



Mixed Convection in a Lid-Driven Horizontal Rectangular Cavity Filled with Hybrid Nanofluid by Finite Volume Method

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ABSTRACT

In the present work, a new type of nanofluid called the hybrid nanofluid (Al_2O_3 -Cu-water) is used to enhance the heat transfer. The Finite-Volume-Method (FVM) along with the SIMPLE-algorithm has been utilized to study the heat-transfer and, mixed convection fluid-flow of the hybrid nanofluid (Al_2O_3 -Cu-water), placed within the lid-driven rectangular cavity. The bottom and top walls are subjected to constant high temperature (T_h) and low temperature (T_c) respectively. The side walls are treated as adiabatic. The top wall moves in the positive x-direction. The effects of Reynolds number and hybrid nanoparticle volume fraction on the flow field have been investigated. It is found that the mean Nusselt number increases with respect to Reynolds numbers and hybrid nanoparticle volume fraction.

1. Introduction

Tremendous amount of heat is generated from various engineering applications such as those encountered in manufacturing, thermal power plants, microelectronics, transportation, etc. Efficient coolers have been designed to adequately dissipate heat. In general, cooling method can be categorized into passive and active methods [1–4]. Traditional coolers such as propylene glycol, water, oils and, ethylene glycol have low thermal conductivities. In order to enhance the heat transfer, the thermal conductivity of the fluid should be enhanced. One of the methods is mixing the base fluid with nano-sized particles (hence the term nanofluid [5]). The frequently used nanoparticles are metals (Ni, Ag, Au and, Cu), metal-oxides (CuO , Al_2O_3 , ZnO , MgO , Fe_2O_3 , TiO_2 and, SiO_2), metal-nitride (AlN), metal-carbide (SiC) and carbon materials (MWCNTs, CNT, Diamond and, Graphite). In general, the thermal conductivity of nanofluid is dependent on parameters such as shape, size, stability of scattered nano-particles, type of base-fluid, mass concentration of nanoparticles and fluid

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temperature [6,7]. As compared to traditional fluids, nanofluids have been shown to exhibit better thermal performance in a wide range of engineering applications [8-11].

Rasul *et al.*, [12] studied the effect of the presence of a heat source and its location on natural convection in a C-shaped enclosure saturated by a nanofluid is investigated numerically using the lattice Boltzmann method. They concluded that maximum increase is obtained when the heat source is located in the upper part of the vertical. Dogonchi *et al.*, [13] studied numerically investigate the effects of shape factors of nanoparticles on natural convection in a fluid-saturated porous annulus developed between the elliptical cylinder and square enclosure. They concluded that enhancement of Rayleigh number increases the velocity of nanofluid. Seyed *et al.*, [14] studied Hybrid thermal performance enhancement of a circular latent heat storage system by utilizing partially filled copper foam and Cu/GO nano-additives. They found that the charging power can be enhanced to about four times at the cost of only a 3% reduction of the thermal storage's capacity. Mohammad *et al.*, [15] studied free convection heat transfer analysis of a suspension of nano-encapsulated phase change materials (NEPCMs) in an inclined porous cavity. They found that the presence of the NEPCM particles generally leads to heat transfer improvement. Sadeghi *et al.*, [16] studied the effect of charging and discharging of multi-layers of Phase Change Materials (PCMs) in coaxial cylinders with a time-periodic boundary condition. Mehryan *et al.*, [17] studied conjugate phase change heat transfer in an inclined compound cavity partially filled with a porous medium. They found that the rates of melting and heat transfer are enhanced as the thickness of the porous layer increases. Tilehnoee *et al.*, [18] studied natural convection analysis conjugated with entropy generation analysis in an incinerator shaped permeable enclosure loaded with Al_2O_3 -water nanofluid subjected to the magnetic field with a rectangular wavy heater block positioned on the bottom of the cavity wall. They found that the Nusselt number and entropy generation number increase as the Rayleigh number and the Darcy number grow. Menni *et al.*, [19] studied the hydrodynamic and thermal analysis of turbulent forced-convection flows of pure water, pure ethylene glycol and water-ethylene glycol mixture, as base fluids dispersed by Al_2O_3 nano-sized solid particles, through a constant temperature-surfaced rectangular cross-section channel. They found that the pure ethylene glycol with Al_2O_3 nanoparticles showed a significant heat transfer enhancement.

Also, the thermal conductivity of nanoparticle can be further enhanced by mixing (hybridization) two (or more) types of nanoparticles (or hybrid-nanoparticles). Their hybrid nanoparticles are simply the extension of mono-nanoparticles. Undoubtedly, hybrid nanofluids exhibit higher thermal-conductivity than conventional nanofluids consisting of only one type of nano-particles[20–23].

Internal flow in enclosures could be driven by natural or mixed convections. Mixed convection is commonly found in manufacturing of float glass, solar collectors, solar ponds, food-processing and lubrication. Cimpean *et al.*, [24] studied mixed convection in a trapezoidal porous cavity filled with the hybrid nanofluid (Al_2O_3 , Cu -water). They found that higher Reynolds number would increase the heat transfer. Ismael *et al.*, [25] investigated the mixed convection in a lid-driven cavity filled with Al_2O_3 -Cu-water hybrid nanofluid. The nanofluid was heated by a triangular heater and cooled isothermally from the right vertical wall. They found that the hybrid nanofluid is a cost-effective solution as the amount of nanoparticles can be reduced. Mohammad *et al.*, [26] studied conjugate natural convection flow of Ag–MgO/water hybrid nanofluid in a square cavity. They found that the local Nusselt number at the surface of the conjugate wall decreases substantially by moving from the bottom of the cavity toward the top. Wakif *et al.*, [27] studied the effects of thermal radiation and surface roughness on the complex dynamics of water conveying alumina and copper oxide nanoparticles. They found that the partial substitution of the alumina nanoparticles by the copper oxide nanomaterials in the mixture stabilizes importantly the hybrid nanofluidic medium. Some advanced experimental studies using hybrid nanofluids have been reported [28–34]. The aim of this

study is to investigate the effects of hybrid nanofluid volume fraction and Reynolds number on the flow field in the rectangular cavity.

2. The Mathematical Modelling (Formulation)

The two dimensional (2D) Mixed convection problem in the rectangular cavity of length ($L=2$) is shown in Figure 1. The upper and lower walls are isothermal, where the lower wall temperature T_h is higher than the upper wall temperature T_c . Both side walls are adiabatic. The fluid inside the rectangular cavity is water-based hybrid nanofluid (Al_2O_3 , Cu). The dimensional governing equations are (Ali *et al.*, 2020) and (Azizul *et al.*, 2020)

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho_{hnf}} \frac{\partial p}{\partial x} + \nu_{hnf} \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) \quad (2)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho_{hnf}} \frac{\partial p}{\partial y} + \nu_{hnf} \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) + g\beta_{hnf}(T - T_c) \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \alpha_{hnf} \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) \quad (4)$$

The definition of the boundary-conditions as follows

$$\text{The top wall-side: } u = u_0 ; v = 0 ; T = T_c \quad (5)$$

$$\text{The bottom wall-side: } u = 0 ; v = 0 ; T = T_h \quad (6)$$

$$\text{The left and, right wall-sides: } u = v = 0 ; \frac{\partial T}{\partial x} = 0 \quad (7)$$

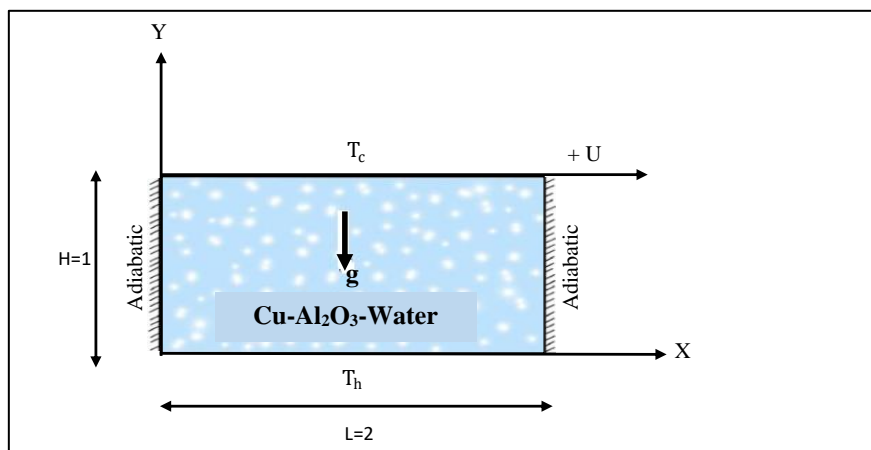


Fig. 1. Physical model

where the x and y indicate the Cartesian coordinates in the horizontal and vertical directions, respectively, g is the gravity acceleration, ρ_{hnf} is the density of the hybrid nanofluid, β_{hnf} is the thermal expansion coefficient of the hybrid nanofluid, ϕ is the solid volume fraction, α is the thermal

diffusivity of the hybrid nanofluid and, ν_{hnf} is the kinematic viscosity of the hybrid nanofluid. The physical properties of the hybrid nanofluid [35] are given below.

The hybrid nanofluid density ρ_{hnf} is given as

$$\rho_{\text{hnf}} = \phi_{\text{Cu}}\rho_{\text{Cu}} + \phi_{\text{Al}_2\text{O}_3}\rho_{\text{Al}_2\text{O}_3} + (1 - \phi_{\text{Cu}} - \phi_{\text{Al}_2\text{O}_3})\rho_f \quad (8)$$

The hybrid nanofluid heat capacitance $(\rho c_p)_{\text{hnf}}$ is given as

$$(\rho c_p)_{\text{hnf}} = \phi_{\text{Cu}}(\rho c_p)_{\text{Cu}} + \phi_{\text{Al}_2\text{O}_3}(\rho c_p)_{\text{Al}_2\text{O}_3} + (1 - \phi_{\text{Cu}} - \phi_{\text{Al}_2\text{O}_3})(\rho c_p)_f \quad (9)$$

The hybrid nanofluid buoyancy coefficient $(\rho\beta)_{\text{hnf}}$ can be calculated via

$$(\rho\beta)_{\text{hnf}} = \phi_{\text{Cu}}(\rho\beta)_{\text{Cu}} + \phi_{\text{Al}_2\text{O}_3}(\rho\beta)_{\text{Al}_2\text{O}_3} + (1 - \phi_{\text{Cu}} - \phi_{\text{Al}_2\text{O}_3})(\rho\beta)_f \quad (10)$$

The dynamic viscosity ratio of a nanofluid can be determined using the method developed by Corcione *et al.*, [36]

$$\frac{\mu_{\text{hnf}}}{\mu_f} = 1 / (1 - 34.87 \left(\frac{d_p}{d_f}\right)^{-0.3} \phi^{1.03}) \quad (11)$$

Finally, the thermal conductivity ratio of the nanofluid is determined as [36]

$$\frac{k_{\text{hnf}}}{k_f} = 1 + 4.4 \text{Re}_B^{0.4} \text{Pr}^{0.66} \left(\frac{T}{T_{fr}}\right)^{10} \left(\frac{k_p}{k_f}\right)^{0.03} \phi^{0.66} \quad (12)$$

where T_{fr} is the freezing point of the base fluid (273.15K).

Based on these mathematical models, the dynamic viscosity ratio and the thermal-conductivity ratio of the hybrid nanofluids (Al₂O₃-Cu)-water of particle sizes 33 nm and 29 nm in the ambient condition can be calculated as

$$\frac{\mu_{\text{hnf}}}{\mu_f} = 1 / \{1 - 34.87 (d_f)^{0.3} [(d_{\text{Cu}})^{-0.3} (\phi_{\text{Cu}})^{1.03} + (d_{\text{Al}_2\text{O}_3})^{-0.3} (\phi_{\text{Al}_2\text{O}_3})^{1.03}]\} \quad (13)$$

$$\frac{k_{\text{hnf}}}{k_f} = 1 + 4.4 \text{Re}_B^{0.4} \text{Pr}^{0.66} \left(\frac{T}{T_{fr}}\right)^{10} (k_f)^{-0.03} [(k_{\text{Cu}})^{0.03} (\phi_{\text{Cu}})^{0.66} + (k_{\text{Al}_2\text{O}_3})^{0.03} (\phi_{\text{Al}_2\text{O}_3})^{0.66}] \quad (14)$$

where Re_B defined for hybrid nanofluid is

$$\text{Re}_B = \frac{\rho_f u_B (d_{\text{Cu}} + d_{\text{Al}_2\text{O}_3})}{\mu_f} \quad (15)$$

$$u_B = \frac{2 k_b T}{\pi \mu_f (d_{\text{Cu}} + d_{\text{Al}_2\text{O}_3})^2} \quad (16)$$

Here; $k_b = 1.380648 \times 10^{-23}$ (J/K) is the Boltzmann-constant, $l_f = 0.17$ nm is the mean-path of fluid particles and, d_f is the molecular-diameter of water [36]

$$d_f = \frac{6 M}{N^* \pi \rho_f} \quad (17)$$

where; M denotes the molecular-mass of the working-fluid, N^* define is the Avogadro-number and, ρ_f is the working fluid-density at normal temperature (310K). In the present work, thenon-dimensional variables are presented as

$$X = \frac{x}{L}, Y = \frac{y}{L}, U = \frac{u}{U_0}, V = \frac{v}{U_0}, \theta = \frac{T-T_c}{T_h-T_c} = \frac{T-T_c}{\Delta T}, Pr = \frac{\nu_f}{\alpha_f}, P = \frac{\rho L^2}{\rho_f \alpha_f^2}, Ri = \frac{Gr}{Re^2} \quad (18)$$

Then, the non-dimensional governing equations

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} = 0 \quad (19)$$

$$U \frac{\partial U}{\partial X} + V \frac{\partial U}{\partial Y} = -\frac{\partial P}{\partial X} + \frac{1}{Re} \frac{\mu_{hnf}}{\mu_f} \frac{\rho_f}{\rho_{hnf}} \left(\frac{\partial^2 U}{\partial X^2} + \frac{\partial^2 U}{\partial Y^2} \right) \quad (20)$$

$$U \frac{\partial V}{\partial X} + V \frac{\partial V}{\partial Y} = -\frac{\partial P}{\partial Y} + \frac{1}{Re} \frac{\mu_{hnf}}{\mu_f} \frac{\rho_f}{\rho_{hnf}} \left(\frac{\partial^2 V}{\partial X^2} + \frac{\partial^2 V}{\partial Y^2} \right) + \left(\frac{(\rho\beta)_{hnf}}{\rho_{hnf}\beta_f} \right) Ri \theta \quad (21)$$

$$U \frac{\partial \theta}{\partial X} + V \frac{\partial \theta}{\partial Y} = \frac{\alpha_{hnf}}{\alpha_f} \frac{1}{Pr Re} \left(\frac{\partial^2 \theta}{\partial X^2} + \frac{\partial^2 \theta}{\partial Y^2} \right) \quad (22)$$

As well as, the dimensionless of boundary conditions are

$$\text{The top wall-side: } U = 1; V = 0; \theta = 0 \quad (23)$$

$$\text{The bottom wall-side: } U = 0; V = 0; \theta = 1 \quad (24)$$

$$\text{The left and, right wall-sides: } U = V = 0; \frac{\partial \theta}{\partial X} = 0 \quad (25)$$

The local Nusselt numbers for the hot wall, cold wall and the average Nusselt number are given in Eq. (26) – Eq. (28), respectively

$$Nu_x = -\frac{k_{hnf}}{k_f} \left(\frac{\partial \theta}{\partial Y} \right)_{Y=0} \quad (26)$$

$$Nu_x = -\frac{k_{hnf}}{k_f} \left(\frac{\partial \theta}{\partial Y} \right)_{Y=1} \quad (27)$$

$$\overline{Nu} = \int_0^D Nu_x dx \quad (28)$$

3.Numerical Technique

The governing equations are solved numerically using FVM [37]. The convection term is approximated using the power-law scheme. The SIMPLE algorithm is used for pressure-velocity coupling. Then, the algebraic system of equations is solved using the TDMA algorithm written in FORTRAN 90 programming language. The relaxation factor is set below 0.5 for momentum and energy equations in order to obtain convergence. The convergence criterion is calculated as

$$\text{error} = \frac{\sum_{j=1}^m \sum_{i=1}^n |\eta_{i,j}^{k+1} - \eta_{i,j}^k|}{\sum_{j=1}^m \sum_{i=1}^n |\eta_{i,j}^{k+1}|} \leq 10^{-7} \quad (29)$$

where m and n are denoted as the grid-point numbers in the x and, y directions, respectively, η is any transport quantity and k is the iteration number.

4. Mesh Independent and Validation

To check for grid-independence, simulations using four different grid sizes, i.e. 80×40 , 100×50 , 120×60 , 140×70 are executed. The numerical setting can be found in Table. 1. Based on the table, the result obtained on the 120×60 grid is already grid - independent. The result has been compared to that of Ismael *et al.*, [38] who studied the mixed convection in a double lid-driven square cavity with the partial slip. The results showed good agreement has been found as shown in Figure 2.

Table 1
 Mesh convergence

Size	Average Nusselt number \bar{Nu}
80x40	4.869276
100x50	4.889277
120x60	4.897964
140x70	4.900624

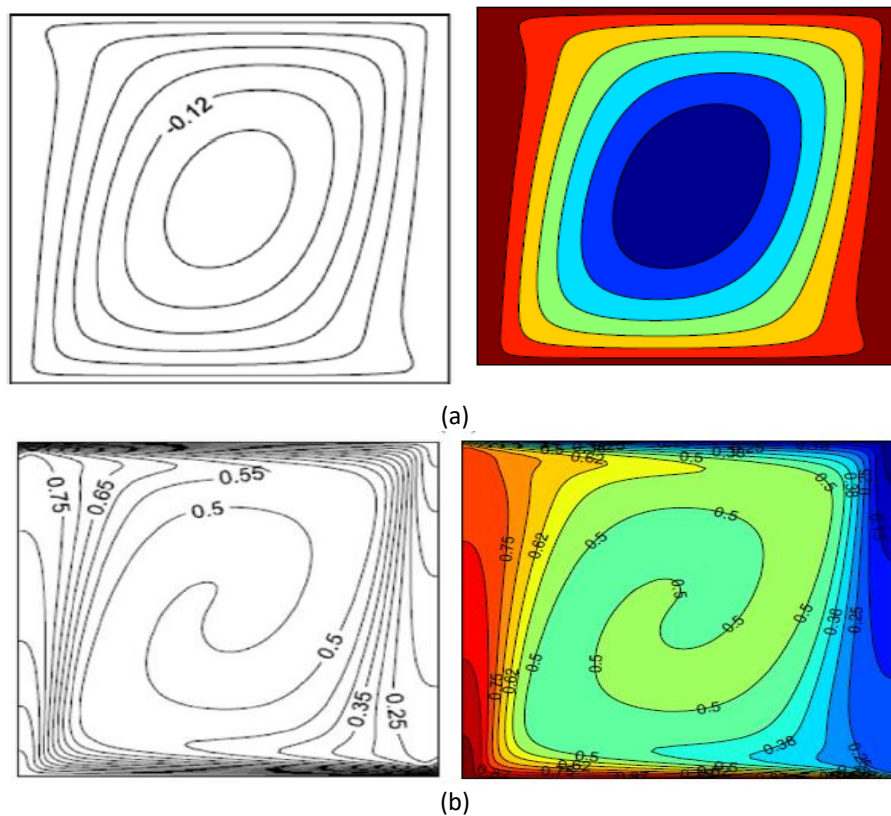


Fig. 2. Streamlines patterns (a), in left Ismael *et al.*, [38]; in right present study and, validation of isotherms (lines) (b), in left Ismael *et al.*, [38], in right present study

5. Results and Discussion

The heat transfer properties within the rectangular cavity filled with hybrid nanofluid (Al_2O_3 -Cu-water) have been studied. The effects of parameters such as volume fraction and Reynolds number on the heat transfer with $\text{Pr} = 6.2$ have been investigated. Streamlines, isotherms and averaged Nusselt number have been investigated. The thermo-physical characteristics of the basic fluid (water) and the $\text{Al}_2\text{O}_3 + \text{Cu}$ nanoparticles are reported in Table 2. Figure 3 shows the streamlines and isotherms at $\text{Re} = 10$, $L = 2.5$, $\text{Ri} = 1$. A primary recirculation cell rotating in the clockwise direction can be observed. As the volume fraction of the hybrid nanoparticle increases, the intensity of the vortex increases, and the streamlines move closer to each other. The isothermal lines are clustered near the isothermal walls, indicating that the temperature gradients are relatively high in these regions. As the volume fraction of nanoparticle increases, the isothermal lines become less congested.

Figure 4 shows the effect of Re on the streamlines and isotherms at $\text{Ri} = 10$, $L = 2.5$, $\phi = 0.02$. There is a central vortex rotating in the clockwise direction. The isotherms at $\text{Re} = 1$ follow closely to those observed in the pure conduction case. Pure conduction occurs due to weak convection as shown in Figure 4 (a, b). Stratification tends to be more apparent as Re is increased up to 10. By further increasing the Re as shown in Figure 4 (c, d), the cavity center tends to become isothermal. Figure 5 shows the distribution of local (area) Nusselt number along the hot wall for different Re values ($\text{Ri} = 10$, $\phi = 0.02$ and, $L = 2$).

As shown in Figure 6, the local Nusselt number increases with respect to Re due to more intense mixing. Figure 7 shows the effect of volume fraction on the local Nusselt number ($\text{Re} = 10$, $\text{Ri} = 10$, $L = 2$). As expected, the increase in volume fraction can enhance the local Nusselt number in the warm regions.

Table 2

Thermo-physical characteristics of water, Cu, Al_2O_3 nanoparticles ($T = 310 \text{ K}$) [39]

Physical properties	Base fluid water	Cu	Al_2O_3
$k \text{ (Wm}^{-1}\text{K}^{-1}\text{)}$	0.628	400	40
$\mu \times 10^6 \text{ (kg/ms)}$	695	-	-
$\rho \text{ (kg/m}^3\text{)}$	993	8933	3970
$C_p \text{ (J/kgK)}$	4178	385	765
$\beta \times 10^{-5} \text{ (1/K)}$	36.2	1.67	0.85
$d_p \text{ (nm)}$	0.385	29	33

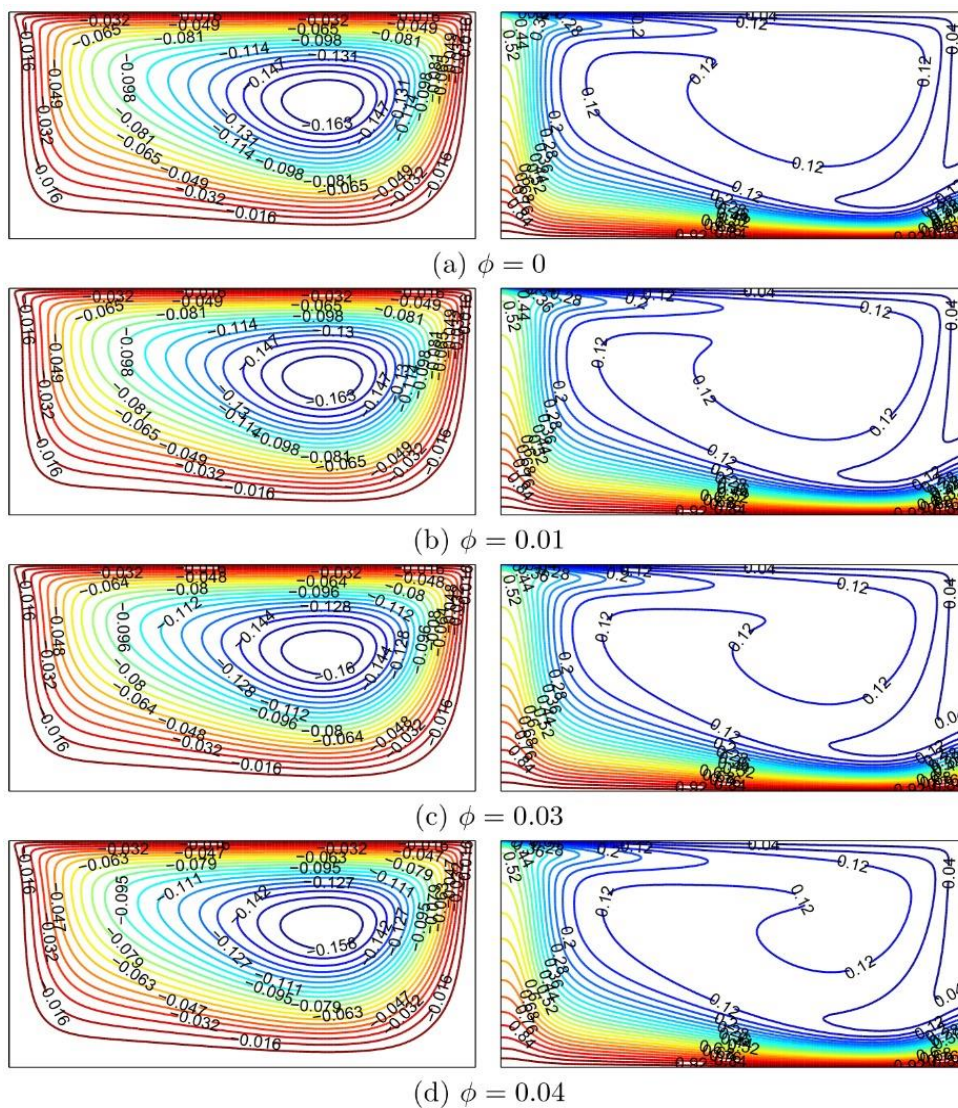


Fig. 3. Variations of streamlines in left and, isotherms in right, when (a) $\phi = 0.0$, (b) $\phi = 0.01$, (c) $\phi = 0.03$, (d) $\phi = 0.04$

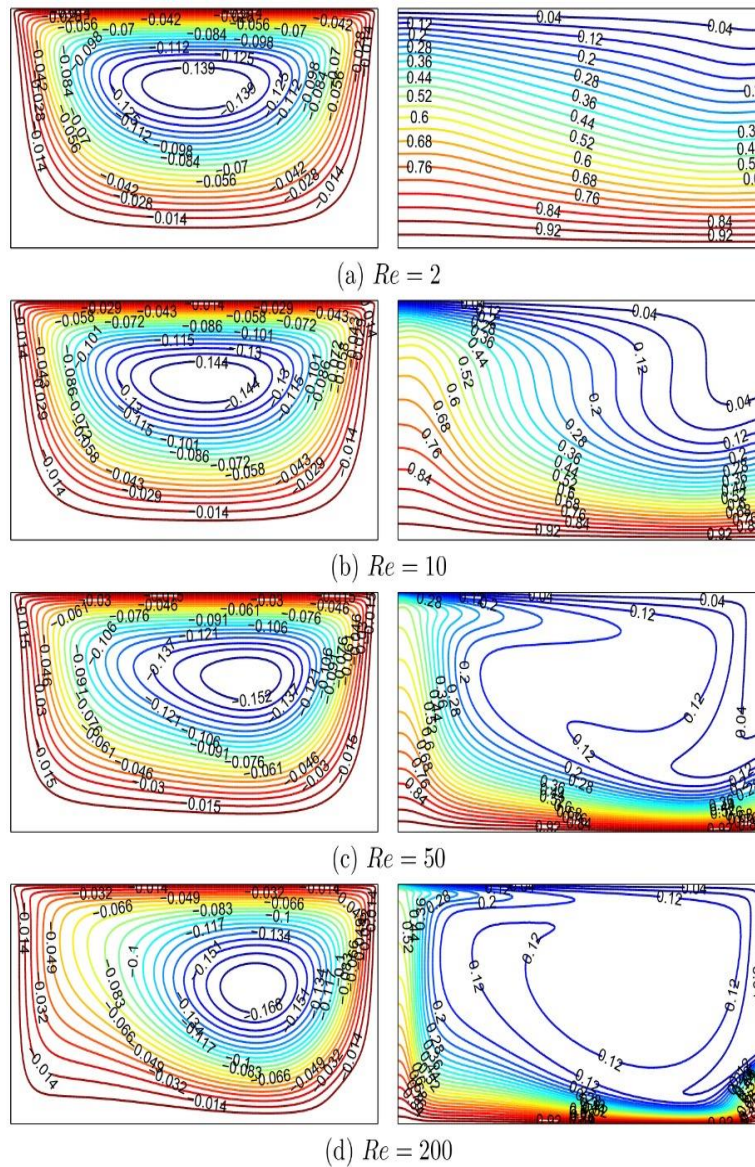


Fig. 4. Variations for streamlines in left and, isotherms in right, when (a) $Re = 2$, (b) $Re = 10$, (c) $Re = 50$, (d) $Re = 200$

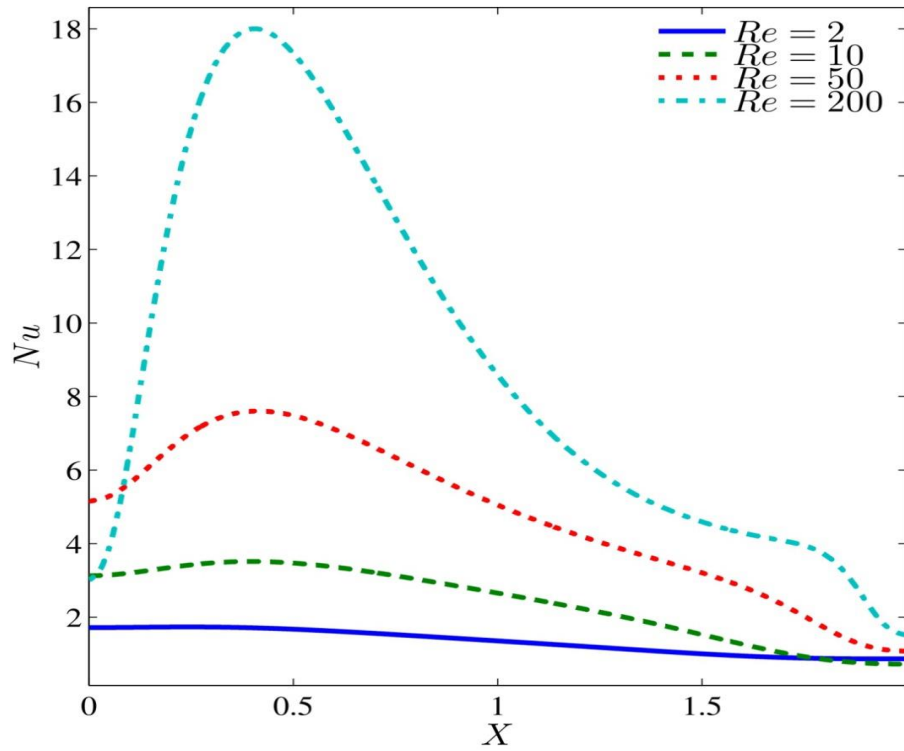


Fig. 5. Variations of the local Nusselt-number against X for different Re

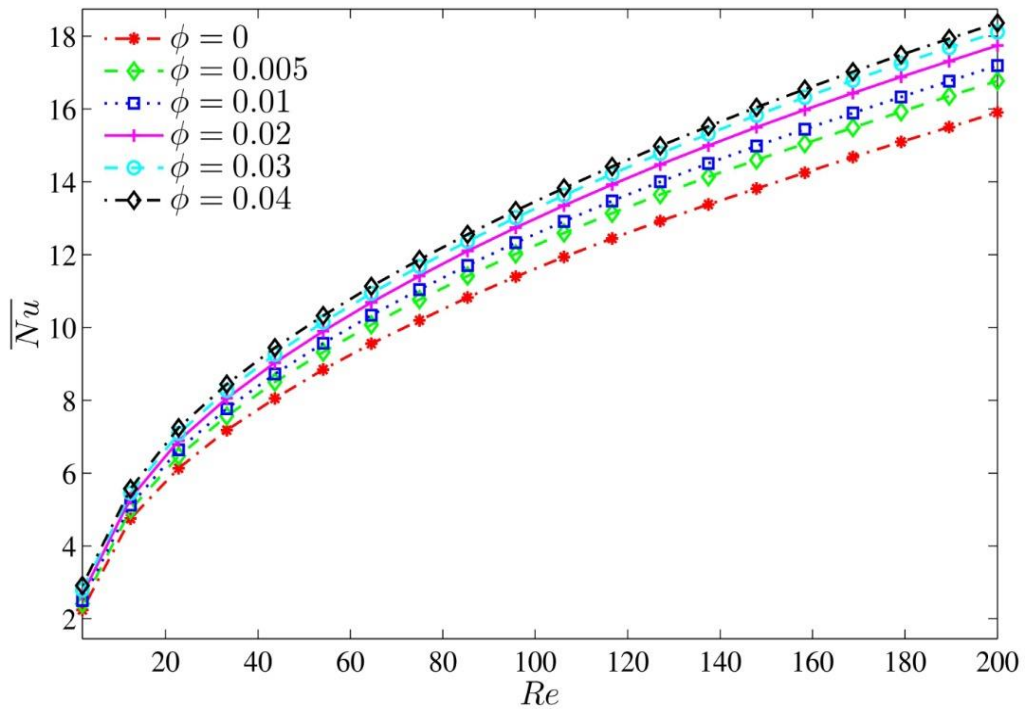


Fig. 6. Variations of the average Nusselt-number against Re for different ϕ

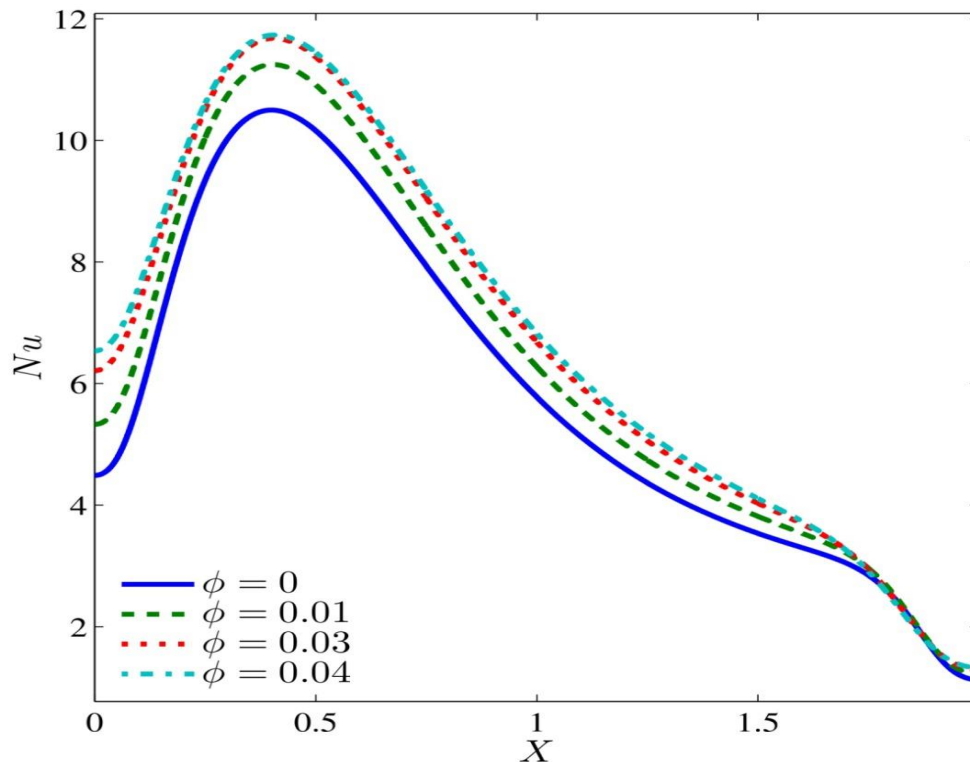


Fig. 7. Variations of the local Nusselt-number against X for different ϕ

6. Conclusions

The purpose of this study is to numerically study the mixed convection in a rectangle lid-driven cavity filled with hybrid nanofluid by employing the finite volume method. The walls on the left and right are fully isolated. The bottom horizontal wall is kept at a constant high temperature, while the top horizontal wall is kept at a stable low temperature and moves to the positive direction. The effects of Reynolds number Re and, solid volume fraction ϕ on the hybrid nanofluid flow and heat transfer behavior were discussed. The increase in the Reynolds number increases heat transfer. Heat transfer occurs higher in nanofluids in unlike pure water and is maximum in the case of Al_2O_3 -Cu-Water hybrid nanofluids. The increase in the volume fraction increases the heat transfer.

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