



Assessment and Prediction of Heat Transfer Performance of Oscillating Heat Pipe using Acetone

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ABSTRACT

Heat pipe is a device to enhance the performance of heat transfer, in particular to transition phase change process. The present investigation is carried out to measure the thermal performance of a closed loop acetone filled oscillating heat pipe with four turns is fabricated and tested. The test was carried out for the inner diameter of 1.7 mm copper tube by varying the acetone of 50%, 60%, 70% and 80% filler ratio with a heat input of 15 W to 40 W in steps of 5 W has been considered. The results shows that 80% acetone filled OHP provides the better thermal performance with an average minimum temperature difference between condenser and evaporator by 6.03%, heat transfer coefficient increased by 77% and the thermal resistance decrease by 43% respectively. The mathematical modelling was developed to predict the performance of the heat transfer. The model clearly shows that the independent variables are statistically significant with a p-value of 0.05 and the uncertainty analysis between the experimental and predicted values are less than 10%.

1. Introduction

In heat pipes, pulsating heat pipe was the promising device for the heat transportation in heat transfer unit. Therefore, micro-grooved OHP is one of the effective modes to evaluate the performance heat transfer of the system. This device would enhance the allowable input heat flux by condensate the backflow to the evaporator when the filling ratio ranging from 30% to 60% [1]. Due to increase in filling ratio, heat added to the evaporator section leads to increase in temperature and pressure during the flow process. Therefore, filler ratio was the major part to increase the heat input for the oscillation motion of the working fluid [2]. To heat the oscillating pipe many methods was applied in the evaporator section. There was a pulsed supply with regulated current method was used to heat the system. This method generates a large amplitude oscillation to heat up for a short period of time [3]. To increase the heat transfer mechanisms of oscillating pipe a mathematical model

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was developed by considering spring mass system to for an annular flow with a slug causing of penetrate liquid. This flow trains the liquid by disappearing the vapour bubbles by creating the pulsating effect of the liquid [4]. For the performance improvement of oscillating pipe mixing of self-wetting fluids and nano-fluids was developed. To determine the high performance of the OHP optimum concentration of the nanoparticles (16%) and self-wetting (12%) was used [5]. In case of hybrid flexile oscillating heat pipe at the adiabatic section at the heating and cooling side, a micro grooved copper tube was designed and fabricated. This structural design creates a deformation of adiabatic section and exhibits a spatial flexibility to improve the heat transfer performance of the new design [6]. If the filler ratio was 40% to 80% in case of self-wetting fluid can ensure a higher heating load compare to water or ethanol as a working medium with a filler ratio of 30% [7]. Multilayer OHP was also employed for the measurement of heat transfer rate and it was effectively work for all the working fluids [8]. To evaluate the characteristics of the working fluids micro OHP was used with trapezoidal channels. Two different start-up behaviours were used such as start-up with and without bubble nucleation. Comparison was made and finally, concluded that start-up with bubble nucleation was the better than that of without bubble nucleation [9]. To measure performance of the start-up mechanism filler ratio, heat input, working fluids are the major concern in evaluation process. Finally, in case of acetone filled OHP had a higher thermal performance compare to the water filled OHP at 60 and 300 W [10]. Whereas in multilayer OHP system, two kinds of novel 3D-OHPs coupled with 2D-OHPs were used by using phase change materials (paraffin wax) for the thermal management. The solidification of paraffin wax with 4 layers OHPs was 0.48 times greater than that of pre paraffin wax with 3 layers [11]. Whereas in case of ferrite ferro-nano-fluids with OHP operation had a high heat transfer and extreme temperature functionality for the applications can be used [12]. In sintered copper-form wicks OHP with an ethanol as a working fluid with 50% of volumetric filling ratio. These combinations profound improvement in the FPOHP performance and there was a reduction in start-up temperature [13].

A novel method of directive absorptive nano-fluids in the OHP was introduced. It was noticed that an effective capture of solar energy and transport it simultaneously without any external pumping power is required [14]. A novel periodic expansion for condenser was proposed to evaluate the performance of thermo-hydrodynamic with phase change process. The result reveals that the thermal efficiency was increased by 45% at the expansion condenser [15]. In high-temperature liquid metal oscillating heat pipe with sodium-potassium alloy was used as a working fluid. With a filling ratio of 45% at different input power, study reviled that at 3169 W there was a minimum thermal resistance of $0.08^{\circ}\text{C}/\text{W}$ was achieved [16]. OHP-LiCl solution was investigated there was a reduction in thermal resistance of 62%. In case of low filling ratio of 45% of LiC solution it reduces the temperature at evaporator section [17]. The flat plate OHP with dual-serpentine-channel was designed and determines the OHP thermal performance. The start-up temperature was increased slowly and it reaches the approximately 41 to 46°C . The overall thermal conductivity was increased by 5.8 times compare to the existing setup [18]. To reduce the negative effects a multiple heat source was implemented and finally, developed minimum thermal resistance was achieved than compare to the Al6063 Alloy [19]. For all the working fluids the rate of increase in heat transfer was 10%, to evaluate this heat exchanger at the model was developed and model was agreed very well with the experimental data [20]. The thermal performance of OHP with ionic liquids was investigated the heat transfer performance showed a slight decrease of 10% for 220W [21-25].

According to the about mentioned reports, behaviour of nano-fluids, thermal performance of the novel setup, development of new fluids with OHP was determined. But comparative statements were not been carried out with the existing results. Therefore, optimum combinations of the nano-fluids with OHP need to be evaluated for the better understating of the combined Li effect of nano-fluids. In

the present investigations, prediction of acetone for the close loop OHP with a filler ration of 50% to 80%. Results were drawn based on the observations and finally, predictive equations were developed for the evaluation of performance prediction models.

2. Methodology

Experiments was conducted by using a newly fabricated oscillating heat pipe setup consists of copper tubes, glass tube, silicon rubber tube, mica heater, condenser, K-type thermocouple, glass wool, data acquisition system, and heat control unit respectively. Acetone with four turns oscillating heat pipe was used to determine the thermal performance of the OHP system [25-30]. The physical and thermodynamic properties of Acetone (working fluid) is tabulated in Table 1. To evaluate the thermal performance filler ratio of 50%, 60%, 70% and 80%) and heat input of 30 W, 35 W and 40 W were considered as an input to the OHP. The required amount of working fluid is filled through a syringe by opening one end the silicon rubber tube and the rubber tube is closed and ensured for leakage proof. After performing the leakage proof thermocouples display was checked, Mica heater plate was connected to the power controller by adjusting the suitable heat input to maintain the steady state temperature. If once the pulsation of the liquid begins and the reading has been taken until flow reaches steady state. Once the actual reading for a particular heat input is reached, the system is kept for cooling the temperature of the copper pipes and the glass tube is monitored in the system. Once the pulsations of the liquid are stopped the procedure repeats the heater plate is adjusted to the suitable heat input and the readings are tabulated. The overall oscillating heat pipe setup is shown in Figure 1.



Fig. 1. Experimental setup

Table 1

The physical and thermodynamic properties of Acetone

Working Fluid	Boiling Point (°C)	Melting Point (Solid state) (°C)	Useful Temp. Range (°C)	Specific Heat, C_p (J/Kg-K)
Acetone	57	-95	0-120	2031

3. Results and Discussion

Heat transfer performance of the OHP with acetone was determined by considering filler ratio of 50% to 80% and heat input of 15W, 20W, 25W, 30W, 35W and 40W was considered. The difference in temperature of evaporator and condenser section temperatures with heat input is studied at steady state condition [26-30]. The obtained results indicated that higher fill ratio of working fluid shows the better results in terms of reduction in difference in temperature, increased heat transfer coefficient across the evaporator and condenser. Based on the experimental investigations the change in temperature, heat transfer coefficient and thermal resistance was measured. Finally, experimental result was validated by using statistical analysis. Based on uncertainty analysis, measured and predicted values were explained in details for the better understanding of the developed OHP [31-35].

3.1 Temperature Variation for Acetone

For all the filler ratio of 50% to 80% by varying the heat input of 15W to 40W was noted down. Oscillations is depended on the thermal properties of the filled fluid and the heat input. At the heat input of 15W there was no oscillations up to 1850 seconds was observed as shown in Figure 4(a), whereas in case of 20 W, 25 W, 30 W, 35 W and 40 W with a filler ration of 50% was observed at 1650s, 1250s, 800s, 700s and 550s respectively. At the filler ratio of 70% with a heat input of 30W and 35W, there was not much different in temperature was achieved at 800s. The average increase in temperature for 50%, 60%, 70% and 80% were 7.02°C, 6.38°C, 6.79°C and 6.03°C respectively. Therefore, there was a minimum temperature different was measured for 80% filler ratio at 40W heat input [32-35]. Similar results were reported elsewhere [36-38]. The variation of temperature with different filler ratio of acetone with increase in heat input for all the combinations is shown in Figure 2(a) to Figure 2(f). Similarly, average temperature difference (T_e-T_c) with heat input is shown in Figure 3.

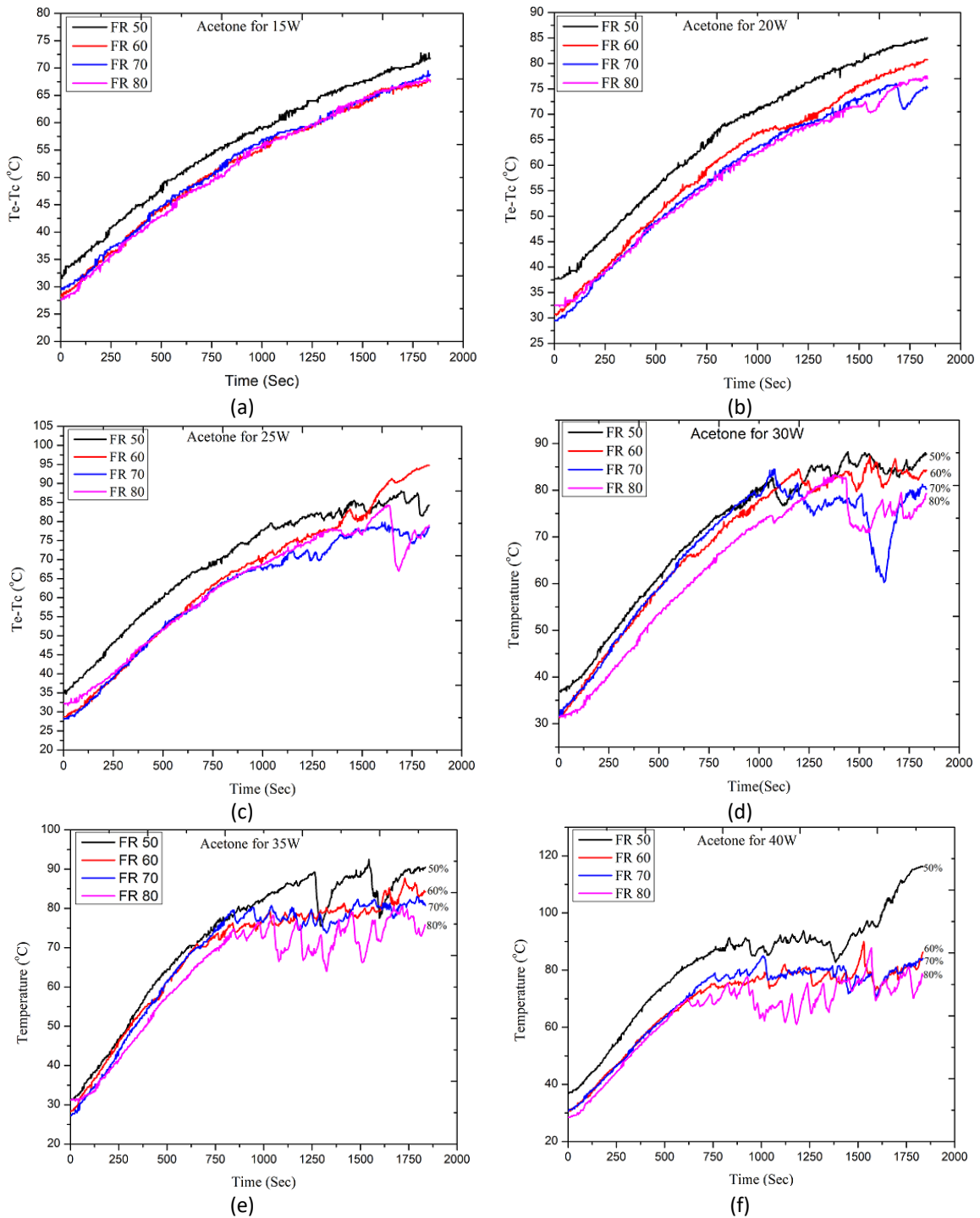


Fig. 2. Temperature variation for acetone filled at different heat input: (a) 15W, (b) 20W, (c) 25W, (d) 30W, (e) 35W and (f) 40W

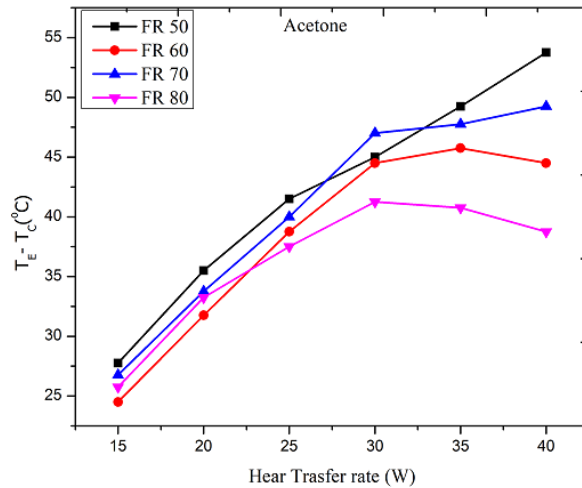


Fig. 3. Average temperature difference (T_e-T_c) with heat input for different filler ratio

3.2 Performance of Heat Transfer Coefficient with Acetone

Based on the different heat input with filter ratio combinations considered heat transfer rate is determined. Figure 4 illustrates the heat transfer coefficient and heat input for different filler ratio. For the developed OHP system with acetone at 50% filler ratio the increase in heat transfer coefficient of 37%. Whereas in case of 80% filler ratio it was 77% increase in heat transfer coefficient with a heat input of 40 W. Therefore, as the filler ratio increases, there is an increase in heat transfer coefficient because of high convective heat transfer coefficient as the filler ratio increases. Convective heat transfer co-efficient is given by:

$$h = \frac{Q}{A(T_E - T_C)} \frac{W}{m^2 C} \quad (1)$$

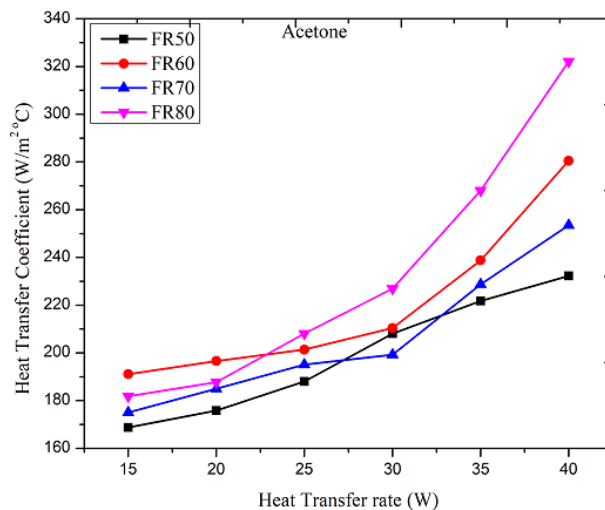


Fig. 4. Average heat transfer coefficient with heat transfer rate for different filler ratio

3.3 Performance of Thermal Resistance with Acetone

Figure 5 illustrate that the thermal resistance and heat input for different filler ratio of OHP is drawn. The experiments were conducted for three times to ensure the accuracy of the new equipment and experimentations. It can be seen that the filler ratio of 80% there is a decrease thermal resistance by 43% than compare to 50% filler ratio with a heat input of 40W. This is because as the volume increases by 80% there was a better heat transfer can be achieved come to the 50%. The Thermal Resistance R is given by:

$$R = \frac{TE-TC}{Q} \text{ } ^\circ\text{C/W} \tag{2}$$

Therefore, there is a decrease in thermal resistance with increase in filler ratio for the higher heat input of 40W is shown in Figure 5.

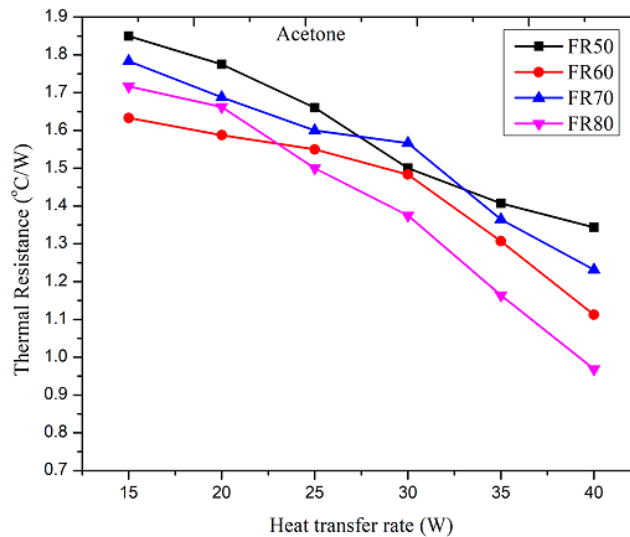


Fig. 5. Average thermal resistance with heat transfer rate for different filler ratio

3.4 Normal Probability Analysis

To observe the normality of the experimental data sets, Kolmogorov test was used to perform the probability value. This test is clearly shows that the observed values for T_e-T_c , heat transfer coefficient and thermal resistance data sets are normally distributed on 45° line with a μ values are 39.34, 214.34, 1.492 and σ values are 8.12, 37.25, 0.226 as represented in the Figure 6, Figure 7 and Figure 8 respectively. Hence the data recorded form the developed setup is reasonably good with acceptable range.

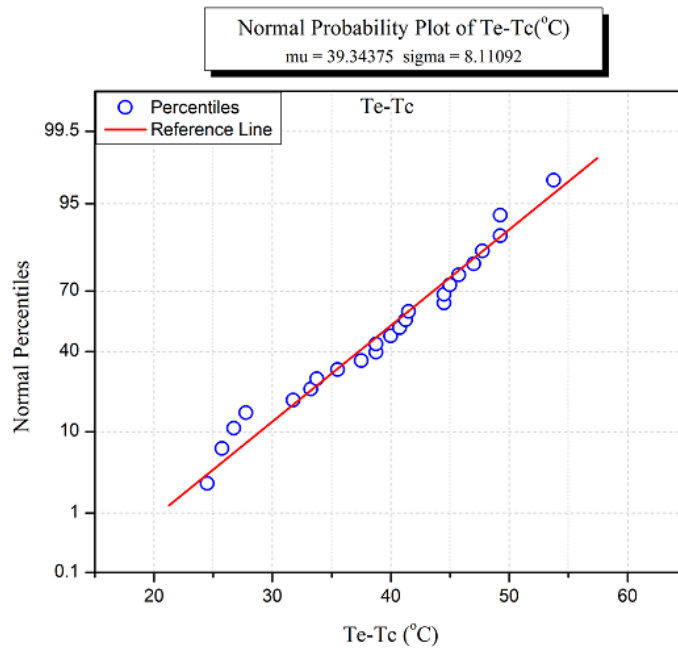


Fig. 6. Normal probability plot for change in temperature of acetone for evaporator and condenser

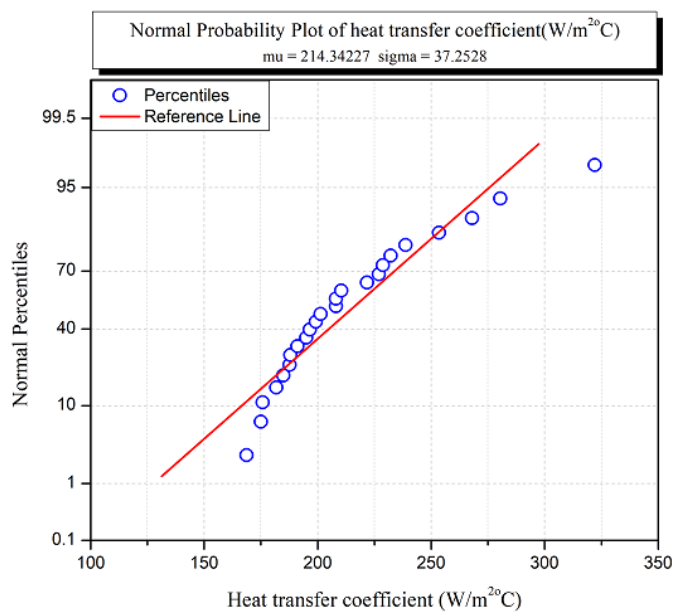


Fig. 7. Normal probability plot for heat transfer coefficient for acetone

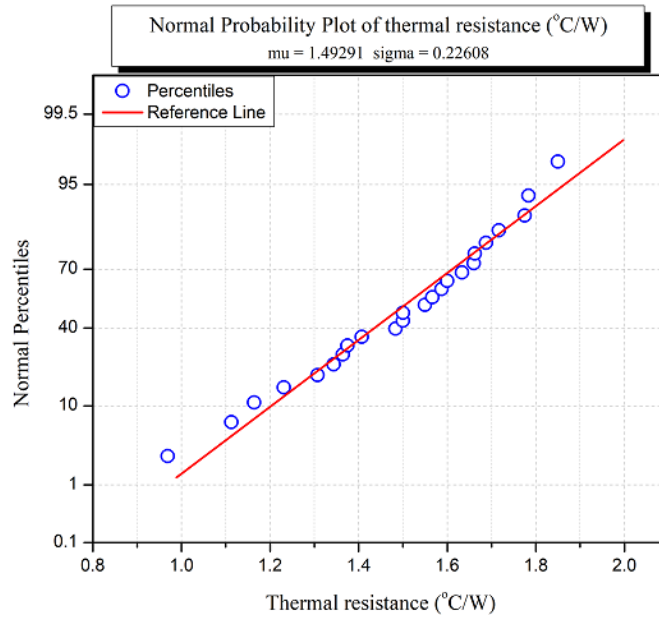


Fig. 8. Normal probability plot for thermal resistance for acetone

3.5 Statistical Analysis

Regression and Analysis of variance (ANOVA) method is used to predict the parameters experimentally to find the significant factors are statistically significant. MINITAB was a powerful statistical tool to obtained or analyse the significance of factors [22-25,32-36]. In the present analysis filler ratio and heat input was considered as an input variable to determine temperature difference ($T_e - T_c$), heat transfer coefficient and thermal resistance. Final based on the multiple regression analysis significant parameters was determined. Based on the F test results heat input and combination of heat input and filler ratio was the major significant parameters on heat transfer coefficient and thermal resistance for acetone. For all the combinations considered the predicted equations for $T_e - T_c$, heat transfer coefficient and thermal resistance the coefficient of determinations was 93.68%, 89.08% and 91.24% respectively and is shown in Eq. (3) to Eq. (5). Therefore, the models are clearly shows that the P-value of the independent variables is 95% of confidence interval and the details results are shown in Table 2. To measure the degree of fitness the relationship between the predicted and experimental values are shown in Figure 9(a) to Figure 9(c).

Finally, uncertainty analysis is carried out to differential the measured and predicted data. Figure 10(a) to Figure 10(c) clearly shows that the error between the samples was less than 5% for $T_e - T_c$, heat transfer coefficient and thermal resistance. Therefore, the predicted equations can be utilized for the different combinations of filler ratio and heat input with a confidence interval of 95%.

$$T_e - T_c = -29.7 + 0.449 \text{ FR} + 3.712 \text{ heat transfer} - 0.00177 \text{ FR} * \text{FR} - 0.03656 \text{ heat transfer} * \text{heat transfer} - 0.01353 \text{ FR} * \text{heat transfer} \quad R^2=93.68 \quad (3)$$

$$\text{Heat transfer coefficient} = 354 - 3.20 \text{ FR} - 9.17 \text{ heat transfer} + 0.0143 \text{ FR} * \text{FR} + 0.1382 \text{ heat transfer} * \text{heat transfer} + 0.0802 \text{ FR} * \text{heat transfer} \quad R^2=89.80 \quad (4)$$

$$\text{Thermal resistance} = 1.645 + 0.0021 \text{ FR} + 0.0214 \text{ heat transfer} + 0.000007 \text{ FR} \cdot \text{FR} - 0.000482 \text{ heat transfer} \cdot \text{heat transfer} - 0.000283 \text{ FR} \cdot \text{heat transfer} \quad (5)$$

$$R^2=91.24$$

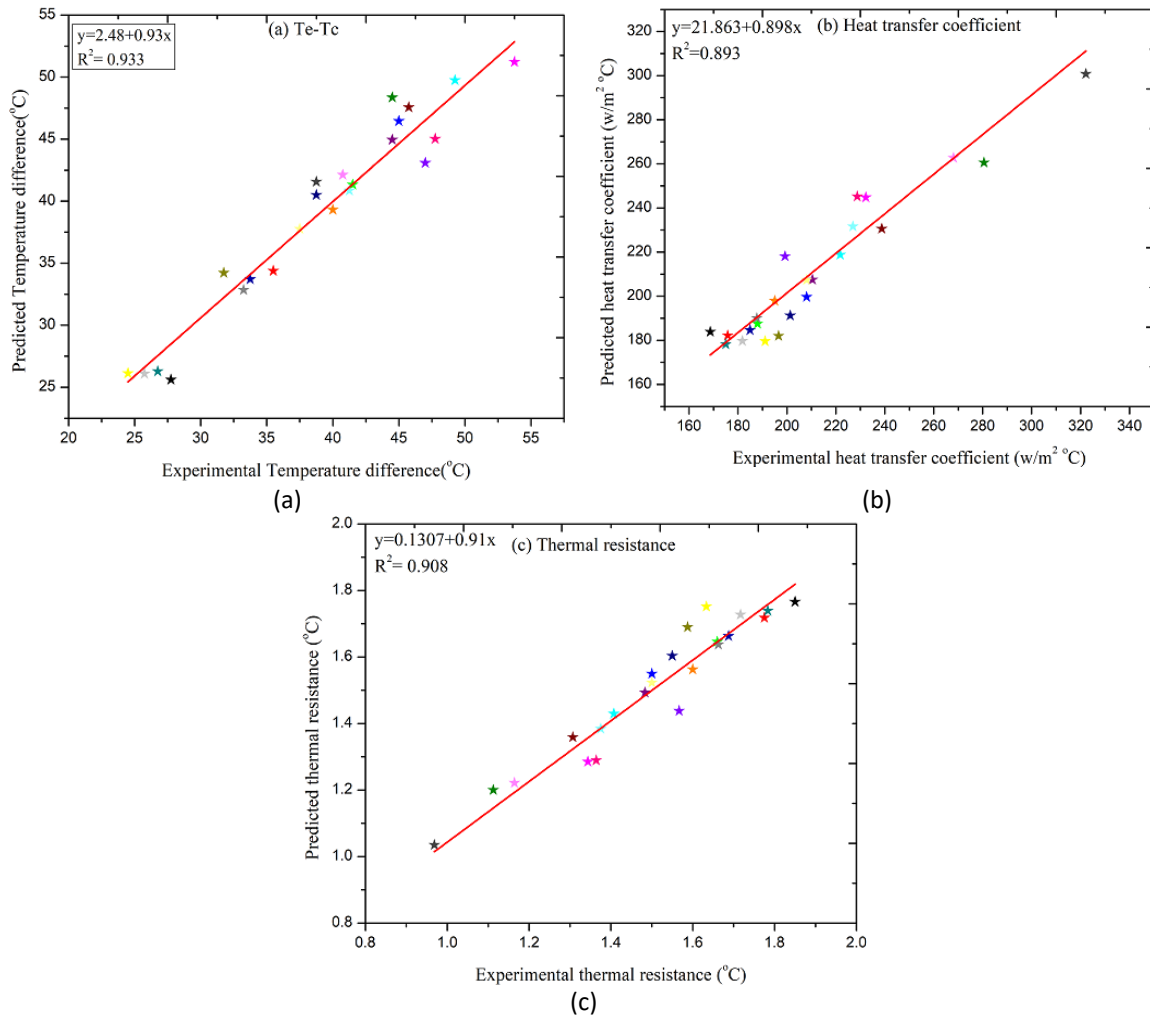


Fig. 9. Relationship between predicted and experimental values for (a) Te-Tc, (b) heat transfer coefficient and (c) Thermal resistance

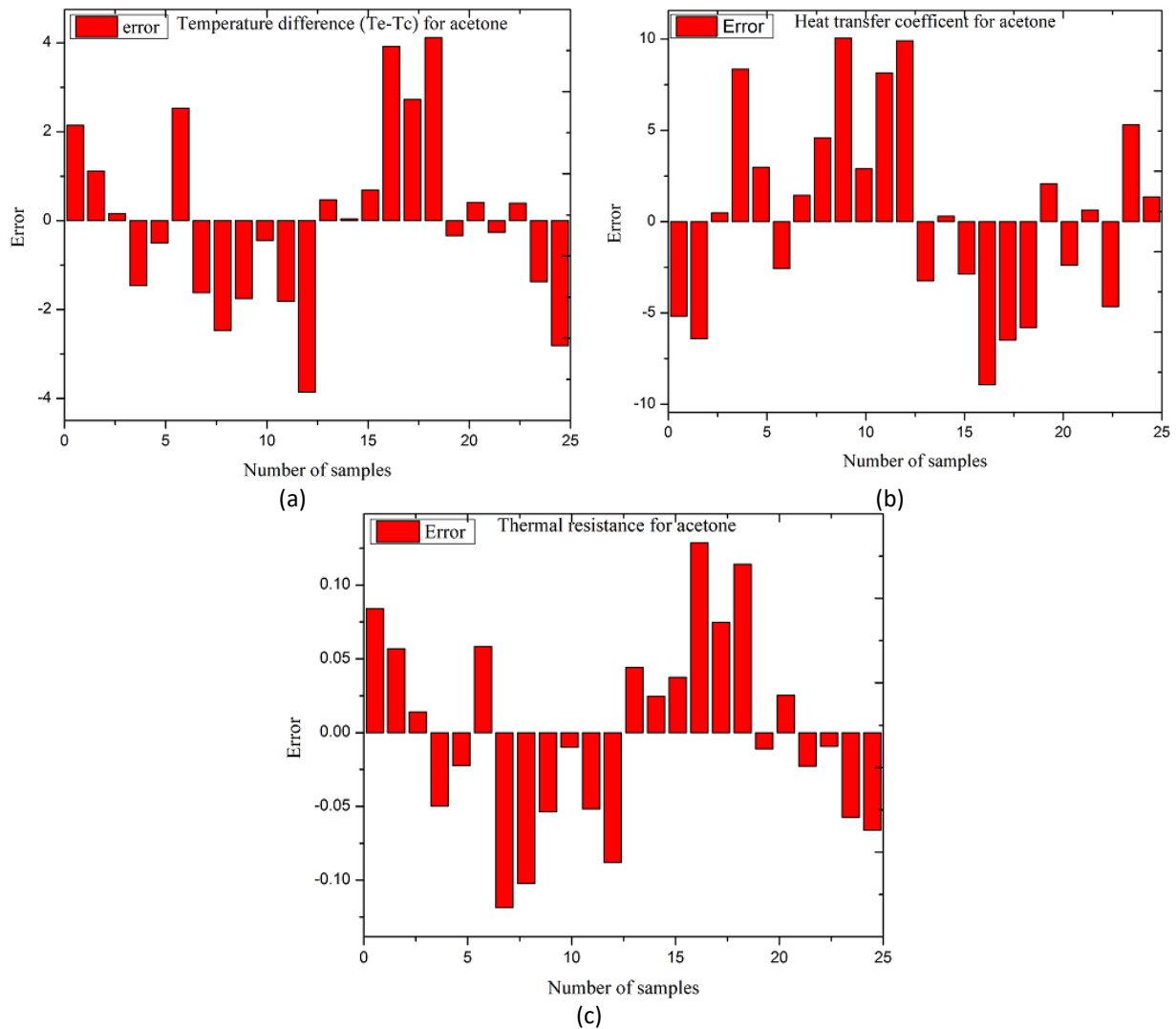


Fig. 10. Error values for (a) Te-Tc, (b) heat transfer coefficient and (c) Thermal resistance

Table 2

Regression models for significant variables

Model	Variable	Coefficient	Standard error	t-value	Tabulated t-value	F-value	Tabulated F-ratio	R ² (%)	Adjusted R ² (%)
Eq. (4)	Temperature difference (Te-Tc)								
	Constant	-29.7	22.0	-1.35	1.71	53.40	1.97	93.68	91.93
	Filler Ratio	0.449	0.628	0.72		0.51			
	Heat transfer rate	3.712	0.527	7.04		49.63			
	Filler ratio *	-0.00177	0.00470	-0.38		0.14			
	Filler ratio								
	Heat transfer rate * Heat transfer rate	-0.03656	0.00754	-4.85		23.50			
Eq. (5)	Filler ratio*	-0.01353	0.00493	-2.75		7.54			
	heat transfer								
	Heat Transfer Coefficient								
	Constant	354	129	2.75	1.71	31.69	1.97	89.80	86.97
	Filler ratio	-3.20	3.66	-0.87		0.76			
	Heat transfer rate	-9.17	3.08	-2.98		8.89			

	Filler ratio *	0.0143	0.0275	0.52		0.27		
	filler ratio							
	Heat transfer rate * Heat transfer rate	0.1382	0.0440	3.14		9.86		
	Filler ratio*	0.0802	0.0288	2.79		7.77		
	heat transfer							
Eq. (6)	Thermal Resistance							
	Constant	1.645	0.724	2.27	1.71	37.50	1.97	91.24 88.81
	Filler ratio	0.0021	0.0206	0.10		0.01		
	Heat transfer rate	0.0214	0.0173	1.24		1.53		
	Filler ratio *	0.000007	0.000154	0.04		0.00		
	filler ratio							
	Heat transfer rate * Heat transfer rate	-0.000482	0.000248	-1.95		3.79		
	Filler ratio*	-0.000283	0.000162	-1.75		3.05		
	heat transfer							

4. Conclusions

In this study, experimental investigations of a newly fabricated four turned OHP system were developed to determine the effect acetone as a working fluid on the thermal performance of an OHP. Based on the different heat input and filler ratio the conclusions were drawn as follows

- i. Based on the above results the heat input of 40W with a filler ratio of 80% the change in temperature was minimum of 6.03% than compare to the 50% of filler ratio of 7.20%. Because of acetone filled OHP had a high oscillating amplitude capacity compare to the water filled OHP.
- ii. For newly developed setup, heat transfer coefficient was 37% for 50% filler ratio with 40W heat input and suddenly increased by 77% for 80% filler ratio with a heat input of 40W was achieved with acetone filled OHP.
- iii. The thermal resistance was decreased by 43% with a filler ratio of 80% of acetone than compare to the 50% of filler ratio with 40W heat input was achieved. Therefore, increase in acetone as a filler ratio there was an increase in heat transfer coefficient and decrease in thermal resistance with a minimum temperature difference between the evaporator and condenser can be achieved.
- iv. Finally, statistical analysis was used to validate the data extracted from the experimental results. The independent variables are statistically significant for with a P-value of 0.05. The coefficient of determination for T_e-T_c , heat transfer coefficient and thermal resistance is 0.936, 0.898 and 0.912 respectively.

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