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Quasi Three-Dimensional Design for a Novel Turbo-Vapor Compressor and the Last Stage of a Low-Pressure Steam Turbine

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ARTICLE INFO	ABSTRACT
Article history: Received 6 May 2021 Received in revised form 22 June 2021 Accepted 3 July 2021 Available online 5 August 2021 Keywords: Freshwater and electricity production; turbo-vapor compressor; low-pressure	Turbo-vapor compressors (TVCs) are used to create a vacuum pressure in the evaporator of a novel combined cycle for electricity and freshwater production were invented. A novel design conceived of a TVC is introduced to increase the efficiency, allowable mass flow rate and reduce costs and losses. The system consists of a single axial compressor rotor followed by a single axial turbine rotor which drives the upstream compressor, allowing high flow rates. A quasi-3D design is carried out for the TVC to calculate the flow velocity components and angles and ensure that the turbo-vapor turbine work is equal to the turbo-vapor compressor work. A preliminary design of the low-pressure power turbine (LPT) is done to examine the size and number of stages. The (LPT) size is twice the size of TVC at typical cycle operating conditions. A three-stage design is the most appropriate choice for the number of stages. It satisfies the accelerating relative flow condition at the last stage over a range of flow coefficients. A quasi-3D design is carried out for the LPT's last stage to ensure a multi-
steam turbine	stage power turbine's safe design.

1. Introduction

There is a significant need for green electricity production due to crude oil and natural gas depletion all over the world, especially Europe [1] and some researches on electricity consumption optimization [2]. There is an immediate need for freshwater production due to water shortages in some regions, such as deserts. Several authors developed methods to produce freshwater from saltwater using solar energy [3, 4]. In contrast, other authors developed new methods for water consumption in agriculture [5]. A novel combined electricity and freshwater production thermal cycle developed by Amin Mobarak [6, 7] can produce a massive amount of fresh water and electricity at a higher efficiency. The novel cycle operates at low temperatures (60–90°C) using water vapor as a working medium under pressure below the atmospheric pressure. This is achieved by a turbo-vapor compressor, TVC (to create negative pressure in the evaporator), a conventional low-pressure water vapor turbine, LPT (to produce electricity), and a condenser working in an open cycle. The current

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work focuses on the quasi 3D design of the turbo-vapor compressor and some preliminary design aspects concerning the low-pressure water vapor turbine.

In this research, a parametric study between the last stage of low-pressure water vapor turbine and turbo-vapor compressor is done to examine the effect of evaporator temperature, rotational speed, and hub flow coefficient ratio $\phi_{h,TVC} / \phi_{h,LPT}$ on the size or diameter ratio $D_{t,LPT} / D_{t,TVC}$. Moreover, the authors proposed a novel TVC design in Patent No. 2020/798 [8] (under review) using a quasi three-dimensional design to obtain the velocity triangles at different spanwise sections. The water vapor properties are estimated at the inlet and exit from the turbo-vapor compressor and at the turbo-vapor turbine's exit. Finally, a preliminary design of the low-pressure water vapor turbine is carried out to minimize the stages. The last stage of the LPT is designed based on the same methodology used in the TVC to ensure that the entire turbine operates efficiently over a wide range of flow coefficients.

2. Selection of Turbo-Vapor Compressor

2.1 Selection of Type and Blade Row of the TVC

The turbo-vapor compressor consists of a water vapor turbine that drives the water vapor compressor to create a suction pressure at the compressor inlet for industrial purposes. The first suggested design can be a centrifugal compressor followed by a centrifugal turbine (e.g., Turbocharger) [9, 10], as shown in Figure 1. The centrifugal compressor consists of an impeller, diffuser ring, and scroll casing. The centrifugal turbine consists of a volute casing, nozzle ring, rotor, and a diffuser. The second suggested design can be an axial compressor stage equipped with a rotor, diffuser, and possibly, inlet guide vanes. The compressor is driven by an axial turbine stage, which comprises a stator, rotor, and possibly, outlet guide vanes.



Fig. 1. Turbocharger [9]

In the present work, a novel design of a turbo-vapor compressor consists of an axial compressor rotor driven by an axial turbine rotor without any stators for the turbine or compressor to avoid extra losses, as shown in Figure 2. The authors propose the design in Patent No. 2020/798 [8]. A starting electric motor is used to start the compressor and turbine by using a clutch coupling between the staring motor and turbo-vapor compressor shafts. After the system reaches a steady state (turbine work equals compressor work), the clutch is decoupled to allow the turbine to run the compressor.



The compressor and turbine are using the same shaft, which means they run at the same speed. Fortunately, the current application requires a small pressure ratio of the order of 1.05. Therefore, a single axial compressor rotor driven by a single axial turbine rotor is the most economical design. Axial compressor design can accommodate more airflow than a centrifugal design of the same size but provides lower pressure ratios. The Turbo-vapor compressor is selected as an axial flow compressor to accommodate the water vapor mass flow rate of 100 kg/sec.



Fig. 2. Turbo-vapor compressor layout [8]

2.2 Selection of LPT to TVC Diameter Ratio

In this Section, the size limits and ratios of the LPT and TVC are examined. Some parameters are tested to determine the size ratio of the LPT to TVC. It is found that the design ratio $D_{t,LPT} / D_{t,TVC}$ should be kept around 2.0 for safe operation [11]. By applying the continuity equation along with the TVC and the LPT in addition to some manipulations, Eq. (1) [12] yields

$$\rho_{TVC} \frac{\pi}{4} D_{t,TVC}^{3} \left(1 - v_{TVC}^{2}\right) v_{TVC} \frac{\pi N_{TVC}}{60} \phi_{h,TVC} = \rho_{LPT} \frac{\pi}{4} D_{t,LPT}^{3} \left(1 - v_{LPT}^{2}\right) v_{LPT} \frac{\pi N_{LPT}}{60} \phi_{h,LPT}$$
(1)

where the axial hub velocity Ca_h is kept constant along with the TVC and LPT. The hub-to-tip diameter ratios v_{TVC} v_{LPT} are set to be 0.5 to account for the worst-case scenario in terms of blade twist and reaction. The hub section is selected as it is the most critical Section in terms of flow deflection. Eq. (1) is used for the following analysis to choose the design diameter ratio $D_{t,LPT} / D_{t,TVC}$ based on some input parameters.

2.2.1 Effect of evaporator temperature

The evaporator temperature on the diameter ratio $D_{t,LPT} / D_{t,TVC}$ is investigated when $N \phi_h v$ held constant for both LPT and TVC. The condenser's exit temperature is roughly constant at 30° C, so the density at the exit from the stage of multi-stage low-pressure water vapor turbine is assumed to be similar to that of the condenser (0.0304 kg/m³). Changing the evaporator temperature from 70° to 90° C will increase $D_{t,LPT} / D_{t,TVC}$ from 1.8 to 2.4, as shown in Figure 3.





Fig. 3. Effect of evaporator temperature on $D_{t,LPT}$ / $D_{t,TVC}$

2.2.2 Effect of TVC rotational speed

The effect of N_{TVC} on $D_{t,LPT} / D_{t,TVC}$ is investigated when evaporator temperature $\phi_h v$ and is held constant for both LPT and TVC. The low-pressure water vapor turbine's rotational speed is also kept constant at 3000 rpm [11]. The turbo-vapor compressor's rotational speed changes from 1500 to 4500 rpm—consequently, the diameter ratio $D_{t,LPT} / D_{t,TVC}$ increases from 1.7 to 2.4, as shown in Figure 4.



2.2.3 Effect of hub flow coefficient ratio

The effect of $\phi_{h,TVC} / \phi_{h,LPT}$ on $D_{t,LPT} / D_{t,TVC}$ is investigated when N and ν for both LPT and TVC, and the evaporator temperature is held constant as the ratio $\phi_{h,TVC} / \phi_{h,LPT}$ changes from 0.7 to 1.3. The diameter ratio $D_{t,LPT} / D_{t,TVC}$ increases from 1.8 to 2.2, as shown in Figure 5.



Fig. 5. Effect of $\phi_{h,TVC}$ / $\phi_{h,LPT}$ on $D_{t,LPT}$ / $D_{t,TVC}$



It is evident from the previous analysis that the LPT diameter is around twice the TVC diameter for an evaporator temperature of 80° C, a condenser temperature of 30° C, $N_{TVC} = N_{LPT} = 3000$ rpm and $\phi_{h,TVC} / \phi_{h,LPT} = 1$.

3. Calculations of TVC Tip and Hub Diameters

The sizing of the tip diameter of the TVC is carried out based on a maximum flow rate of 100 kg/sec, hub-to-tip diameter ratio ranging from ν =0.5 to ν =0.8, and unity ϕ_h [13]. By applying the continuity equation at the inlet of the TVC as well as performing some mathematical manipulations, Eq. (2) yields

$$D_{t}^{3} = \frac{240 \times v_{TVC1} \times \dot{m}_{TVC}}{\pi^{2} \times v (1 - v^{2}) \times \phi_{h} \times N}$$
(2)

where the inlet specific volume v_{TVC1} is the saturated vapor specific volume at 80° C. The absolute inlet velocity is axial (no inlet guide vanes) and is assumed to be constant along the spanwise direction. The rotational speed N is held constant at 3000 rpm. MATLAB R2018a and the function XSteam [14] are used for mathematical calculations and vapor properties calculations.

The first tip diameter is calculated based on a flow rate of 100 kg/s and ν =0.5 from Eq. (2). Afterward, the tip diameter is fixed, and the iteration is applied on Eq. (2) to find the ratio ν for mass flow rates below 100 kg/s with 10 kg/s step. The flow area reduction associated with flow rate reduction leads to an increase in the hub diameter ν . For a mass flow of 70 kg/s, the ratio ν reaches 0.83 (at D_t =1.9452 m), exceeding the upper limit set for that ratio. Therefore, the ratio ν is set back to 0.5 at 70 kg/s. New tip diameter is calculated, and iterations are performed to obtain new ratios ν at flow rates below 70 kg/s while setting the upper limit of 0.8. The procedure is repeated until a mass flow of 10 kg/s is reached, as shown in Table 1. In this study, the mass flow rate of 50 kg/s and a hub-to-tip ratio, ν =0.5, are applied for the TVC design. The static inlet conditions are assumed to be saturated vapor at the evaporator temperature of 80° C.

Table 1				
Summary of TVC sizing results				
$\dot{m}_{_{TVC}}$ (kg/s)	<i>Dt</i> (m)	<i>D_h</i> (m)	V	
10	0.9029	0.4514	0.5000	
20	1.1376	0.5688	0.5000	
30	1.3022	0.6511	0.5000	
40	1.5439	1.2143	0.7865	
50	1.5439	0.7720	0.5000	
60	1.7272	1.3117	0.7594	
70	1.7272	0.8636	0.5000	
80	1.9452	1.5299	0.7865	
90	1.9452	1.4311	0.7357	
100	1.9452	0.9726	0.5000	

4. Velocity Triangles and Shape of blades for the TVC

The hub-to-tip diameter ratio of 0.5 is selected since it is associated with high losses, circulation, and boundary layer problems. If the design is acceptable in this case, it will be adequate for hub-to-tip diameter ratios [13]. Therefore, a mass flow rate of 50 kg/s ensures that the turbo-vapor



compressor operates safely in the most critical conditions. The deceleration rate should be maintained above the limit, $W_2/W_1 \ge 0.72$, to avoid separation [15]. Flow separation occurs when the boundary layer travels far enough against an adverse pressure gradient. The speed of the boundary layer relative to the wall falls almost to zero. The fluid flow becomes detached from the object's surface and takes the forms of eddies and vortices. In aerodynamics, flow separation leads to increased drag, particularly pressure drag, caused by the pressure differential between the object's front and rear surfaces as it travels through the air.

4.1 One-Dimensional Design at the Hub Section

The primary compressor inlet and exit velocity triangles are shown in Figure 6. The axial velocity is assumed to be constant, along with spanwise and streamwise directions. The flow angles are measured from the axial direction. For a mass flow rate of 50 kg/s, inlet temperature = 80° C, N =3000 rpm, ϕ_h =1, D_t =1.5439 m and ν =0.5, velocity components and angles are readily calculated at the inlet. A deceleration ratio is set as 0.85 at the hub to ensure safe diffusion at all spanwise sections. Using the given deceleration ratio and the assumption of constant streamwise axial velocity, all velocity components and angles are calculated at the hub outlet. The stagger angle is assumed to be the arithmetic average of the relative flow angles at the compressor's inlet and outlet. Table 2 (Hub Section column) shows the calculation results in the hub section. The compressor's specific work at the hub is 4895 J/kg, which is assumed to be constant along the span. The hub flow turning, which is the maximum turning along the span, is 11.3°. This means that there is no risk of boundary layer separation at the suction surface of compressor blades. Figure 8 (a) shows the velocity triangles and shape of blades at the compressor inlet at the hub (first two triangles from left).



Fig. 6. Basic compressor velocity triangle

Calculated compressor velocities and angles at three different sections	Table 2
	Calculated compressor velocities and angles at three different section

	Hub section	Mean section	Tip section	
D (m)	0.7720	1.1579	1.5439	
U (m/s)	121.2597	181.8896	242.5194	
C1=Ca (m/s)		121.2597		
W1 (m/s)	171.4871	218.6041	271.1450	
β1(degree)	45.000	56.3099	63.4349	
W2 (m/s)	145.7641	196.7782	253.2521	
Wu₂(m/s)	80.8903	154.9766	222.3347	
Cu₂ (m/s)	40.3694	26.9129	20.1847	
β₂(degree)	33.7066	51.9590	61.3923	
Work (J/kg)	4895.1811			
Stagger, γ (degree)	39.3533	54.1345	62.4136	
Turning, ϑ (degree)	11.2934	4.3509	2.0427	



4.2 Quasi Three-Dimensional Design at the Tip and Mean Sections (Based on Simple Free Vortex Design)

Assuming free vortex design, work and axial velocity are constant along span [13]. The inlet velocity diagram can be calculated at any spanwise section given that inlet axial velocity, which is constant, and blade speed are known at any section. The exit velocity diagram can be obtained at any section, given that the spanwise work and axial velocity are constant at all sections. Table 2 (Mean and Tip Sections) lists the velocity components and angles at the mean and tip sections. Again, the stagger is assumed to be the arithmetic average of the inlet and outlet relative flow angles. Figure 7 (Left) shows the compressor blade's preliminary stacked profiles at the three main sections based on the NACA65 series profile. The velocity triangles along with the shape of blades at mean and tip sections are shown in the first and second diagrams of Figure 8 (b, c)

5. Calculations for Turbo-Vapor Turbine

Table 2

The Turbo-vapor turbine has the same hub, mean and tip diameters calculated from the compressor at 50 kg/s and the same rotational speed. The specific work of the turbo-vapor turbine is assumed to be equal to that of the turbo-vapor compressor. The axial flow velocity is considered to be constant along the streamwise and spanwise direction. The turbine-specific work is also constant along the spanwise constant based on free vortex design. It is noted that the stagger and turning angles are identical to those of the compressor due to the assumption of constant work and axial velocity. The turbine exit velocities and angles are similar to those of the compressor inlet, as shown in Table 3. Figure 7 (right) shows the stacked turbine profiles at the main three sections. Figure 8 (third column of diagrams) shows the turbine exit velocity diagrams. The absolute exit velocity is axial to avoid the installation of outlet guide vanes.

lable 5				
Calculated TVC turbine velocities and angles at three different sections				
	Hub section	Mean section	Tip section	
D (m)	0.7720	1.1579	1.5439	
U(m/s)	121.2597	181.8896	242.5194	
C₃=Ca (m/s)		121.2597		
W₃ (m/s)	171.4871	218.6041	271.1450	
β₃(degree)	45.000	56.3099	63.4349	
Work (J/kg)		4895.1811		
Stagger, γ (degree)	39.3533	54.1345	62.4136	
Turning, ϑ (degree)	11.2934	4.3509	2.0427	

6. Calculations of Water Vapor Properties Across Turbo-Vapor Compressor

At the inlet to the axial compressor, the static temperature of water vapor is 80° C. The static inlet conditions are assumed to be saturated vapor. To find the outlet conditions, the compressor and turbine total-to-total efficiencies are considered to be 0.92 and 0.94, respectively. The water vapor properties are calculated using the MATLAB function XSteam [14]. Figure 9 shows the calculations flow chart. Table 4 shows the output values of the water vapor properties across the TVC.





Fig. 7. Stacked profiles at hub, mean, and tip of axial turbo-vapor compressor and turbine



Fig. 8. Velocity triangles and shape of blades at (a) Hub section, (b) Mean section, and (c) Tip section across the axial turbo-vapor

$$t_{1} = t_{Sat,Vap.} \rightarrow p_{1}, h_{1}, s_{o1}, \upsilon_{1}$$

$$C_{1} = Ca, h_{1} \rightarrow h_{o1}$$

$$h_{o1}, s_{o1} \rightarrow p_{o1}, t_{o1}$$

$$work, h_{o1} \rightarrow h_{o2}$$

$$h_{o1}, h_{o2}, \eta_{u,C} \rightarrow h_{o2s}$$

$$h_{o2s}, s_{o1} \rightarrow p_{o2}$$

$$p_{o2}, h_{o2} \rightarrow s_{o2}, t_{o2}$$

$$h_{o2}, C_{2} \rightarrow h_{2}$$

$$h_{2}, s_{o2} \rightarrow p_{2}, t_{2}$$

$$p_{2}, s_{o2} \rightarrow \upsilon_{2}$$

$$h_{o3}, \eta_{u,T} \rightarrow h_{o3s}$$

$$h_{o3s}, s_{o2} \rightarrow p_{o3}$$

$$p_{o3}, h_{o3} \rightarrow s_{o3}, t_{o3}$$

$$h_{o3}, C_{3} \rightarrow h_{3}$$

$$h_{3}, s_{o3} \rightarrow \upsilon_{3}$$

Fig. 9. Procedures of properties calculations across the TVC



Table 4

Water vapor properties across turbo-vapor compressor			
Properties	perties Compressor Inlet Compressor Exit Tur		Turbine Exit
t₀ (°C)	83.8501	86.4043	83.8324
p₀ (bar)	0.4961	0.5099	0.4940
h₀ (kJ/kg)	2650.367	2655.2615	2650.37
s₀ (kJ/kg.K)	7.6110	7.6121	7.6130
t (°C)	80.0000	82.1277	79.9851
p (bar)	0.4741	0.4851	0.4721
h (kJ/kg)	2643.01	2647.0946	2643.01
υ (m³/kg)	3.4053	3.3412	3.4202

7. Multi-Stage Low-Pressure Water Vapor Turbine Design

7.1 Multi-Stage Low-Pressure Water Vapor Turbine Preliminary Calculations

The inlet and exit conditions of the LPT should be known for the calculation procedures. The LPT's inlet conditions are assumed to be the same as the turbo-vapor turbine's exit conditions listed in Table 4. The LPT's exit pressure is considered to be related to the condenser saturated pressure at 30° C through the static pressure recovery coefficient. A diverging duct is placed between the LPT exit and the condenser inlet. The LPT's total-to-total efficiency is assumed to be 0.9 [16], and the pressure recovery coefficient is considered to be 0.12 [17]. The pressure recovery coefficient is given by Eq. (3)

$$C_{p} = \frac{p_{cond} - p_{4}}{0.5(\rho C a^{2})_{4}}$$
(3)

 p_{cond} The saturation pressure at 30° C and subscript 4 represent the conditions at the low-pressure turbine's exit. The LPT is designed at 3000 rpm, 50 kg/s (same as TVC), and a range of flow coefficient, $\phi_h = 0.8$ to $\phi_h = 1.2$. Again, the axial velocity is assumed to be constant along the spanwise direction. The hub-to-tip diameter ratio $_{v}$ is assumed to be 0.5. Since the exit density or specific volume is not explicitly defined, an exit density and total-to-static efficiency are assumed. An iterative process is applied until the solution converges to the correct specific volume and targets total-to-total efficiency, as shown in Figure 10.

It should be noted that subscript 3 denotes the LPT inlet condition, which is identical to the TVC exit condition and subscript 4 represents the LPT exit condition. Table 5 lists some of the exit conditions at different flow coefficients. The total-to-static efficiency is lower at higher flow coefficients since it is associated with higher exit kinetic energy loss.

7.2 Preliminary Design of the Number of Stages and The Last Stage of the LPT

It is vital to determine the number of stages and the design of the last stage of turbines for sizing and economic reasons. The most economical choice is, of course, a single-stage design. However, a check should be performed on the acceleration ratio of the relative velocity across the turbine blades to ensure $W_2 > W_1$. A series of trials to check the effect of the number of stages are performed, but the details are not listed in this paper.

The inlet and exit of the last stage will be denoted by 1 and 2, respectively. The inlet velocity diagram is calculated from work and assuming a constant streamwise axial velocity. The blade speed is already known in all sections from the procedures listed in Figure 10. The absolute exit velocity is



considered to be purely axial. The inlet and exit velocity diagrams are fully defined. The hub section is the Section of interest since it shows the worst acceleration ratios and highest flow turning.



Fig. 10. Procedures of properties calculations across the LPT

The single-stage design gives $W_{2h} < W_{1h}$, which is inappropriate for turbines. For multi-stage designs, an equal specific work per stage is assumed. The two-stage design also gives decelerating relative flow ($W_{2h} < W_{1h}$) at all flow coefficients, which should be avoided. A three-stage design gives $W_{2h} > W_{1h}$ at all flow coefficients. This is the most reliable and economical choice for the given conditions. Table 6 lists the acceleration ratio and turns for the LPT's last stage based on a three-stage design. Figure 11 shows the velocity diagram at the hub, mean, and tip sections based on the free vortex design at $\phi_h = 1.2$. The procedures of calculating the velocity diagrams for the LPT are the same as those for the TVC. Figure 12 depicts the LPT expansion process and a close-up of the TVC compression and expansion processes on the h-s diagram. Figure 13 shows a schematic drawing of the three-stage LPT and the upstream TVC, and the starting motor. All components utilize the same shaft and hence, the same rpm.



Table 5

Multi-stage low-pressure turbine calculations results for three-stage de	esign
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$oldsymbol{\phi}_h$	0.8	1.0	1.2
D _h (m)	1.7266	1.6064	1.5152
D _t (m)	3.4532	3.2127	3.0304
υ₄(m³/kg)	30.4809	30.6819	30.8990
P ₀₄ (bar)	0.0499	0.0529	0.0562
Ca _h (m/s)	216.9713	252.3250	285.6069
Total Work (kJ/kg)	295.8470	289.3446	282.3160
$\eta_{\scriptscriptstyle ts,LPT}$ %	84.0691	81.9978	79.7734

Table 6

Calculations of the last stage of the multi-stage low-pressure turbine for three-stage design

ϕ_h	0.8	1.0	1.2
Stage Work (kJ/kg)	98.6157	96.4482	94.1053
α_1	59.1747	56.5702	54.1579
W1h (m/s)	235.8245	283.8050	326.1003
W2h (m/s)	347.3235	356.8415	371.7769
W_{2h}/W_{1h}	1.4728	1.2573	1.1401
Turning, ϑհ (degree)	74.4062	72.2423	68.6628



Fig. 11. Velocity triangles of the last stage of the lowpressure water vapor turbine at ϕ_h =1.2 for threestage design at (a) Hub, (b) Mean, and (c) Tip sections



Fig. 12. Enthalpy-entropy diagram for the processes of the TVC and LPT





Fig. 13. A schematic drawing of the TVC and LPT

8. Conclusions

A preliminary design for some components of a novel freshwater and electricity production thermal cycle was carried out. This paper discussed the design of a novel TVC and a preliminary design of the low-pressure steam turbine. For typical operating conditions (evaporator temperature of 80°C, 3000 rpm, unity hub flow coefficient), the diameter of the last stage of the LPT should be twice that of the TVC. The mass flow rate was selected to be 50 kg/s to ensure safe design at a hub-to-tip ratio equals to 0.5. The novel TVC comprises an axial compressor rotor followed by an axial turbine rotor is proposed to reduce losses. A quasi 3D design was applied to ensure equal work for the compressor and turbine at all spanwise sections. For the low-pressure steam turbine running at 50 kg/s, an equal work per stage was assumed to find the most appropriate and economical number of stages. A three-stage design was selected to satisfy an accelerating relative flow condition across the last stage at all spanwise sections and over a range of hub flow coefficients from 0.8 to 1.2. While the total-to-static efficiency is higher at $\phi_h = 0.8$ by 5.7%, the size of LPT is larger by 13.3% compared with $\phi_h = 1.2$, which means higher manufacturing costs lower flow coefficient designs.

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