



Homogeneous And Heterogeneous Reactions on The Peristalsis of Bingham Fluid with Variable Fluid Properties Through a Porous Channel

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ABSTRACT

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The exploration addresses the effect of variable viscosity and thermal conductivity on the peristaltic mechanism of Bingham fluid. A two-dimensional non-uniform porous channel is considered for the fluid flow, which is assumed to be inclined. The impact of heat, slip conditions, wall properties, homogeneous and heterogeneous reactions are examined. The resulting nonlinear differential equations are solved by employing the perturbation method. The solutions acquired are analyzed and sketched through graphs that show that the variable viscosity renders a critical role in regulating the velocity of the fluid in the channel's central part. The stream function has been analyzed to observe the trapping phenomenon. Further, the obtained results find its application in understanding the flow of blood in micro arteries.

1. Introduction

The peristaltic mechanism is an inherent property caused by the contraction and expansion of the sinusoidal wave due to the flexible tube/channel walls. This mechanism is essential to understand bio-fluids' flow, such as blood, urine, eye drops, chyme movement, spermatozoa, etc. The mechanism was first investigated by Latham [1] using a Newtonian fluid model. He studied the spread of infection from bladder to kidney in the ureter. Shapiro *et al.*, [2] investigated the peristaltic transport with a longer wavelength and lowered Reynolds number. In earlier days, research was carried out for Newtonian fluid. Later, Raju and Devanathan [3] studied the properties of peristaltic flow using non-Newtonian fluid. The mechanism of peristalsis of Herschel-Bulkley fluid was analyzed by Vajravelu *et al.*, [4,5] in an inclined tube, which investigates the flow characteristics of fluids. Jiménez-Lozano *et al.*, [6] analyzed the peristalsis in a two-phase model to investigate the mechanism involved in ureteral biomechanics. Vaidya *et al.*, [7] considered an inclined tube to study the transport of a

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Bingham fluid and analyze the heat transfer effects during the peristalsis. Further, Manjunatha *et al.*, [8] examined the function of convective boundary conditions, porous-walled tube, and variable liquid properties in the peristaltic movement of a non-Newtonian Bingham fluid.

The slip effects on biological fluids have gained many researchers' attention in modern times for their vast application in the field of medicine. The initial studies on the influence of slip effects on peristaltic transport are carried out by El-Shehawey and Husseny [9] and El-Shehawey *et al.*, [10]. Awgichew and Radhakrishnamacharya [11] investigated the slip effect on the flow of a couple-stress fluid flowing in a symmetric two-dimensional channel with mild Stenosis. Akbar *et al.*, [12] emphasized the impacts of slip effects on the sinusoidal flow of nanofluids. Later on, Ellahi and Hussain [13] considered a rectangular duct in their studies on a Jeffrey fluid's peristalsis. They obtained a closed-form solution of the problem and studied the effects of MHD and partial slip conditions on the fluid transport. Akbar [14] studied the impact of thermal slip and velocity on the MHD peristaltic motion of a *Cu* water nanofluid. Hayat *et al.*, [15] analyzed the motion in a non-uniform permeable medium under the thermal slip conditions and radial magnetic field while accounting for the variable fluid viscosity. Recently, Manjunatha *et al.*, [16] explored the effect of slip on the peristaltic flow of Rabinowitsch fluid inside an inclined non-slippery tube. Furthermore, the slip effects on peristaltic transport of different non-Newtonian fluids with different geometries are studied [17-22].

Over the past years, studies have shown that flow through porous media is also an essential factor in peristaltic studies, given its applications in various industrial and biological processes. Elshehawey *et al.*, [23] obtained a precise form of the streamline function in their attempt to study the peristalsis in an asymmetric permeable conduit. Further, Alsaedi *et al.*, [24] investigated the flow of an incompressible couple stress fluid in a permeable medium. They examined the effect of couple stress and permeability parameters on peristalsis inside a medium having pores. Nadeem *et al.*, [25] studied the porous medium's influence on the peristalsis of a nanofluid. Ramesh and Devakar [26] studied the influence of heat and mass transfer in the peristalsis of a couple-stress fluid in a vertical asymmetric channel. They considered the effects of the magnetic field and homogeneous permeable medium. Recently, Rajashekhar *et al.*, [27] examined the impact of variable liquid properties of the peristaltic transport through a porous medium.

In the past few years, the researchers noticed the importance of thermophysical properties in understanding various mechanisms associated with the human body. It is seen that in physiological fluids like blood and other liquids, these properties are not constant. In the variation in these properties, it is necessary to reflect on the variable thermal conductivity as well viscosity. The influence of varying viscosity was taken into consideration by Farooq *et al.*, [28] in their peristaltic study on Jeffrey fluid. Abbasi *et al.*, [29] revealed facts on the variable thermal conductivity and convective heat conditions in their investigations on the peristaltic motion of Carreau-Yasuda fluid. Both the properties of varying viscosity and thermal conductivity were reported by Baliga *et al.*, [30] while investigating the peristalsis of Herschel-Bulkley fluid. In an attempt to investigate the effects of variable properties of a Bingham Fluid exhibiting porous peristaltic motion, Divya *et al.*, [31] considered an inclined magnetic field. Due to its immense applicability in bioengineering and medicine, numerous researchers have studied its impact on various geometries [32-40].

The chemical reaction can be modified as either a homogeneous or heterogeneous process. It depends on whether they occur at an interface or as a single-phase volume reaction. The response is heterogeneous/homogeneous if it happens at an interface/in solution. There is the involvement of both homogeneous and heterogeneous reactions in several chemically reacting systems. Mention may be made to the processes occurring in catalysis, combustion, biochemical techniques, cooling towers, fog dispersion, crop-damaging through freezing, and many others. The study on modelling

the peristaltic flow under the chemical reactions can be found in [41-43]. Recently, numerous studies have been carried on the investigation of non-Newtonian fluids in various geometries [44-47].

Having considered the various researchers and their work the author concludes that no attempts has been made to analyze the characteristic flow of a Bingham fluid during peristalsis through a non-uniform, inclined porous channel, where both variations of viscosity and thermal conductivity have also been considered. Moreover, the present study also investigates the homogeneous and heterogeneous reactions. The study also includes wall properties to understand the applications in industries and medicine better. Heat transfer is investigated with convective conditions. The mathematical model is solved by the method of perturbation. The consequences of relevant parameters on temperature, velocity, streamlines, and concentration are reported with graphs using MATLAB and the outcomes are explained.

2. Formulation of the Problem

A non-compressible non-Newtonian fluid flowing through an inclined non-uniform permeable channel is considered for analysis. The flow is governed by the Bingham Fluid model. The flow is induced by peristaltic waves moving with a constant speed C . The Cartesian coordinate system is chosen such that x' is the axial direction and y' is perpendicular to it.

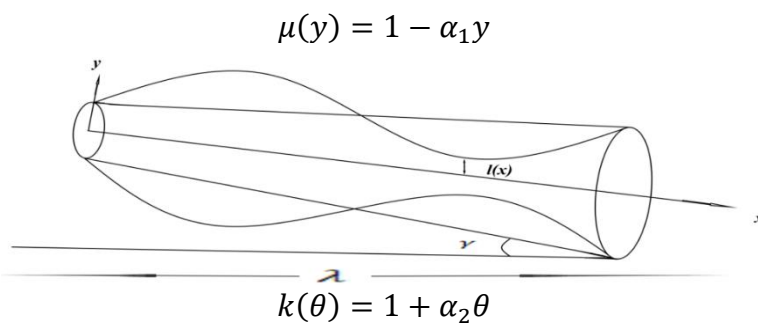


Fig. 1. Geometry of the physical model

We consider the homogeneous-heterogeneous reaction model between two chemical species \hat{I} and \hat{J} as defined below [41,42]



Further, single, isothermal and first order chemical reaction is considered on the catalyst surface. Thus, we have



where I and J are the concentration of \hat{I} and \hat{J} respectively, while K_c and K_s are the rate constants. Note that here both the reaction processes take place at the same temperature.

The equations that govern the flow are

$$\frac{\partial u'}{\partial x'} + \frac{\partial w'}{\partial y'} = 0, \quad (3)$$

$$\rho \left[\frac{\partial u'}{\partial t'} + u' \frac{\partial u'}{\partial x'} + w' \frac{\partial u'}{\partial y'} \right] = -\frac{\partial p'}{\partial x'} + \frac{\partial \tau'_{x'x'}}{\partial x'} + \frac{\partial \tau'_{x'y'}}{\partial x'} - \frac{\mu}{\kappa} (w' + C) + \rho g \beta' \sin \gamma (T_1 - T_0), \quad (4)$$

$$\rho \left[\frac{\partial w'}{\partial t'} + u' \frac{\partial w'}{\partial x'} + w' \frac{\partial w'}{\partial y'} \right] = -\frac{\partial p'}{\partial x'} + \frac{\partial \tau'_{x'y'}}{\partial x'} + \frac{\partial \tau'_{y'y'}}{\partial x'} - \frac{\mu}{\kappa} (u') + \rho g \beta' \cos \gamma (T_1 - T_0), \quad (5)$$

$$\rho C_p \left[\frac{\partial T'}{\partial t'} + u' \frac{\partial T'}{\partial x'} + w' \frac{\partial T'}{\partial y'} \right] = k_1 \left[\frac{\partial}{\partial x'} \left(k(T') \frac{\partial T'}{\partial x'} \right) + \frac{\partial}{\partial y'} \left(k(T') \frac{\partial T'}{\partial y'} \right) \right] + Q_0, \quad (6)$$

$$\frac{dI}{dt} = M_I \left(\frac{\partial^2 I}{\partial x'^2} + \frac{\partial^2 I}{\partial y'^2} \right) - kcIJ^2, \quad (7)$$

$$\frac{dJ}{dt} = M_J \left(\frac{\partial^2 J}{\partial x'^2} + \frac{\partial^2 J}{\partial y'^2} \right) + kcIJ^2, \quad (8)$$

where u', w' are components of velocity in radial and axial directions respectively. ρ is the fluid density, P' is the pressure, $\tau'_{x'x'}, \tau'_{x'y'}, \tau'_{y'y'}$ are extra stress components, while k_1, T', C_p, M_I, M_J , denotes thermal conductivity, temperature, specific heat at constant volume and mass diffusivity coefficient for homogeneous and heterogeneous reactions respectively.

The conditions at the boundary are

$$\frac{\partial w'}{\partial y'} = \tau_0 \quad \text{at } y' = 0, \quad (9)$$

$$w' + \beta_1 \frac{\partial w'}{\partial y'} = 0 \quad \text{at } y' = H' = l(x') + b' \sin \left(\frac{2\pi}{\lambda} (x' - ct') \right), \quad (10)$$

$$\frac{\partial T'}{\partial y'} = 0 \quad \text{at } y' = 0, \quad (11)$$

$$-k_1 \frac{\partial T'}{\partial y'} = \eta (T' - T_0') \tau_0 \quad \text{at } y' = H', \quad (12)$$

$$I = I_0 \quad \text{at } y' = 0, \quad (13)$$

$$M_I \frac{\partial I}{\partial y'} = k_s I \quad \text{at } y' = H', \quad (14)$$

$$J = J_0 \text{ at } y' = 0, \quad (15)$$

$$M_J \frac{\partial J}{\partial y'} = -k_s J \text{ at } y' = H', \quad (16)$$

where H' represents non-uniform wave wherein $l(x')$ is the non-uniform radius. The meanings of other variables used are given in the nomenclature section.

We now introducing the dimensionless quantities

$$\begin{aligned} x &= \frac{x'}{\lambda}, \quad y = \frac{y'}{a'}, \quad w = \frac{w'}{a'}, \quad u = \frac{\lambda u'}{Ca}, \quad \tau_{xx} = \frac{a' \tau'_{xx} x'}{C\mu}, \quad \tau_{xy} = \frac{a' \tau'_{xy} y'}{C\mu}, \quad \tau_{yy} = \frac{a' \tau'_{yy} y'}{C\mu}, \quad t = \frac{ct'}{\lambda}, \\ \text{Re} &= \frac{aC\rho}{\mu}, \quad p = \frac{a'^2 p'}{C\lambda\mu}, \quad \theta = \frac{T' - T'_0}{T_1 - T_0}, \quad \text{Pr} = \frac{\mu C_p}{k_1}, \quad Da = \frac{k_1}{a'}, \quad y'_p = \frac{y_p}{a'}, \quad \beta = \frac{Q_0 a'^2}{k_1(T_1 - T_0)}, \\ K_s &= \frac{k_s I}{M_I}, \quad \xi = \frac{M_I}{M_J}, \quad Gr = \frac{\rho \beta' g a'^2 (T_1 - T_0)}{\mu C}, \quad g = \frac{I}{I_0}, \quad f = \frac{I}{I_0}, \quad \delta = \frac{a'}{\lambda}, \quad \varepsilon = \frac{b'}{a'}, \\ E_1 &= \frac{-\sigma a'^3}{\lambda \mu C}, \quad E_2 = \frac{m a'^3 C}{\lambda^3 \mu}, \quad E_3 = \frac{a'^3 C}{\lambda^3 \mu}, \quad h = \frac{H'}{a'} = 1 + mx + \varepsilon \sin(2\pi(x-t)) \end{aligned} \quad (17)$$

Using Eq. (17) in Eq. (3)-(8) and by using low Reynolds number and long wavelength approximations, the non-dimensional governing equations take the form as below

$$\frac{\partial p}{\partial x} = \frac{\partial \tau_{xy}}{\partial y} - \frac{1}{Da} (w+1) + Gr\theta \sin y, \quad (18)$$

$$\frac{\partial p}{\partial y} = 0, \quad (19)$$

$$\frac{\partial}{\partial y} \left(k(\theta) \frac{\partial \theta}{\partial y} \right) + \beta = 0, \quad (20)$$

$$\frac{1}{Sc} \frac{\partial^2}{\partial y^2} = Kfg^2, \quad (21)$$

$$\frac{\xi}{Sc} \frac{\partial^2 g}{\partial y^2} = -Kfg^2, \quad (22)$$

where f, g are the dimensionless concentration of chemical species \hat{I} and \hat{J} . Further, τ_{xy} denotes constitutive equation of Bingham fluid

$$\tau_{xy} = \mu \dot{\gamma} + \tau_0, \quad \tau_{xy} \geq \tau_0, \quad (23)$$

$$\dot{\gamma} = 0, \quad \tau_{xy} \leq \tau_0. \quad (24)$$

The dimensionless boundary conditions are

$$\frac{\partial w}{\partial y} = \tau_0 \quad \text{at } y = 0, \quad (25)$$

$$w + \beta_1 \frac{\partial w}{\partial y} = 0 \quad \text{at } y = h, \quad (26)$$

$$\frac{\partial \theta}{\partial y} = 0 \quad \text{at } y = 0, \quad (27)$$

$$\theta + \beta_2 \frac{\partial \theta}{\partial y} = 0 \quad \text{at } y = h, \quad (28)$$

$$f = 1 \quad \text{at } y = 0, \quad (29)$$

$$\frac{\partial f}{\partial y} = K_s f \quad \text{at } y = h, \quad (30)$$

$$g = 1 \quad \text{at } y = 0, \quad (31)$$

$$\frac{\partial g}{\partial y} = -K_s f \quad \text{at } y = h, \quad (32)$$

where β_1 and β_2 are velocity and temperature slip parameters respectively.

Assuming the diffusion constants M_I and M_J to be equal (i.e., $\xi = 1$), which makes Eq. (29)-(32) take the following form

$$f + g = 1. \quad (33)$$

Using the above, Eq. (21) and Eq. (22) take the forms

$$\frac{1}{Sc} \frac{\partial^2 f}{\partial y^2} = Kf(1-f)^2, \quad (34)$$

with the boundary condition

$$f = 1 \quad \text{at } y = 0, \quad (35)$$

$$\frac{\partial f}{\partial y} = K_s f \quad \text{at } y = h, \quad (36)$$

The varying viscosity across the wall channel thickness is

$$\mu(y) = 1 - a_1 y, \text{ for } a_1 \ll 1, \quad (37)$$

where a_1 is the variable viscosity coefficient.

With respect to temperature, the thermal conductivity varies and is given by

$$k(\theta) = 1 - a_2 \theta, \text{ for } a_2 \ll 1, \quad (38)$$

where a_2 is the coefficient of variable thermal conductivity.

3. Solution to the Problem

Eq. (18)-(22) are nonlinear equations. To solve these equations, we apply perturbation technique for smaller values of coefficients of variable viscosity and thermal conductivity respectively.

3.1 Perturbation Solution

The solution for velocity and temperature is obtained by solving Eq. (18) and Eq. (20) along with conditions at the boundary given by Eq. (25)-(28) using the perturbation series as follows

$$w = \sum_{n=0}^{\infty} (a_1^n w_n). \quad (39)$$

$$\theta = \sum_{n=0}^{\infty} (a_2^n \theta_n). \quad (40)$$

Also, the perturbation solution is obtained for the Eq. (34) for small parameter K .

$$f = \sum_{n=0}^{\infty} (K^n f_n). \quad (41)$$

3.1.1 Zeroth Order Solution

$$w_0 = C_1 \sin \frac{y}{\sqrt{Da}} + C_2 \cos \frac{y}{\sqrt{Da}} - PDa + B_1 (Day^4 - 12Da^2 y^2 + 24Da^3) + B_2 (Day^2 - 2Da^2) + B_3 Da. \quad (42)$$

$$\theta_0 = \left(\frac{\beta}{2} y^2 + \beta \beta_2 h + \frac{\beta}{2} h^2 \right). \quad (43)$$

$$f_0 = 1 + \frac{yK_s}{1 - hK_s}. \quad (44)$$

3.1.2 First Order Solution

$$w_1 = C_3 \sin \frac{y}{\sqrt{Da}} + C_4 \cos \frac{y}{\sqrt{Da}} + (G_1 + G_3)y + G_2 y^3 + C_1 \left(\left(y - \frac{1}{4} \right) \sin \frac{y}{\sqrt{Da}} + \left(\frac{y^2}{4\sqrt{Da}} - \frac{\sqrt{Da}}{8} \right) \cos \frac{y}{\sqrt{Da}} \right) + C_2 \left(\frac{y}{4} \cos \frac{y}{\sqrt{Da}} - \left(\frac{y^2}{4\sqrt{Da}} + \frac{\sqrt{Da}}{8} \right) \sin \frac{y}{\sqrt{Da}} \right) \quad (45)$$

$$\theta_0 = a_2 \left(\frac{\beta}{2} y^2 + \beta \beta_2 h + \frac{\beta}{2} h^2 \right) \quad (46)$$

$$f_1 = \frac{ScK_s^2 \left(y^4 (-1 + hK_s) (-5 + 5hK_s - 3yK_s) - 2h^3 y (10 - 5hK_s + h^2 K_s^2) \right)}{60(-1 + hK_s^4)} \quad (47)$$

With the velocity expression, upper bound of the plug flow region is found with the help of following boundary condition

$$\frac{\partial w}{\partial y} = 0 \quad \text{at} \quad y = y_p \quad (48)$$

Using the above condition, we obtain the expression for stress in plug flow region. i.e.,

$$\tau_0 = \frac{(S_1 + S_2) - a_1 (S_3 + S_4 + S_5 + S_6)}{S_7 + \alpha_1 (S_8 + S_9 + S_{10} + S_{11})} \quad (49)$$

Using Eq. (42) and Eq. (45) we can also obtain the plug flow velocity when $y = y_p$ as

$$w_p = X_1 \cos \frac{y_p}{\sqrt{Da}} + X_2 \sin \frac{y_p}{\sqrt{Da}} + X_3 + X_4 + a_1 X_5 \quad (50)$$

We now obtain the stream function using the following expression given below

$$w = \frac{\partial \psi}{\partial y}, \quad u = -\frac{\partial \psi}{\partial x} \quad (51)$$

with the boundary condition,

$$\psi = 0 \quad \text{at} \quad y = h \quad (52)$$

Then the expression for Stream function is given as

$$\psi = \psi_0 + \alpha_1 \psi_1 \quad (53)$$

where,

$$\begin{aligned} \psi_0 = & C_2 \sqrt{Da} \sin \frac{y}{\sqrt{Da}} - C_1 \sqrt{Da} \cos \frac{y}{\sqrt{Da}} - P Da y + B_1 \left(Da \frac{y^5}{5} - 12 Da^2 \frac{y^3}{3} + 24 Da^3 y \right) \\ & + B_2 \left(Da \frac{y^3}{3} - 2 Da^2 y \right) + B_3 Da y \end{aligned} \quad (54)$$

$$\begin{aligned} \psi_1 = & C_4 \sqrt{Da} \sin \frac{y}{\sqrt{Da}} - C_3 \sqrt{Da} \cos \frac{y}{\sqrt{Da}} + C_2 \left(-\frac{\sqrt{Da}}{4} y \sin \frac{y}{\sqrt{Da}} - \left(\frac{y^2}{4} + \frac{Da}{8} \right) \cos \frac{y}{\sqrt{Da}} \right) \\ & + C_1 \left(\frac{\sqrt{Da}}{2} \left(\frac{1}{4} + y \right) \cos \frac{y}{\sqrt{Da}} + \left(\frac{y^2}{4} + \frac{3Da}{8} \right) \sin \frac{y}{\sqrt{Da}} \right) + (G_1 + G_2) \frac{y^2}{2} + G_2 \frac{y^4}{4} \end{aligned} \quad (55)$$

The expressions for $A_1, A_2, B_1, B_2, B_3, C_i (i = 1, 2, 3, 4), D_j (j = 1, 2, \dots, 8), F_k (k = 1, 2, \dots, 7), G_1, G_2, G_3, Q_i (i = 1, 2, 3, \dots, 11)$ and $X_n (n = 1, 2, \dots, 5)$ are mentioned as follows

$$P = \frac{\partial p}{\partial x} = 8\epsilon\pi^3 \left(-(E_1 + E_2) \cos(2\pi(x - t)) + E_3 \frac{\sin(2\pi(x - t))}{2\pi} \right)$$

$$A_1 = -\frac{\beta}{2}$$

$$A_2 = \beta\beta_2 h + \beta \frac{h^2}{2}$$

$$B_1 = Gr A_1^2 \alpha_2 \sin \gamma$$

$$B_2 = Gr (A_1 + 2 A_1 A_2 \alpha_2) \sin \gamma$$

$$B_3 = Gr A_2^2 \alpha_2 \sin \gamma$$

$$C_1 = \tau_0 \sqrt{Da}$$

$$C_2 = C_1 F_1 + F_2 + F_3 + F_4$$

$$C_3 = \sqrt{Da} \left(\tau_0 - G_1 - G_3 - \frac{C_2}{8} + \frac{C_1}{4} \right)$$

$$C_4 = C_3 F_1 + F_5 + C_2 F_6 + C_1 F_7$$

$$D_1 = \frac{\beta_1}{\sqrt{Da}} \sin \frac{h}{\sqrt{Da}} - \cos \frac{h}{\sqrt{Da}}$$

$$D_2 = \frac{\beta_1}{\sqrt{Da}} \cos \frac{h}{\sqrt{Da}} + \sin \frac{h}{\sqrt{Da}}$$

$$D_3 = B_2 (-Da h^2 + 2 Da^2 - 2 Da \beta_1 h)$$

$$D_4 = B_1 (Da h^4 - 12 Da^2 h^2 + 24 Da^3 + 4 Da h^3 \beta_1 - 24 Da \beta_1 h)$$

$$D_5 = B_3 Da - P Da$$

$$D_6 = (G_1 + G_3)(h + \beta_2) + G_2 h^2 (h + 3 \beta_1)$$

$$D_7 = \left(\frac{h}{4} + \frac{\beta_1 h^2}{4 Da} + \frac{1}{8} \right) \cos \frac{h}{\sqrt{Da}} - \left(\frac{h^2}{4\sqrt{Da}} + 5 \frac{\sqrt{Da}}{8} - \frac{h}{4} \right) \sin \frac{h}{\sqrt{Da}}$$

$$D_8 = \left(\frac{h^2}{4\sqrt{Da}} - \frac{\sqrt{Da}}{8} + \frac{3}{2} \beta_1 h - \frac{\beta_1}{4\sqrt{Da}} \right) \cos \frac{h}{\sqrt{Da}} + \left(h - \frac{1}{4} - \frac{\beta_1 h^2}{4 Da} + 7 \frac{\beta_1}{8} \right) \sin \frac{h}{\sqrt{Da}}$$

$$F_1 = \frac{D_2}{D_1}$$

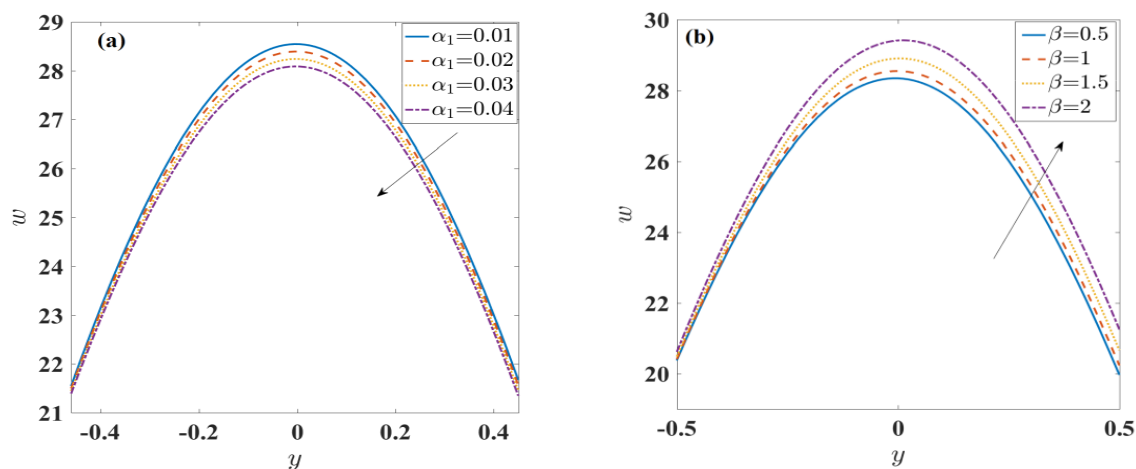
$$\begin{aligned}
 F_2 &= -\frac{D_3}{D_1} \\
 F_3 &= \frac{D_4}{D_1} \\
 F_4 &= \frac{D_5}{D_1} \\
 F_5 &= \frac{D_6}{D_1} \\
 F_6 &= \frac{D_7}{D_1} \\
 F_7 &= \frac{D_8}{D_1} \\
 G_1 &= -144 B_1 \sqrt{Da^5} \\
 G_2 &= 16 B_1 \sqrt{Da^3} \\
 G_3 &= 4 B_2 \sqrt{Da^3} \\
 S_1 &= B_3 Da (24 Da y_p - y_p^3) - 2 B_2 Da \\
 S_2 &= -\frac{(F_1 + F_3)}{\sqrt{Da}} \sin \frac{y_p}{\sqrt{Da}} \\
 S_3 &= (G_1 + G_3) + G_2 y_p^2 \\
 S_4 &= \frac{(F_2 + F_3)}{\sqrt{Da}} \left(\frac{y_p^2}{4 Da} + \frac{1}{8} \right) \cos \frac{y_p}{\sqrt{Da}} - \left(\frac{y_p}{4} + \frac{\sqrt{Da}}{2} \right) \sin \frac{y_p}{\sqrt{Da}} \\
 S_5 &= -\frac{(G_1 + G_3)}{\sqrt{Da}} \cos \frac{y_p}{\sqrt{Da}} \\
 S_6 &= -\frac{D_6}{\sqrt{Da}} \sin \frac{y_p}{\sqrt{Da}} \\
 S_7 &= F_1 \sin \frac{y_p}{\sqrt{Da}} + \cos \frac{y_p}{\sqrt{Da}} \\
 S_8 &= F_1 \sqrt{Da} \left(\frac{y_p^2}{4 Da} + \frac{1}{8} \right) \cos \frac{y_p}{\sqrt{Da}} - \left(\frac{y_p}{4} + \frac{\sqrt{Da}}{2} \right) \sin \frac{y_p}{\sqrt{Da}} \\
 S_9 &= \sqrt{Da} \left(-\frac{y_p^2}{4 Da} + \frac{7}{8} \right) \sin \frac{y_p}{\sqrt{Da}} + \frac{3}{2} \sqrt{Da} y_p - \frac{1}{4} \cos \frac{y_p}{\sqrt{Da}} \\
 S_{10} &= -\left(1 + \frac{\sqrt{Da}}{4} - \frac{F_1}{8} \right) \cos \frac{y_p}{\sqrt{Da}} \\
 S_{11} &= \left(\left(1 + \frac{\sqrt{Da}}{4} - \frac{F_1}{8} \right) \frac{F_1}{\sqrt{Da}} + \frac{F_1 F_6}{\sqrt{Da}} + \sqrt{Da} F_7 \right) \sin \frac{y_p}{\sqrt{Da}} \\
 X_1 &= C_2 + \alpha_1 \left(C_1 \left(\frac{y_p^2}{4 \sqrt{Da}} - \frac{\sqrt{Da}}{8} \right) + C_2 \frac{y_p}{4} + C_4 \right) \\
 X_2 &= C_1 + \alpha_1 \left(C_1 \left(y - \frac{1}{4} \right) + C_2 \frac{\sqrt{Da}}{8} + C_3 \right) \\
 X_3 &= B_2 (Da y_p^2 - 2 Da^2) + B_3 Da - P Da \\
 X_4 &= B_1 (Da y_p^4 - 12 Da^2 y_p^2 + 24 Da^3) \\
 X_5 &= (G_1 + G_3) y_p + G_2 y_p^3 - C_2
 \end{aligned}$$

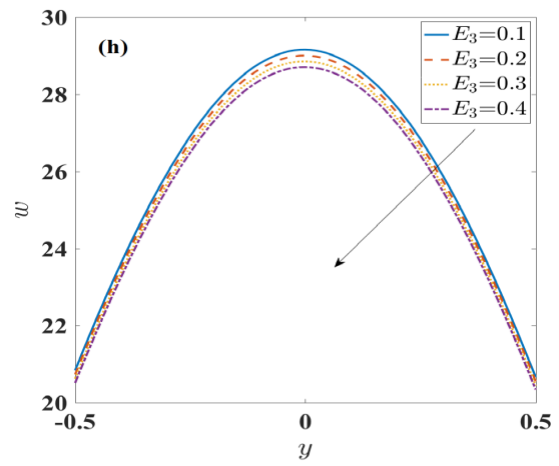
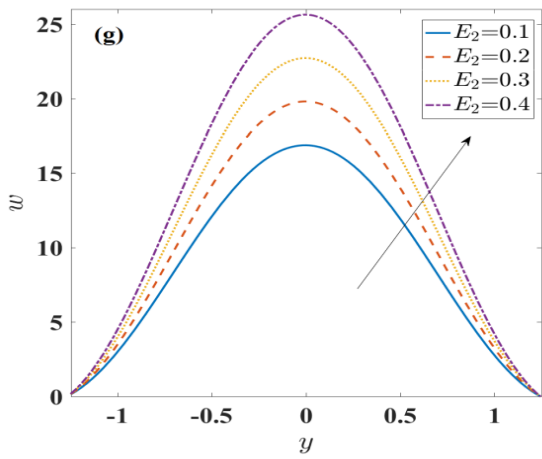
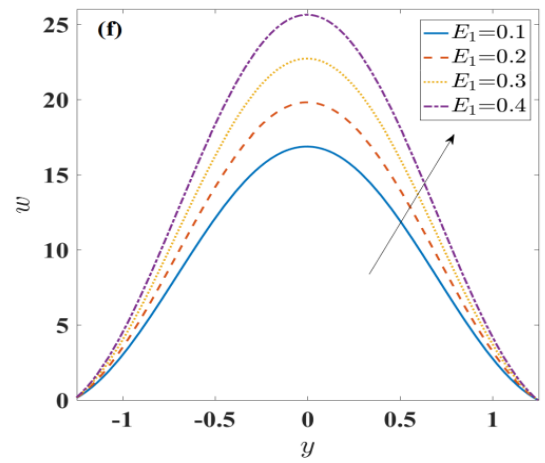
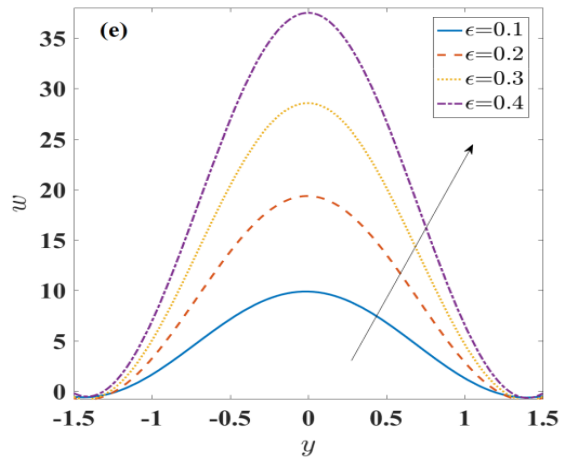
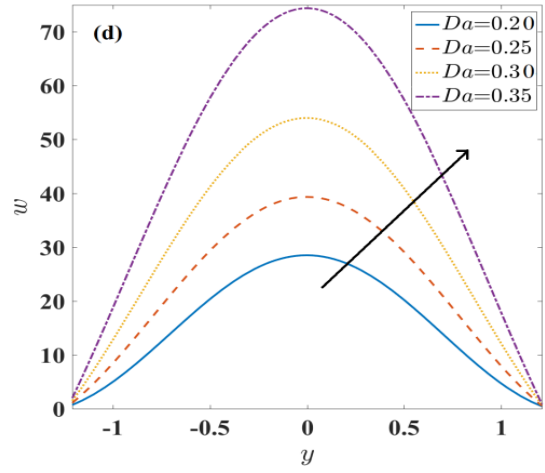
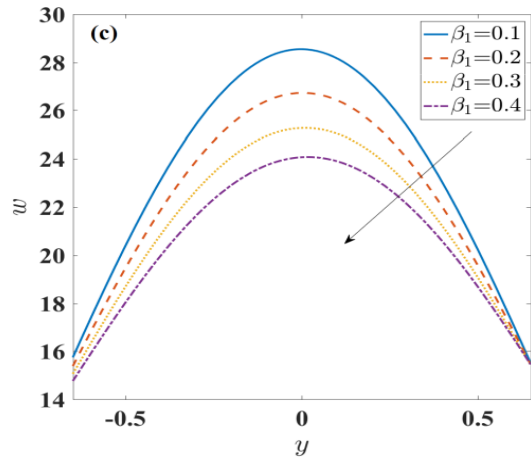
4. Results and Discussion

In the current segment, the influence of important parameters on the temperature profiles, velocity profiles and stream function are discussed. The effects of rigidity parameter (E_1), stiffness parameter (E_2), viscous damping force parameter (E_3), variable viscosity (α_1), Darcy number (Da), velocity slip parameter (β_1), temperature slip parameter (β_2), non-uniformity parameter (m), strength of heterogeneous reaction (K_s) and homogeneous reaction (K), Schmidt number (Sc), are analyzed and discussed through graphs. MATLAB programming has been employed for the pictographic depictions of pertinent parameters of importance, taking the following values of parameters: $E_1=0.5$, $E_2=0.5$, $E_3=0.5$, $m=0.1$, $Da=0.2$, $\alpha_1=0.01$, $t=0.2$, $x=0.22$, $\beta_1=0.1$, $\beta_2=2$, $Gr=1$, $y_p=0.3$, $\epsilon=0.3$, $K_s=2$, $K=0.2$; $Sc=0.5$ and $\gamma=\frac{\pi}{3}$.

4.1 Velocity Profiles

The influence of α_1 , β , β_1 , Da , ϵ , E_1 , E_2 , E_3 , γ and m on velocity are illustrated through Figure 2. Each of these parameters are studied for their influence on velocity of the Bingham fluid model. The Figure 2(a) to Figure 2(j) clearly exhibit the parabolic profiles for velocity. Figure 2(a) is drawn to analyze the behavior of variable viscosity on the velocity profiles. The figure infers that, in the central part, growth of variable viscosity diminishes the velocity profiles of the fluid, while the behavior is contrast in the central part of the conduit for heat generating parameter Figure 2(b). The influence of velocity slip on velocity profile is represented in Figure 2(c) and we notice a decrease in velocity when the velocity slip parameter value increases. The velocity enhances for an increase in the porosity at the center of the channel (see Figure 2(d)). As the amplitude ratio rises, the central channel velocity enhances with larger estimation (Figure 2(e)). The effects of changes in the wall properties on the fluid are plotted. It is noticed that enhancing the values of E_1 and E_2 confronts an increase in the fluid velocity. With rise in the values of E_3 , the velocity of the flow diminishes, and we can also notice that the change in velocity with respect to varying E_3 is so small that it can be negligible (see Figure 2(f) to Figure 2(h)). From the Figure 2(i) we observe that larger the inclination angle of the channel, faster the fluid moves. Also, as the channel becomes more non-uniform, velocity of the fluid reduces (see Figure 2(j)).





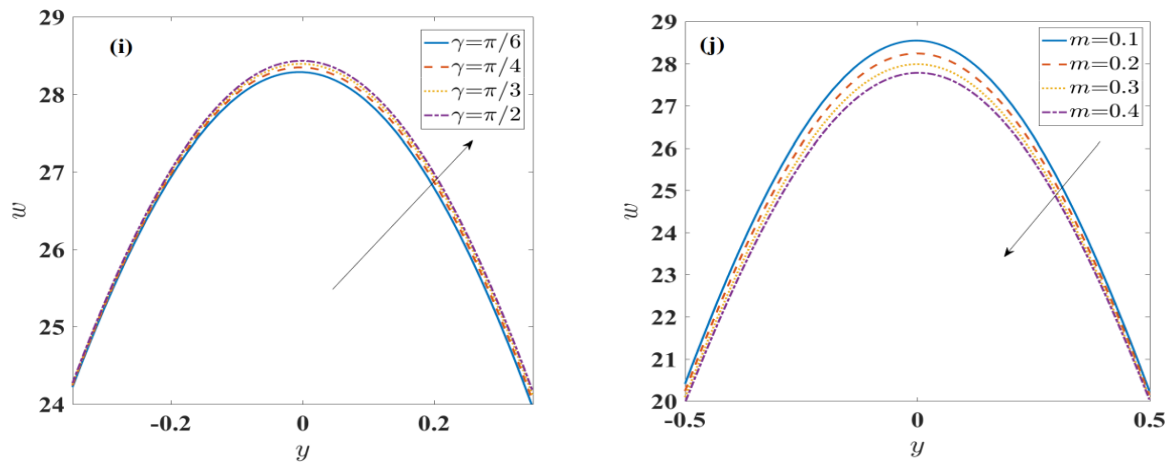


Fig. 2. Velocity profiles for varying (a) α_1 , (b) β , (c) β_1 , (d) Da , (e) ε (f) E_1 , (g) E_2 , (h) E_3 , (i) γ and (j) m

4.2 Temperature Profiles

Graphical representations in Figure 3(a) to Figure 3(d) depict the variation in temperature profiles for varying physical parameters. The significance of β in fluid temperature is shown in Figure 3(a), where it can be seen to increase the temperature with its rising value. In the flow of blood in arterioles, this behavior is reasonable due to the thickening of the boundary layer as heat is generated, which results in an appreciable rise in the temperature of the boundary layer. However, Figure 3(b) shows an enhancement in the fluid temperature with increasing variable thermal conductivity. The effect of thermal slip parameter can be seen to have an enhancement in temperature with an increase in these parameters (see Figure 3(c)). Figure 3(d) shows that the non-uniformity parameter enhances the temperature.

4.3 Homogeneous and Heterogeneous Reaction Effects

The effect of heterogeneous and homogeneous reactions K_s and K , Schmidt number Sc and non-uniformity parameter m on the concentration profiles are plotted in Figure 4(a) to Figure 4(d). From Figure 4(a) and Figure 4(b), it can be understood that while the parameter K_s enhances the concentration with its increasing values, higher values of the parameter K results in a diminution in the concentration. An increase in Sc would mean an increase in the molecular diffusion, thus resulting in a reduction in the concentration. This behavior is reflected in Figure 4(c). A contrary behavior of the non-uniformity parameter is depicted in Figure 4(d).

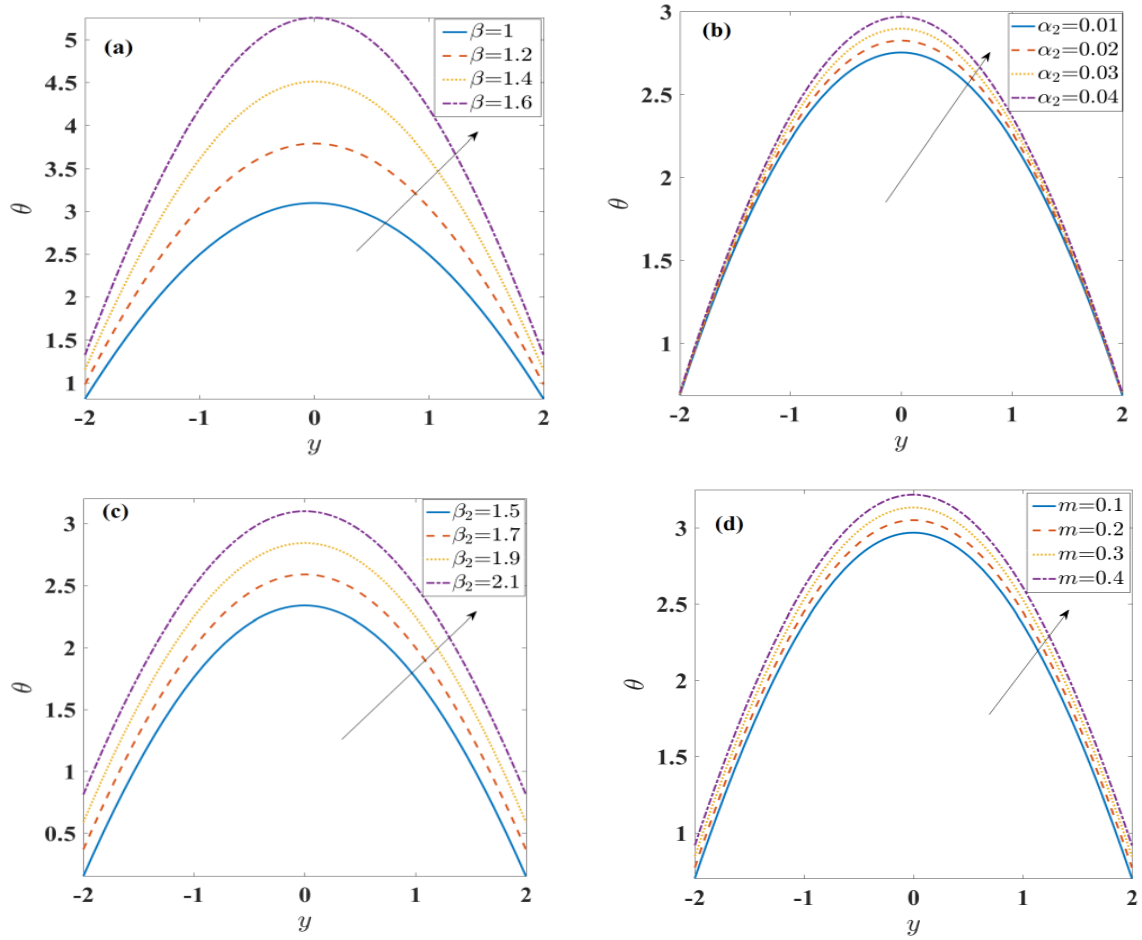
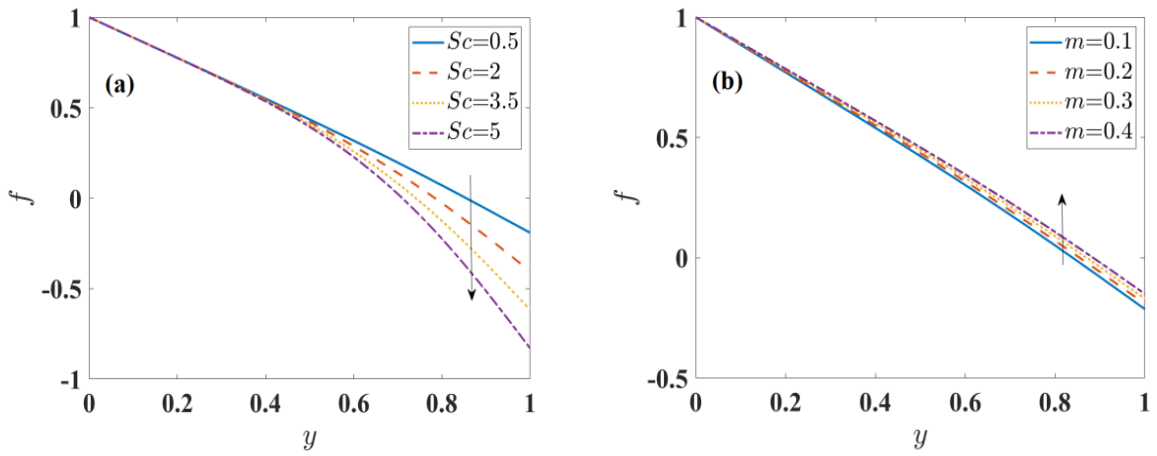


Fig. 3. Temperature profiles for varying (a) β , (b) α_2 , (c) β_2 and (d) m



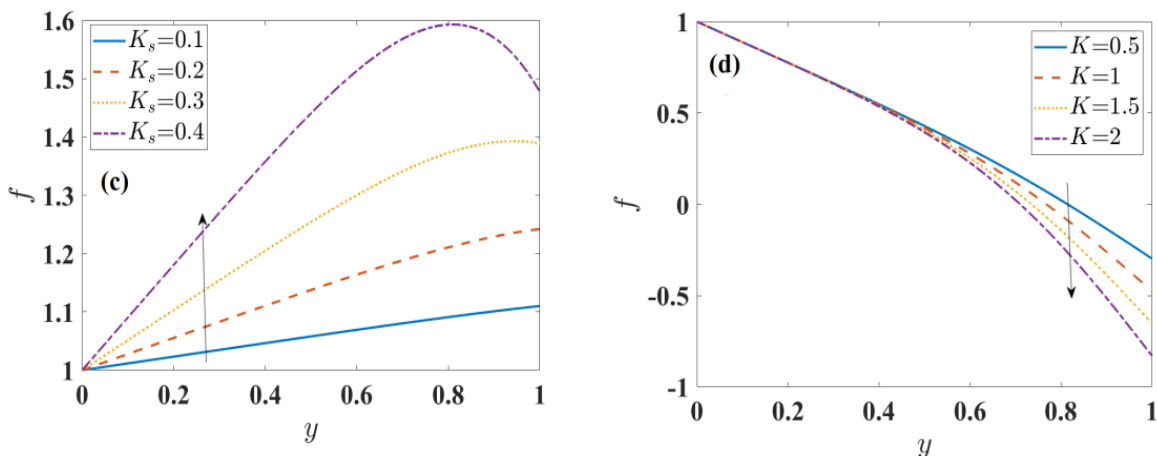


Fig. 4. Concentration profiles for varying (a) Sc , (b) m , (c) K_s and (d) K

4.4 Trapping Phenomenon

Trapping mechanism is an integral part of the peristaltic movement. This phenomenon occurs during peristalsis when few of its streamlines gets closed, resulting in the development of bolus that circulates on the inside and advances with speed of the peristaltic waves. This section attempts to study this interesting phenomenon of trapping through the plots of stream functions. Figure 5 is plotted to study the influence of variable viscosity on the pattern of stream function, in which it can be noticed that α_1 contributes to a decrease in the bolus size. Effects of porous parameter Da is seen to increase the bolus size during peristalsis (see Figure 6). While opposite behavior is seen for velocity slip parameter (Figure 7). A reduction in the bolus size is clearly seen as the value of Grashof number (Gr) increases in Figure 8.

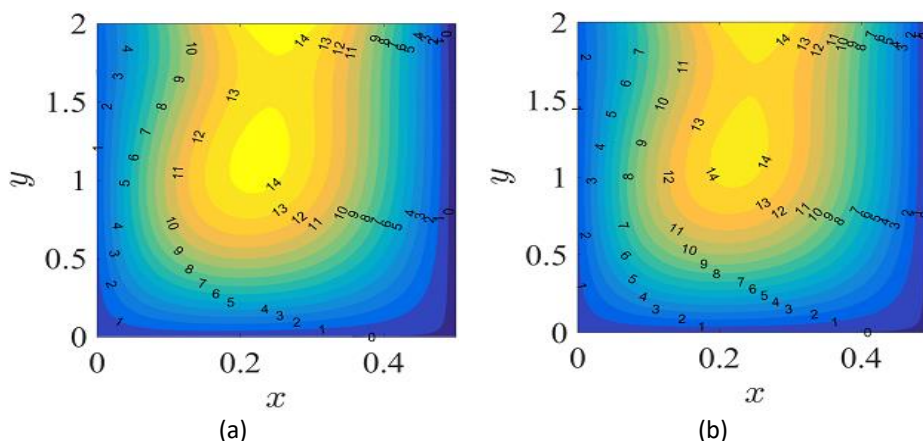


Fig. 5. Streamlines for varying (a) $\alpha_1 = 0.02$ and (b) $\alpha_1 = 0.03$

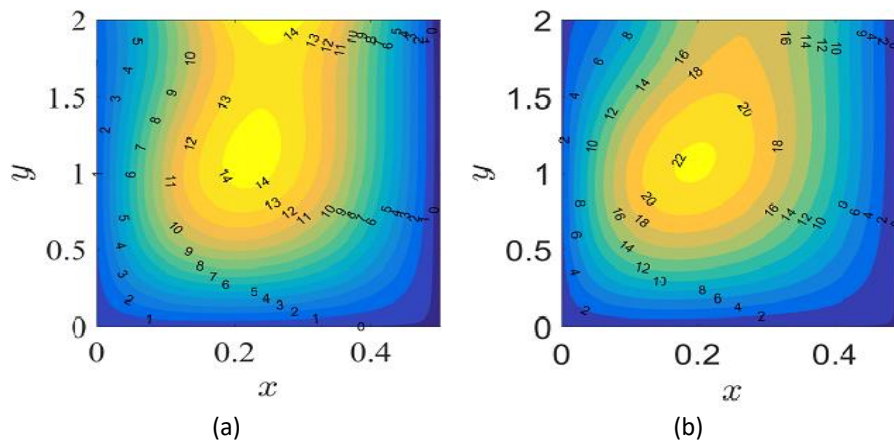


Fig. 6. Streamlines for varying (a) $Da = 0.2$ and (b) $Da = 0.25$

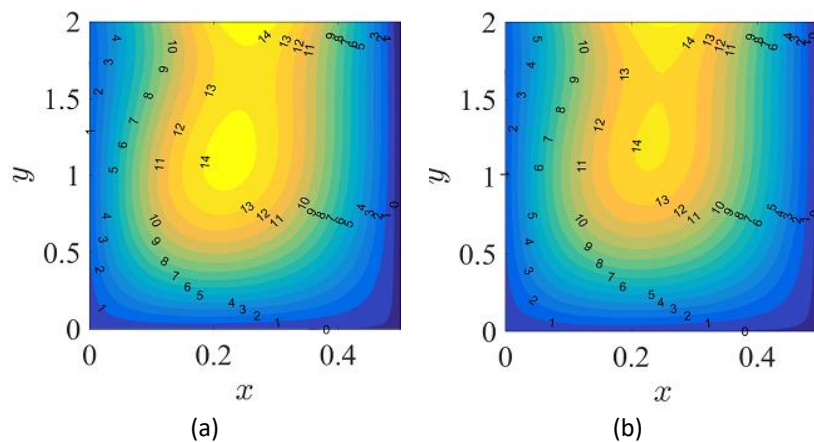


Fig. 7. Streamlines for varying (a) $\beta_1 = 0.1$ and (b) $\beta_1 = 0.15$

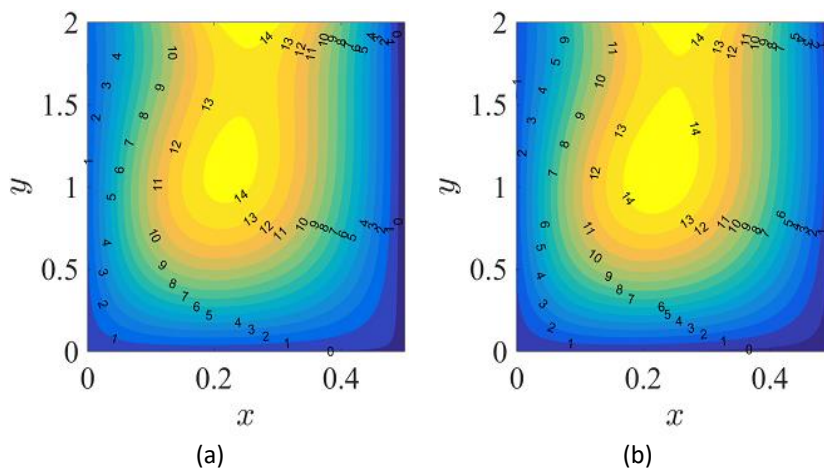


Fig. 8. Streamlines for varying (a) $Gr = 1$ and (b) $Gr = 3$

5. Conclusion

The current model investigates the consolidated impacts of convective boundary conditions and variable fluid properties on the peristaltic component of Bingham liquid in a slanted non-uniform channel. Some considerable findings from the current investigation are:

- Porous parameter aids for enhancing the velocity profiles while the slip parameter diminishes the velocity.

- The variable thermal conductivity and heat generating parameters are increasing function of temperature.
- The wall parameters E_1 and E_2 increases the velocity of the fluid, whereas viscous damping force parameter E_3 reduces the velocity.
- The trapped bolus reduces its volume for higher values of velocity slip parameter and variable viscosity.
- The porous parameter is an aid for increasing the bolus formed during trapping.

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