical engineering and thermodynamic perspective, the Grashof number provides understanding the interaction between buoyant and viscous forces in natural convection circumstances. An increase in Grashof number signifies dominance in buoyant forces causes inclination for fluid motion and thus momentum elevates, and thermal stencil decelerates, as exposed in Figure 5 and Figure 6. As velocity booms with Gr, the skin friction coefficient for hybrid nano liquid escalates and is lower than that of nano liquid, as displayed in Table 4. Table 3 also perceived that the heat transfer rate with hybrid nano liquid is more than that corresponding to a regular nano liquid with similar constraints and that it amplifies as Gr rises.

INUSS	eit num	ber value	STOLE	1 = 0.2					
Gr	λ	Ec	Ν	Μ	ωt	t	δ2	Nusselt Number	
								Cu-H₂O	Cu-TiO ₂ -H ₂ O
5	0.2	0.09	2	5	π/3	1.5	0.05	2.2535	2.3084
10	0.2	0.09	2	5	π/3	1.5	0.05	2.3132	2.3778
15	0.2	0.09	2	5	π/3	1.5	0.05	2.3519	2.4276
5	0.4	0.09	2	5	π/3	1.5	0.05	3.1175	3.1854
5	0.6	0.09	2	5	π/3	1.5	0.05	4.0632	4.1307
5	0.2	0.09	3	5	π/3	1.5	0.05	2.4419	2.4963
5	0.2	0.09	4	5	π/3	1.5	0.05	2.5143	2.5622
5	0.2	0.09	2	6	π/3	1.5	0.05	2.3003	2.3632
5	0.2	0.09	2	7	π/3	1.5	0.05	2.2932	2.3561
5	0.2	0.09	2	5	$\pi/6$	1.5	0.05	2.9725	3.0723
5	0.2	0.09	2	5	π/2	1.5	0.05	1.4044	1.4214
5	0.2	0.08	2	5	π/3	1.5	0.05	2.3467	2.4178
5	0.2	0.07	2	5	π/3	1.5	0.05	2.3804	2.4579
5	0.2	0.09	2	5	π/3	0.5	0.05	3.5626	3.7156
5	0.2	0.09	2	5	π/3	1	0.05	2.6906	2.7822
5	0.2	0.09	2	5	π/3	1	0.10	2.2646	2.3226
5	0.2	0.09	2	5	π/3	1	0.15	2.3251	2.3824

Table 3Nusselt number values for Pr = 6.2

Table 4

Skin Friction Coefficient Values for Pr = 6.2

•					0.2					
Gr	λ	Ec	Ν	М	ωt	t	δ2	Skin Friction Coefficient		
								Cu-H ₂ O	Cu-TiO ₂ -H ₂ O	
5	0.2	0.09	2	5	π/3	1.5	0.05	-4.0506	-4.3461	
10	0.2	0.09	2	5	π/3	1.5	0.05	-2.5864	-2.7344	
15	0.2	0.09	2	5	π/3	1.5	0.05	-0.8170	-1.4135	
5	0.4	0.09	2	5	π/3	1.5	0.05	-3.2369	-3.2394	
5	0.6	0.09	2	5	π/3	1.5	0.05	-3.9978	-3.8199	
5	0.2	0.09	3	5	π/3	1.5	0.05	-2.6449	-2.7719	
5	0.2	0.09	4	5	π/3	1.5	0.05	-2.6772	-2.7924	
5	0.2	0.09	2	6	π/3	15	0.05	-3.3365	-3.3735	
5	0.2	0.09	2	7	π/3	1.5	0.05	-4.0041	-3.9429	
5	0.2	0.09	2	5	π/6	1.5	0.05	-1.7440	-2.1050	
5	0.2	0.09	2	5	π/2	1.5	0.05	-3.7352	-3.5930	
5	0.2	0.08	2	5	π/3	1.5	0.05	-2.5949	-2.7408	
5	0.2	0.07	2	5	π/3	1.5	0.05	-2.6035	-2.7473	
5	0.2	0.09	2	5	π/3	0.5	0.05	-3.3454	-3.4617	
5	0.2	0.09	2	5	π/3	1	0.05	-2.8421	-2.9109	
5	0.2	0.09	2	5	π/3	1	0.10	-4.1290	-4.4213	
5	0.2	0.09	2	5	π/3	1	0.15	-4.1326	-4.4341	

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Fig. 5. Collation of Gr on Velocity pattern



Figure 7 and Figure 8 potray's the enhancement in velocity and temperature as Eckert number enhances. This is real, because enhancement in Eckert number produces more heat in between liquid particles due to frictional forces. Table 3 points out that due to supersize of Ec, the Nusselt number is larger in hybrid nano liquids in contrast to nano liquids. From Table 4 it is clear that skin friction coefficient enlarges for both liquids due to the Ec amplification, which can have conclusion for mixing, heat transfer, and energy efficiency in several chemical engineering and thermodynamic processes. It can be seen from Figure 9 and Figure 10 that enlargement in suction parameter, decelerates the velocity and temperature of both liquids. Physically, it is a fact that on employing suction on the plate surface, catalyses the liquid into the plane, as a result curtailment of momentum and thermal boundary layers lowered as λ rises. In chemical engineering and thermodynamics processes, this tends to reduce fluid velocities, alter temperature profiles, and influence mixing and thermal transfer effectiveness. The Nusselt number elevates upon the escalation of λ for both type of liquids and jacked up in hybrid nano liquids in contrast to nano liquids, which is obeyed from Table 3. The dwindling of coefficient of skin friction with enlargement of λ for both the liquids is pointed in Table 4 and also it is tipped that the hybrid nano liquids coefficient of skin friction is less than that of regular nano liquids.



Fig. 7. Collation of Ec on Velocity pattern



Fig. 8. Collation of Ec on Temperature pattern







From Figure 11 and 12, the velocity of both hybrid nano liquids and nano liquids decreases as M grows whereas temperature increases for both liquids. From chemical engineering and thermodynamic perspective, upwind in M yields in piling up the Lorentz force which catalyzes opposing circulation of fluid, results in development of stress, as a result temperature builds up. It is documented in Table 3 that proliferation of M, yields in depletion of Nusselt number for both type of liquids, the Nusselt number in hybrid nano liquids dominates over nano liquids. From the Table 4, it is noted that due to amplification of M, drop in skin friction is confirmed. However, the skin friction of hybrid nano liquid is lesser than that of nano liquid. From Figure 13 and Figure 14 we understood that due to the amplification of N both velocity and temperature features shrinks. Physically we agree that thermal radiation N is a function of ratio between conduction to radiation, as N accentuates, which results in the lessening of radiative flux induces the suppression of energy transport to the liquid causing the cooling and thinning of momentum and thermal boundary layers from the aspect of chemical engineering and thermodynamics.



Fig. 11. Collation of M on Velocity pattern



Fig. 12. Collation of M on Temperature pattern







Figure 15 and Figure 16 points that each of two hybrid nano liquids and nano liquids velocity drops, but the temperature accelerates with the expansion of δ_2 . Since appending of further nanoparticles leads to ease off the flow area and employ excess energy, which intensify the temperature and hence condense thermal boundary layer by chemical engineering and thermodynamics aspects. Intensification of δ_2 slows down the velocity stream, which evidently drops both types of nano liquids skin friction, shown in Table 4. Figure 17 and Figure 18 narrates that as t escalates the velocity and temperature together enlarges for both the liquids. Also, with the hike in t Nusselt number boosts up for both type of liquids and the Nusselt number is larger in Hybrid nano liquids in contrast to nano liquids which is spotted in Table 4. Proliferation of ω t leads to downsize of velocity and temperature together for both type of liquids as seen in Figure 19 and Figure 20. Upon the rise in ω t, Nusselt number reduces for both type of liquids, Nusselt number is large in Hybrid nano liquids in contrast to nano liquids. It is noted in Table 4 that as ω t rises, both liquids skin friction coefficient drops.





Fig. 16. Collation of δ_2 on Velocity pattern

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6. Conclusions

The outcomes of the present analysis:

- i. Superior heat transmission through Cu-TiO₂ H₂O can be attained than Cu- H₂O by choosing Cu-TiO₂ H₂O as a working liquid.
- ii. The lesser skin friction coefficient is celebrated for Cu-TiO₂ H₂O than Cu-H₂O. Velocity, skin friction parameters are spotted to increase with Gr. However, temperature and Nusselt numbers remain constant for both liquid cases. As Gr enhances, upsurge in buoyancy takes place, as a consequence upswing in velocity is recorded.
- iii. Velocity, temperature and skin friction parameters are shrinking functions of λ for both liquid cases. However, Nusselt number is an inclining function of λ . Physically, it is a fact that on employing suction on the plate surface, catalyzes the liquid into the plane, as a result curtailment of momentum and thermal boundary layers lowered as λ rises.
- iv. Velocity is spotted to reduce with ωt , but skin friction is spotted to grow with ωt . However, temperature and Nusselt numbers remain constant for two types of liquids.
- v. Velocity and temperature are declining functions of N for nano liquid and hybrid nano liquid. However, Nusselt number inclines with N, but skin friction declines with N. Physically we

agree that thermal radiation N is relation between conduction to radiation, as N accentuates, which outcomes the lessening of radiative flux induces the suppression of energy transport to the fluid causing the cooling and thinning of momentum and thermal boundary layers.

- vi. There is enhancement in velocity and temperature as Eckert number enhances. It is fact, because enhancement in Eckert number produces more heat in between liquid particles due to frictional forces.
- vii. Due to supersize of Ec, the Nusselt number is larger in hybrid nano liquids in contrast to nano liquids. Skin friction coefficient enlarges for both liquids due to the Ec amplification, which can have conclusion for mixing, heat transfer, and energy efficiency in several chemical engineering and thermodynamic processes.
- viii. The velocity of both hybrid nano liquids and nano liquids decreases as M grows whereas temperature increases for both liquids. From chemical engineering and thermodynamic perspective, upwind in M yields in piling up the Lorentz force which catalyzes opposing circulation of fluid, results in development of stress, as a result temperature builds up.
- ix. Velocity is spotted to reduce with δ_2 , but the temperature is spotted to grow with δ_2 for both liquid cases. Velocity, temperature and skin friction parameters are inclining functions of time t for both liquids. However, Nusselt number is the declining function of time t.
- x. Some of the applications of the current model which are efficiently used in different engineering fields including hydromagnetic motion in geothermal reservoirs, nuclear coolants, MHD power generation, thermal imaging cameras like building inspections, earth's climate systems such as global temperatures, heat exchanger design where the efficiency of heat transfer between the fluids is designed etc.

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