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Unsteady MHD Free Convection Flow of a Second Grade Casson Fluid with Ramped Wall Temperature

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ABSTRACT

The present study delves into the analysis of unsteady free convection flow involving a non-Newtonian Casson fluid adjacent to an infinitely tall vertical plate. The primary objective of this article is to examine the flow behaviour of a second-grade Casson fluid under varying critical parameters. The plate exhibits a gradual increase in wall temperature and is situated within a porous medium. The governing equations are transformed into a dimensionless form, using non dimensionless variables. The method of Laplace transform (MOLT) is employed to derive accurate solutions for the temperature and velocity within the flow field. To enhance comprehension of the issue, The impact of different physical parameters on the flow field has been examined through the utilization of graphs and tables. Outcome of the problem was compared with existing one which was in good agreement. The study revealed that the velocity magnitude was lower in the scenario with ramped temperature compared to the scenario with isothermal temperature. Finally, skin friction and Nusselt numbers of the present work are tabulated. The significant outcome of the present work is that the flow field for the present phenomena is same as that of the existing one in absence of radiation parameter and heat source parameter when $u(0,t)=0$, $\beta=\infty$.

1. Introduction

Natural convection heat transfer in between a vertical plate and a fluid is a well-studied topic as it has many engineering applications. Researchers have investigated diverse thermal boundary conditions at bounding plates, encompassing continuous and well-defined conditions, non-uniform and arbitrary wall conditions, as well as the impact of radiation and porosity. Some of the most notable studies include those by Raptis and Singh [1,2], Sacheti *et al.*, [3] Chandran *et al.*, [4,5], Ganesan and Palani [6], Fetecau *et al.*, [7,8], Chandran *et al.*, [9], Seth and Ansari [10], Seth *et al.*, [11], Narahari and Bég [12] and Samiulhaq *et al.*, [13]. These studies have led to the development of Closed-form solutions for the velocity and temperature fields under a variety of conditions. Although all of the aforementioned results refer to incompressible viscous fluids, there is still a need to study natural convection heat transfer in other types of fluids, such as non-Newtonian fluids. The

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importance of non-Newtonian fluids has been increased significantly in recent years, and numerous researchers have made significant contributions to the study of flow characteristics. Non-Newtonian fluids are essential to understand because they are used in a wide variety of applications, including plastics manufacturing, lubricants, food processing, and biological fluid dynamics.

Non-Newtonian fluids are fluids whose viscosity varies with the shear rate. This has led to the development of various models of non-Newtonian fluids. Within this category, analysing second-grade fluids is straightforward, allowing for effective modelling of various types of fluids like dilute polymer solutions, slurry flows, and industrial oils. Second-grade fluids offer a versatile approach for examining a diverse array of problems encompassing varying geometries and mechanical as well as thermal boundary conditions. For instance, an examination by Tan and Masuoka [14] delved into the flow of a second-grade fluid in a porous half-space near a heated flat plate. In a separate study, Hayat and Abbas [15] utilized the homotopy analysis method to scrutinize heat transfer in the magneto hydrodynamic (MHD) flow of second-grade fluids within porous media. Khan *et al.*, [16] derived a closed-form solution, Srinivasa *et al.*, [17] investigated thermal effects in Stoke's problem, and Mustafa *et al.*, [18] investigated the natural convection flow of second-grade fluids along a vertical plate, taking into account their viscoelastic properties. Within the realm of engineering, magneto-hydrodynamics (MHD) has been employed to produce electricity from ionized gas through the application of a magnetic field. The investigation of heat and mass transfer within magneto hydrodynamic (MHD) flows holds significance due to its numerous applications in both scientific research and technology. The utilization of heat and mass transfer principles in magneto hydrodynamic (MHD) flows extends to buoyancy-induced flows occurring in the atmosphere, bodies of water, and quasi-solid structures like the Earth. As a result, several researchers Katagiri [19], Jana *et al.*, [20], Mandal and Mandal [21], Ghosh [22], Jha and Apere [23], Krishna *et al.*, [24] have conducted research on heat and mass transfer in the context of magneto hydrodynamic (MHD) flow. Kataria and Mittal [25,26] explored the heat and mass transfer effects of various types of magnetohydrodynamic (MHD) nanofluids from different perspectives, Sheikholeslami *et al.*, [27], Krishna, and Chamkha [28] also investigated similar phenomena. Teh and Ashgar [29], along with Patel *et al.*, [30] conducted studies in this domain. Furthermore, Krishna and Chamkha [31] made a significant contribution to comprehending the impact of Hall and ion slip effects on the unsteady magnetohydrodynamic (MHD) convective rotating flow of nanofluids. Additionally, Krishna *et al.*, [32] delved into the Hall effects on the MHD peristaltic flow of Jeffrey fluid. Magnetic fields have a significant influence on a wide range of natural and technological phenomena. Magnetic fields are also used in a variety of technological applications, such as fast-breeder reactors, controlled thermonuclear fusion, and MHD power generation. To explore intriguing findings on second-grade fluids, one can refer to the citations [33-37]. The purpose of this analysis is to extend the work done by Samiulhaq *et al.*, [33] for Casson fluid flow with variable velocity, radiation and heat source included with ramped wall temperature. Moreover, exact solutions are derived for velocity and temperature for second grade Casson fluid flow by using powerful Laplace transformation method. The solutions obtained meet all the specified initial and boundary conditions.

2. Mathematical Representation of the Phenomenon

An investigation was conducted on the unsteady flow of a non-Newtonian fluid exhibiting Casson behaviour in the vicinity of an infinitely tall vertical plate under the influence of magnetohydrodynamics (MHD), with the added condition of the plate's temperature increasing linearly with time. The electrically conducting fluid flows through a porous medium. We define the x-axis as the upward direction along the plate, and the y-axis as the normal direction to the plane of

the plate. A uniform magnetic field with strength B_0 is applied perpendicular to the flow, as illustrated in Figure 1. At the initial time ($t=0$), both the fluid and the plate are stationary and maintained at a constant temperature. At a later time $t=t_0$, the temperature of the plate is either increased or decreased to $T_0 + (T_w - T_0) \frac{t}{t_0}$ for $t > t_0$, and it is maintained at this constant temperature T_w . The goal of this study is to investigate the natural convection flow of a Casson fluid, incorporating factors such as a heat source with variable velocity, radiation effects, and a temperature that varies with a ramped profile on the bounding plate.

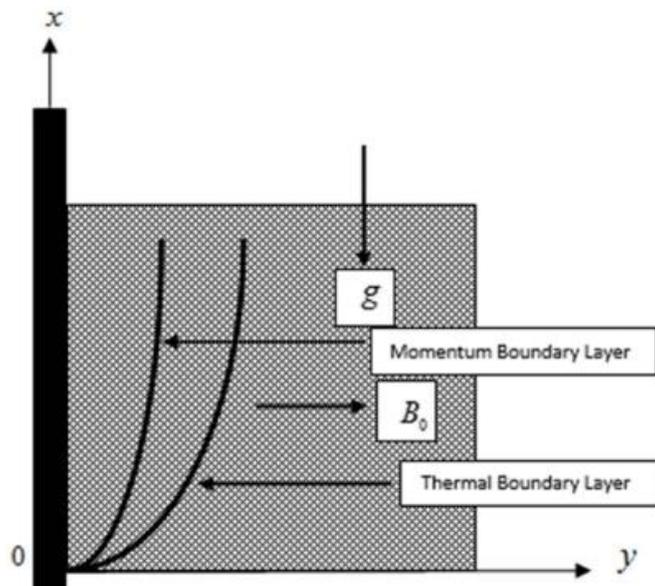


Fig. 1. Physical model of the phenomena

In the course of the analysis, the following assumptions were taken into consideration.

- (i) The impact of viscous dissipation on the energy equation is deemed insignificant.
- (ii) Lorentz force, which is given by $J \times B$, is the body force. B represents the strength of the magnetic field everywhere in space, while J represents the amount of current flowing through a given area.
- (iii) The current density can be calculated using Ohm's law, which states that $J = \sigma(E + V \times B)$, here, σ represents the electrical conductivity of the fluid, and E denotes the electric field.
- (iv) V is the velocity vector field, total magnetic field $B = B_0 + b_1$.
- (v) The magnetic field applied is denoted as B_0 , while the resulting induced magnetic field is represented as b_1 .
- (vi) The current density, J , is expressed under specific assumptions $E=0$, $b_1=0$ and $B=B_0=(0, B_0, 0)$. B_0 modified as $J = \sigma(V \times B_0)$.
- (vii) At last, the Lorentz force becomes $J \times B = -\sigma B_0^2 V$.

Under the Boussinesq approximation the equations governing the flow with reference to Krishna *et al.*, [24] are as follows:

$$\frac{\partial u}{\partial t} = \left[v \left(1 + \frac{1}{\beta} \right) + \frac{\alpha_1}{\rho} \frac{\partial}{\partial t} \right] \frac{\partial^2 u}{\partial y^2} + g\beta(T - T_\infty) - \frac{\sigma B_0^2 u}{\rho} - \frac{\varphi}{k_1} \left(v \left(1 + \frac{1}{\beta} \right) + \frac{\alpha_1}{\rho} \frac{\partial}{\partial t} \right) u(y, t) \quad (1)$$

$$\frac{\partial T}{\partial t} = \frac{k}{\rho c_p} \frac{\partial^2 T}{\partial y^2} - \frac{1}{\rho c_p} \frac{\partial q_r}{\partial y} - \frac{Q}{(T-T_\infty)\rho c_p} \quad (2)$$

Here u is the velocity of the flow in x direction, T is its temperature, ρ is the density of the fluid, g is gravitational force, β is Casson parameter, ν is kinematic viscosity, ϕ is the porosity of the medium, k is permeability, κ is the thermal conductivity, c_p is specific heat at the constant pressure, and α_1 is the material module of second grade fluid. In reference to Samiulhaq *et al.*, [33] the pertinent initial and boundary conditions are outlined below:

$$u^*[y,0]=0, T^*[y,0]=T_\infty, y \geq 0, u^*[0,t]=\frac{t^* t_0 \sqrt{t_0}}{\nu}, t > 0$$

$$T^*[0,t]=T_\infty + (T_w - T_\infty) \frac{t}{t_0}, \text{ for } 0 < t < t_0 \quad (3)$$

$$T^*[0,t]=T_w^* \text{ for } t > t_0$$

$$u^*[y,t] \rightarrow 0 \text{ as } y \rightarrow \infty, T^*[y,t] \rightarrow 0 \text{ as } y^* \rightarrow \infty \text{ and } t \geq 0$$

Introducing the subsequent dimensionless parameters

$$y^* = \frac{y}{\sqrt{\nu t_0}}, t^* = \frac{t}{t_0}, u^* = u \sqrt{\frac{t_0}{\nu}}, \theta = \frac{T^* - T_\infty}{T_w - T_\infty}, Pr = \frac{\mu c_p}{\kappa} = \frac{\nu \rho c_p}{\kappa}$$

$$\alpha = \frac{\alpha_1}{\mu t_0}, M^2 = \frac{\sigma B_0^2 t_0}{\rho}, \frac{1}{k} = \frac{\nu f}{\kappa_1} t_0 \quad (4)$$

$$t_0 = \left[\frac{\sqrt{\nu}}{g\beta(T_w^* - T_\infty)} \right]^{\frac{2}{3}}, q_r = \frac{-4\sigma}{3\kappa_1} \frac{\partial T^{*4}}{\partial y}, Q^* = \frac{Q}{(T - T_\infty)\rho c_p}, \text{ into Eq. (1) and Eq. (2) and dropping } *$$

transformed equations are

$$\left(1 + \frac{1}{\beta}\right) \frac{\partial^2 u}{\partial y^2} + \alpha \frac{\partial^3 u}{\partial t \partial y^2} - \left(1 + \frac{\alpha}{k}\right) \frac{\partial u}{\partial t} - \left(M^2 + \frac{1 + \frac{1}{\beta}}{k}\right) u + \theta = 0 \quad (5)$$

$$\frac{\partial \theta}{\partial t} = \left(\frac{1+R}{Pr}\right) \frac{\partial^2 \theta}{\partial y^2} - Q\theta \quad (6)$$

The transmuted boundary conditions are

$$u[y,0]=0, \theta[y,0]=0, y \geq 0$$

$$u[0,t]=t \quad t > 0$$

$$\theta[0,t]=\begin{cases} t & 0 < t < 1 \\ 1 & t \geq 1 \end{cases} \quad (7)$$

$$u[y,t] \rightarrow 0, \theta[y,t] \rightarrow 0 \quad \text{as } y \rightarrow \infty \quad t \geq 0$$

3. Methodology (Laplace Transform Method)

By applying the Laplace transform to coupled partial differential equations (PDEs) (5) and (6) with respect to the boundary conditions (7), analytical expressions have been derived. These expressions yield the Laplace velocity and temperature equations.

$$(A+\alpha s) \frac{d^2 u}{dy^2} - (Bs+C)u + \theta = 0 \quad (8)$$

$$\frac{d^2 \theta}{dy^2} - E(s+Q)\theta = 0 \quad (9)$$

The corresponding Laplace initial and boundary conditions are determined by

$$u[y,0]=0, \theta[y,0]=0, y \geq 0$$

$$u[0,s]=s^{-2}, \theta[0,s]=\frac{1-e^{-s}}{s^2} \quad (10)$$

$$u[y,s] \rightarrow 0, \theta[y,s] \rightarrow 0 \quad \text{as } y \rightarrow \infty$$

The formulations for Laplace velocity and temperature are presented as follows:

$$u(y,s) = \left[\frac{1}{s^2} - \frac{1}{s^2(s-I_1)(s-I_2)} \frac{1-e^{-s}}{e^s} \right] e^{-y\sqrt{\frac{Bs+C}{\alpha s+A}}} + \frac{1-e^{-s}}{s^2(s-I_1)(s-I_2)} e^{-y\sqrt{E}\sqrt{s+Q}} \quad (11)$$

$$\theta(y,s) = \left(1 - \frac{1}{e^s} \right) s^{-2} e^{-y\sqrt{E}\sqrt{s+Q}} \quad (12)$$

Utilizing the inverse Laplace transform to solve the Eq. (11) and Eq. (12) the corresponding velocity and temperature expressions describing the flow are as follows.

$$u(y,t) = \frac{1}{2} \left[\left(t - \frac{yk_3}{2\sqrt{k_1}} \right) e^{-yk_3\sqrt{k_1}t} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} - \sqrt{k_1}t \right) + \left(t + \frac{yk_3}{2\sqrt{k_1}} \right) e^{-yk_3\sqrt{k_1}t} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} + \sqrt{k_1}t \right) \right]$$

$$\begin{aligned}
 & -J \left[\frac{1}{2} \left\{ e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} - \sqrt{k_1 t} \right) + e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} + \sqrt{k_1 t} \right) \right\} \right. \\
 & - \frac{1}{2} \left\{ e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} - \sqrt{k_1(t-1)} \right) + e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} + \sqrt{k_1(t-1)} \right) \right\} H(t-1) \left. \right] \\
 & -K \left[\frac{1}{2} \left\{ \left(t - \frac{yk_3}{2\sqrt{k_1}} \right) e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} - \sqrt{k_1 t} \right) + \left(t + \frac{yk_3}{2\sqrt{k_1}} \right) e^{yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} + \sqrt{k_1 t} \right) \right\} \right. \\
 & - \frac{1}{2} \left\{ \left(t-1 - \frac{yk_3}{2\sqrt{k_1}} \right) e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} - \sqrt{k_1(t-1)} \right) + \left(t-1 + \frac{yk_3}{2\sqrt{k_1}} \right) e^{yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} + \sqrt{k_1(t-1)} \right) \right\} H(t-1) \left. \right] \\
 & -L \left[\frac{1}{2} \left\{ e^{I_1 t - yk_3\sqrt{k_4}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} - \sqrt{k_4 t} \right) + e^{I_1 t + yk_3\sqrt{k_4}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} + \sqrt{k_4 t} \right) \right\} \right. \\
 & - \frac{1}{2} \left\{ e^{I_1(t-1) - yk_3\sqrt{k_4}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} - \sqrt{k_4(t-1)} \right) + e^{I_1(t-1) + yk_3\sqrt{k_4}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} + \sqrt{k_4(t-1)} \right) \right\} \left. \right] \\
 & +L \left[\frac{1}{2} \left\{ e^{I_2 t - yk_3\sqrt{k_5}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} - \sqrt{k_5 t} \right) + e^{I_2 t + yk_3\sqrt{k_5}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t}} + \sqrt{k_5 t} \right) \right\} \right. \tag{13} \\
 & - \frac{1}{2} \left\{ e^{I_2(t-1) - yk_3\sqrt{k_5}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} - \sqrt{k_5(t-1)} \right) + e^{I_2(t-1) + yk_3\sqrt{k_5}} \operatorname{erfc} \left(\frac{yk_3}{2\sqrt{t-1}} + \sqrt{k_5(t-1)} \right) \right\} H(t-1) \left. \right] \\
 & +J \left[\frac{1}{2} \left\{ e^{-y\sqrt{EQ}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} - \sqrt{Qt} \right) + e^{y\sqrt{EQ}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} + \sqrt{Qt} \right) \right\} \right. \\
 & - \frac{1}{2} \left\{ e^{-y\sqrt{EQ}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} - \sqrt{Q(t-1)} \right) + e^{y\sqrt{EQ}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} + \sqrt{Q(t-1)} \right) \right\} H(t-1) \left. \right] \\
 & +K \left[\frac{1}{2} \left\{ \left(t - \frac{y\sqrt{E}}{2\sqrt{Q}} \right) e^{-y\sqrt{EQ}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} - \sqrt{Qt} \right) + \left(t + \frac{y\sqrt{E}}{2\sqrt{Q}} \right) e^{-y\sqrt{EQ}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} + \sqrt{Qt} \right) \right\} \right.
 \end{aligned}$$

$$\begin{aligned}
 & -\frac{1}{2} \left[\left(t-1 - \frac{y\sqrt{E}}{2\sqrt{Q}} \right) e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2(t-1)^{\frac{1}{2}}} - \sqrt{k_1(1-t)} \right) + \left(t-1 + \frac{y\sqrt{E}}{2\sqrt{Q}} \right) e^{-yk_3\sqrt{k_1}} \operatorname{erfc} \left(\frac{yk_3}{2}(t-1)^{-\frac{1}{2}} + (k_1(t-1))^{\frac{1}{2}} \right) \right] H(t-1) \\
 & +L \left[\frac{1}{2} \left\{ e^{-y\sqrt{E}\sqrt{k_6}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} - \sqrt{k_6t} \right) + e^{y\sqrt{E}\sqrt{k_6}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} + \sqrt{k_6t} \right) \right\} \right. \\
 & -\frac{1}{2} \left\{ e^{-y\sqrt{E}\sqrt{k_6}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} - \sqrt{k_6(t-1)} \right) + e^{y\sqrt{E}\sqrt{k_6}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} + \sqrt{k_6(t-1)} \right) \right\} H(t-1) \\
 & -L \left[\frac{1}{2} \left\{ e^{-y\sqrt{E}\sqrt{k_7}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} - \sqrt{k_7t} \right) + e^{y\sqrt{E}\sqrt{k_7}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} + \sqrt{k_7t} \right) \right\} \right. \\
 & \left. -\frac{1}{2} \left\{ e^{-y\sqrt{E}\sqrt{k_7}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} - \sqrt{k_6t} \right) + e^{y\sqrt{E}\sqrt{k_6}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} + \sqrt{k_6t} \right) \right\} \right] \\
 & -\frac{1}{2} \left\{ e^{-y\sqrt{E}\sqrt{k_7}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} - \sqrt{k_7(t-1)} \right) + e^{y\sqrt{E}\sqrt{k_7}} \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} + \sqrt{k_7(t-1)} \right) \right\} H(t-1) \\
 & \theta(y,t) = \frac{1}{2} \left[\left(t - \frac{y\sqrt{E}}{2\sqrt{Q}} \right) \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} - \sqrt{Qt} \right) + \left(t + \frac{y\sqrt{E}}{2\sqrt{Q}} \right) \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t}} + \sqrt{Qt} \right) \right] \tag{14} \\
 & -\frac{1}{2} \left[\left(t-1 - \frac{y\sqrt{E}}{2\sqrt{Q}} \right) \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} - \sqrt{Q(t-1)} \right) + \left(t-1 + \frac{y\sqrt{E}}{2\sqrt{Q}} \right) \operatorname{erfc} \left(\frac{y\sqrt{E}}{2\sqrt{t-1}} + \sqrt{Q(t-1)} \right) \right]
 \end{aligned}$$

4. Discussion on Findings

To gain a better understanding of the current problem The velocity, denoted as $u [y, t]$, and temperature, denoted as $T [y, t]$, are graphically represented for various y values. The impact of various critical parameters on the velocity and temperature fields of the flow phenomenon is described and visually presented. Elevating the Casson parameter results in an augmented viscosity. High viscosity lowers the fluid velocity. This was depicted in Figure 2. In Figure 3, velocity profiles corresponding to varying permeability parameters are displayed. As the values of k increase, the boundary layer density also rises. Due to this the opposing nature of penetrable medium is negligible which causes rise in velocity of the fluid. In Figure 4, the influence of the second-grade parameter on the flow velocity is depicted. Increase in second grade parameter decreases the boundary layer thickness that results in decrease of the fluid flow. The interaction between induced currents and the magnetic field produces a resistive force that opposes the flow of the fluid. This was shown in Figure 5. A heat source outside of a flow field adds heat to the fluid, which increases the temperature and velocity of the flow. Both the facts are displayed in Figure 6 and Figure 10. When thermal radiation increases in a fluid medium, the kinetic energy of the fluid particles decreases. This leads to a

corresponding decrease in fluid velocity, as shown in Figure 7. The influence of the Prandtl number is illustrated in Figure 8. The Prandtl number is the ratio of kinematic viscosity to thermal diffusivity. With an increase in the Prandtl number, heat transfer efficiency decreases, and the viscosity of the fluid also rises. This results in an increase in the viscosity of the fluid. An increase in fluid viscosity results in a decrease in flow velocity. Figure 9 shows temperature profiles for different values of Prandtl number. As the Prandtl number increases, the thermal conductivity of the fluid decreases, resulting in a decrease in fluid temperature. Figure 11 shows how the radiation parameter affects the temperature field of the flow. Elevating the radiation parameter results in a higher temperature of the fluid. This is likely due to the increase in the radiation variable, leading to a thicker thermal boundary layer. From Figure 12, it is evident that the flow velocity is greater in the case of an isothermal temperature compared to a ramped temperature. The boundary layer is consistently thinner under a ramped temperature condition compared to an isothermal temperature scenario. This is attributed to the steeper temperature gradient induced by the ramped temperature profile, promoting enhanced heat transfer and thereby minimizing the boundary layer thickness.

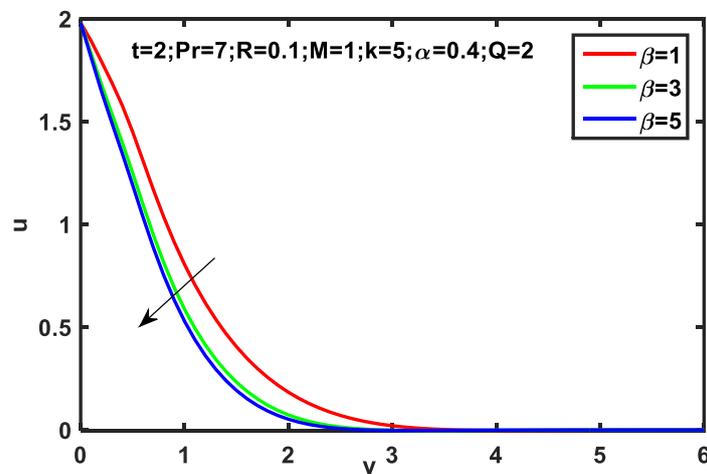


Fig. 2. Influence of Casson parameter on velocity field

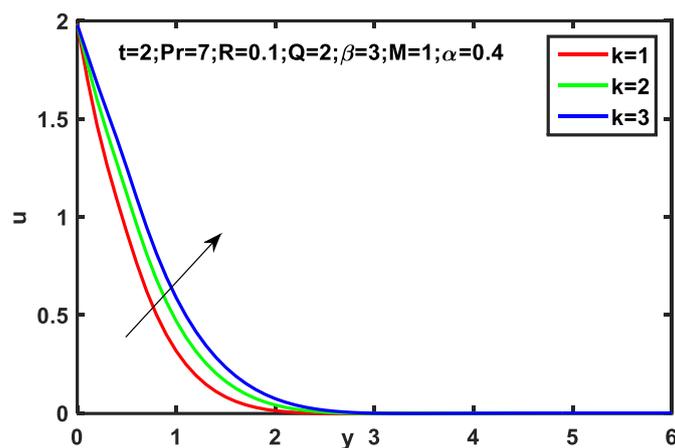


Fig. 3. Velocity Field Variation with Respect to Permeability Parameter

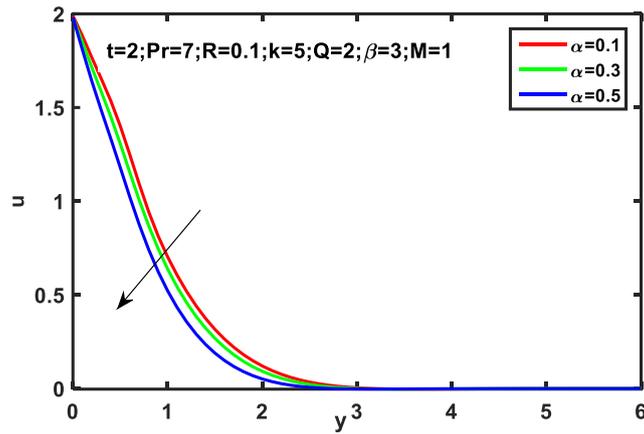


Fig. 4. Impact of second grade parameter on velocity field

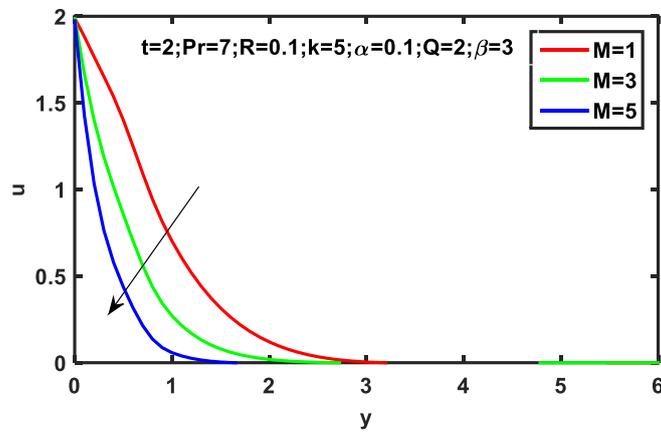


Fig. 5. Variations in velocity field under the Influence of Magnetic parameter

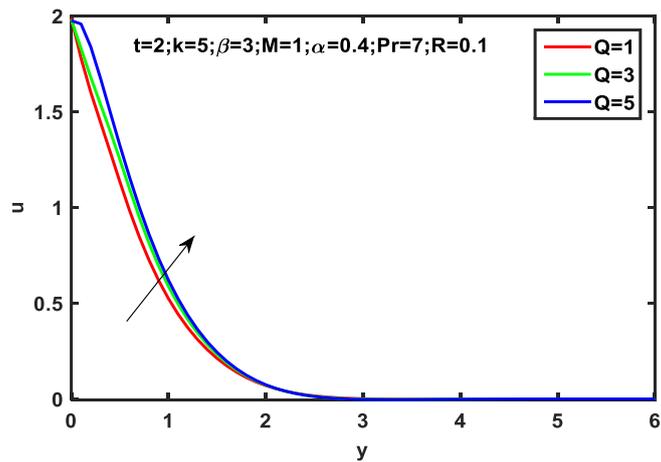


Fig. 6. Result of velocity field with reference to Heat source parameter

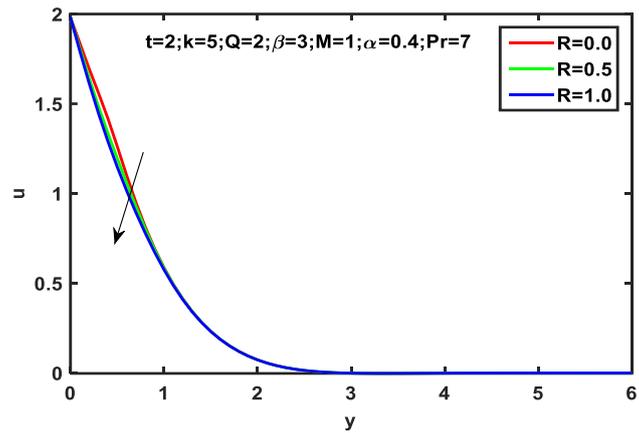


Fig. 7. Impact of the Radiation Parameter on Velocity Distribution

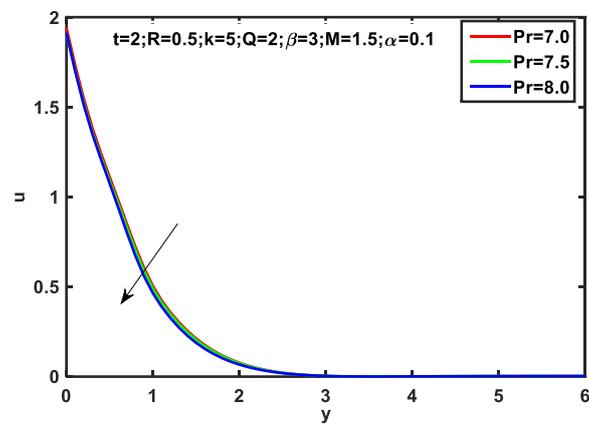


Fig. 8. Influence of the Prandtl parameter on the velocity distribution

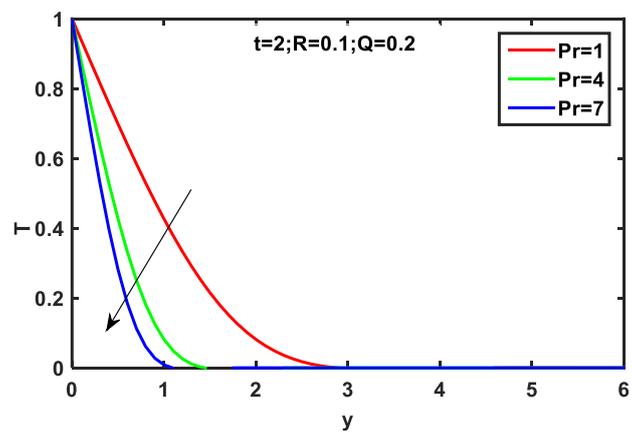


Fig. 9. Effect of the Prandtl parameter on the temperature distribution

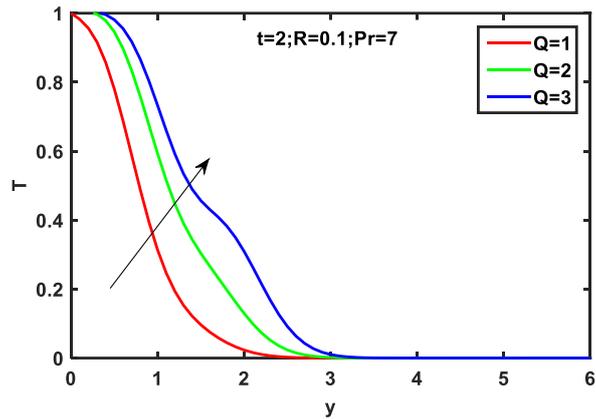


Fig. 10. Impact of the heat source parameter on the temperature distribution

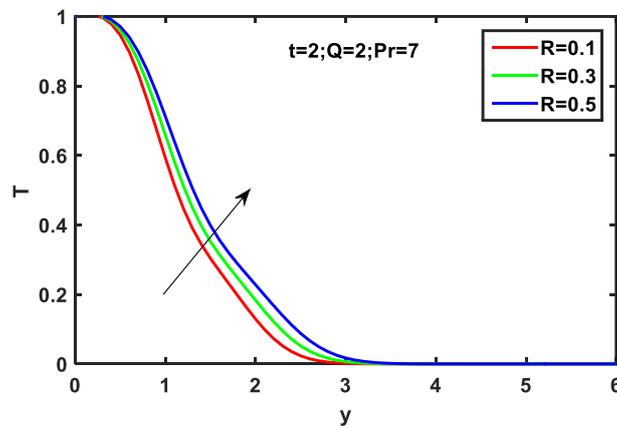


Fig. 11. Influence of Radiation parameter on temperature field

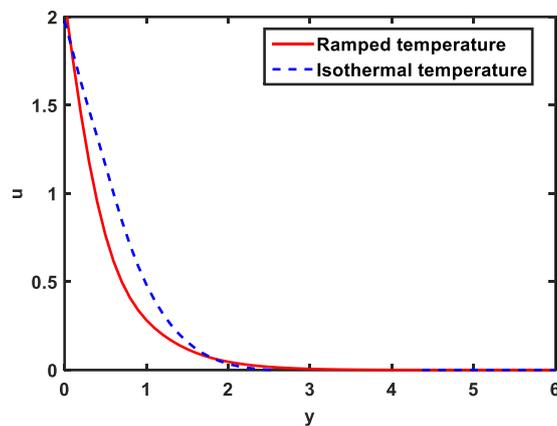


Fig. 12. The impact of ramped and isothermal temperatures on the velocity field

5. Skin Friction and Nusselt Number

Skin friction pertains to the resistance generated by friction between a fluid and the surrounding surface. It holds significance in the context of water-bed boundary conditions, because frictional forces can cause sediment particles to erode from the bed.

$$\text{Skin friction } (s_f) = \mu \left. \frac{\partial u}{\partial y} \right|_{y=0} + \alpha \left. \frac{\partial^2 u}{\partial t \partial y} \right|_{y=0} .$$

The Nusselt number is a nondimensional parameter that quantifies the rate of heat transfer by convection relative to the rate of heat transfer by conduction under the same conditions.

$$\text{Nusselt number } (Nu) = - \left. \frac{\partial T}{\partial y} \right|_{y=0}$$

Table 1 and Table 2 display the changes in skin friction and Nusselt number concerning distinct physical parameters.

Table 1
 Skin friction for different values of M , β , α , k and Q when $Pr=7$, $R=0.1$, $t=1.2$

M	β	α	k	Q	sf
2.1					1.4503
2.2					1.8225
2.3					2.2012
	1				1.4503
	2				2.1701
	3				2.3399
		0.1			1.4503
		0.2			3.2178
		0.3			4.4246
			5		1.4503
			6		1.3884
			7		1.3441
				1	3.9937
				2	1.8225
				3	0.3447

Table 2
 Nusselt number for different values
 $t=2$, $Pr=7$, $Q=1$, $R=0.1$

Pr	Q	R	t	Nu
7				0.1023
8				0.1169
9				0.1315
	1			0.1023
	2			0.0410
	3			0.0336
		0.1		0.1023
		0.2		0.0937
		0.3		0.0865

6. Conclusions

A second grade Casson fluid flow phenomena was studied under the influence of different physical parameters. The governing partial differential equations are made dimensionless. Exact solutions are derived for Flow velocity and temperature by applying the method of Laplace transforms (MOLT). Graphical analysis was performed to examine the non-uniform distribution of velocity and temperature within the flow influenced by varying critical parameters. The disparity in tables displaying skin friction and Nusselt number corresponding to various physical parameters are presented. During the analysis the following conclusions were drawn

- (i) Increase of Permeability parameter and heat source parameter increases the speed of the fluid flow, whereas increase of Casson parameter, second grade fluid parameter, Magnetic parameter, Prandtl number, Radiation parameter decreases the same.
- (ii) An increase in Prandtl number decreases the temperature of the flow field, while an increase in heat source and radiation parameter increases the temperature of the flow field. It is noticed that the velocity of the flow field with ramped temperature lower than that of isothermal temperature.
- (iii) In the present problem boundary condition at wall was taken as $u(0,t)=t$, where as Samiulhaq *et al.*, [33] taken as $u(0,t)=0$.
- (iv) To verify the accuracy of the flow field solution presented in this article, results are compared to existing solutions using graphs. Figure 13 depicts the disparity in velocity fields of existing problem with that of Samiulhaq *et al.*, [33]. Figure 14 depicts that velocity profiles of Present work and Samiulhaq *et al.*, [33] are coincided when the boundary condition $u(0,t)=t$ replaced with $u(0,t)=0$ taking $R=0, \beta=\infty$ and $Q=0$.
- (v) Table 3 describes the nature of the flow phenomena for different values of y and t . It can be noticed that velocity of the flow converges to zero far away from the plate

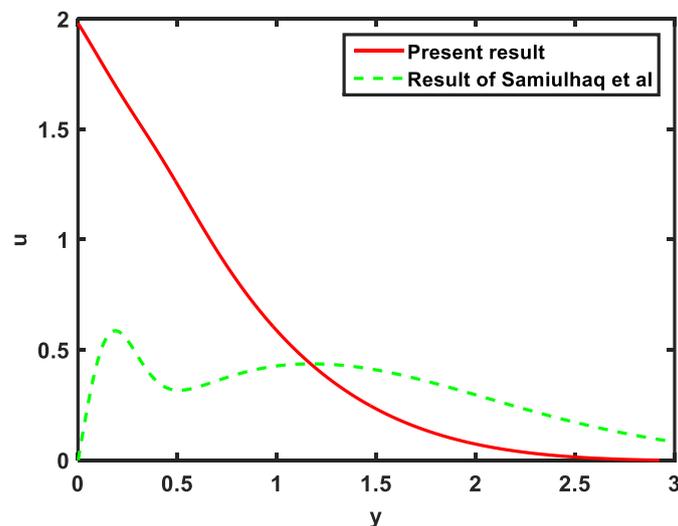


Fig. 13. Comparison of existing results of velocity field with Samiulhaq *et al.*, [33]

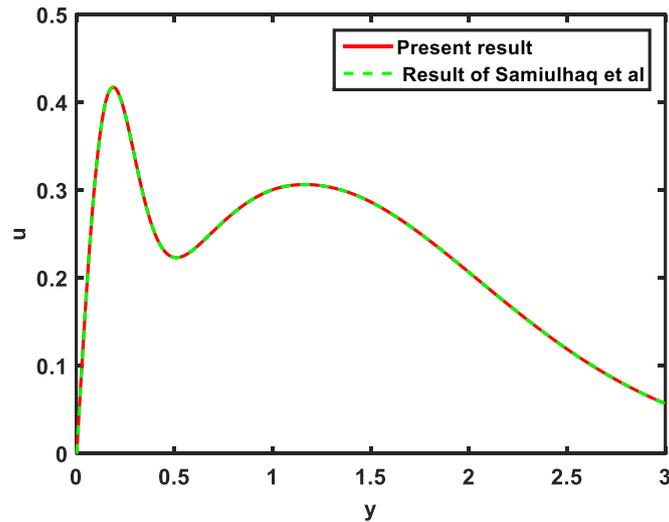


Fig. 14. Comparison of existing results of velocity field with Samiulhaq *et al.*, [33]

Table 3
 Velocity distribution for various values of y and t

y	$t=1.5$	$t=2.0$	$t=2.5$	$t=3.5$
0.0	1.5	2.0	2.5	3.5
0.5	1.0	1.4	1.7	2.3
1.0	0.3	0.7	0.9	1.3
1.5	0.0	0.3	0.4	0.7
2.0	0.0	0.1	0.2	0.3
2.5	0.0	0.0	0.0	0.1
3.0	0.0	0.0	0.0	0.0

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