

The Effects of Pressure and Temperature on Flame Characteristics of Crude Palm Oil Combustion

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ARTICLE INFO	ABSTRACT
Article history: Received 3 April 2022 Received in revised form 11 July 2022 Accepted 24 July 2022 Available online 18 August 2022	Using vegetable oil as a direct combustion fuel is an interesting energy development of lower emissions fuel. In this work, commercial cooking oil extracted from palm oil was burned using a typical nozzle having a diameter of 2 mm. Nozzle gage pressure and preheat temperature of palm oil were varied at 20, 40, 60 psi and 70, 90, 110 °C, respectively. Combustion oxidizer was air at room temperature. Equivalence ratio of ER= 1.1. To initiate combustion of the oil, a pilot flame from LPG with fixed firing rate was placed under the oil spray using a domestic stove. The experimental results shown that higher preheat temperatures and pressure accelerated combustion reactions of
Keywords:	palm oil. The simulation also shown the same result as the experimental results. The
Crude palm oil; direct combustion; combustion characteristics; flame	higher preheat temperature and pressure led to high temperature, large size and long penetration of flame. The largest flame size was at 110 °C and 60 psi.

1. Introduction

Since the Industrial revolution, the energy mix of most countries across the world has become dominated by fossil fuels. The global greenhouse gas emissions 75% result from the burning of fossil fuels that are responsible for large amounts of air pollution and a health problem which leads to at least 5 million deaths each year. To reduce CO₂ emissions and air pollution, the world needs to rapidly shift towards low-carbon sources of energy – renewable energy [1-4].

Biomass energy, one of renewable energy sources, has played a significant role because it offers environmental and social benefits. Moreover, it can be converted into electricity and heat by the most common technique that is called direct combustion [5-7] and become a vital part of the global energy mix and account for an ever-growing share of electric capacity added worldwide [8].

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Several biofuels have been studied to solve emission problems. Hashimoto *et al.*, [9] studied the combustion characteristics compared 100% C-heavy oil with 50% C-heavy oil-crude jatropha oil (CJO) blending. The result shows that NO_x and SO₂ emissions of C-heavy oil-CJO blending were greatly decreased because the nitrogen and sulfur contents in CJO were significantly lower than C-heavy oil. Mahfouz *et al.*, [10] studied the effects of waste cooking - diesel oil blending: 0, 20, 40, 60, 80 and 100% on performance, emissions, and combustion characteristics of industrial oil burner. It was found that NO_x, SO₂ and CO emissions decrease when percentage volume of waste cooking oil increases. Muhammad *et al.*, [11] studied performance of sludge palm oil (SPO) combustion using waste oil burner compared with diesel. SPO was lower in CO, CO₂ and NO_x emissions during the combustion compared to diesel around 34%, 6% and 90 % reduction respectively.

According to some researcher, the results show that vegetable oil released fewer emissions compared with other oil, and blending fuel was less in emissions as well. So, this study focuses on using palm oil which is a high commercial value products in Southeast Asia.

Considering in Southeast Asia, palm oil production is estimated at 72.26 million ton in 2019. Indonesia is expected to produce the biggest share at 40.50 million ton, followed by Malaysia at 20.50 million ton. The two countries account for 84.4% of global production. Thailand ranks third, producing 2.90 million ton a year or 4% of global output [12-15].

According to the US Department of Agriculture data (USDA, 2020), in average, the palm oil harvested areas in Southeast Asia had grown a lot and led to a huge increase in palm oil production in the year 2018-2019 [16]. Due to the oversupply of palm oil, the market price of crude palm oil (CPO) went to a historic low. The governments try to lift the price up by using policies such as biodiesel and fuel in co-firing process [17].

Producing biodiesel from palm oil requires a great number of materials and energy. During the production process, several kinds of emissions are released and affect the environment [18]. Therefore, using crude palm oil as fuel for direct combustion such as in a boiler or industrial cooking process is another interesting development. It is not only to decrease emissions but also a way to help palm farmers.

This study focuses on using palm oil as fuel for direct combustion. Experiment and simulation of palm oil-air combustion were studied. An experiment attempts to investigate flame characteristics. Before entering a combustion chamber, palm oil is preheated 70, 90 and 110 °C with varied air pressure 20, 40 and 60 psi. Pilot flame is used for initial ignition of the fuel-air mixture. Flue gas analyzer, TESTO 350, is used to measure exhaust gas components. The simulation approach used to compare flame characteristics results and study additional result due to an experiment limitation. Computational fluid dynamics (CFD) ANSYS Fluent software is applied to investigate palm oil combustion simulation with same preheat temperature and air pressure conditions.

2. Methodology

2.1 Modelling

In this study, Computational fluid dynamics (CFD) ANSYS Fluent 2019 R3 software is used. Design modelling as shown in Figure 1. A 2 mm-diameter nozzle in the centre of a combustion chamber is used to introduces palm oil. Palm oil enters a combustion chamber with varied preheat temperature 70, 90 and 110 °C at 0.66 m/s. Ambient air enters a combustion chamber at 0.005 m/s. The overall equivalence ratio is 1.1.



Fig. 1. Design Modelling

2.2 Mesh

Grid generation is shown in Figure 2. The grid-dependent test was varied in the element number of 5,000 – 15,000 elements. It was found that the saturated elements which were not changing the results significantly were 12,000 elements. These element numbers were selected to apply to all CFD runs.



Fig. 2. Meshing

2.3 Solution Setup

Table 1 shows general and model setting. Palm oil-air combustion model was studied in axisymmetric 2D-space with energy equation and standard k-epsilon (2eqn). To simplify combustion investigation, the palm oil was given as gas phase. Species transport model was chosen to induce fuel to model. Table 2 shows boundary condition for fuel inlet and air inlet.

Table 1				
General and model setting				
Property	Value			
2D space	Axisymmetric			
Energy equation	On			
Viscous	k-epsilon (2eqn)			
Species	Species transport			
Reactions	Volumetric			
Mixture material	Palm oil-Air			
Turbulence-chemistry Interactio	Eddy-Dissipation			
Table 2				
Boundary condition				
Condition	Fuel inlet	Air inlet		
Diameter (m)	0.002	0.4		
Velocity (m/s)	0.66	0.005		
Temperature (°C)	70, 90, 110	26.85		
Materials	Palm oil	Air		

Table 3 shows palm oil ultimate analysis. The palm oil sample was tested at Office of Scientific Instrument and Testing (OSIT), Prince of Songkla University (PSU), Thailand. CHNS/O Analyzer (Thermo Quest, FlashEA 2000 model, Italy) is used for analyzing the elements C, H, N, S and O in samples by the method of burning samples at high temperature into mixture gas. Then, enter the column to separate and measure the number of elements in the sample. Table 4 shows palm oil property, chemical formula, MW, density, etc., to study palm oil-air combustion [18]. To check convergence of results, define all absolute criteria in residual monitors 0.0001 and run calculation with number of Iteration 100000.

Table	e 3						
Palm oil ultimate analysis							
Samp	ole	Unit	С	Н	0	Ν	
Palm	oil	%wt	75.625±0.204	11.775±0.037	12.581±0.07	0 0.021±0.001	
-	Table	4					
	Palm oil property [19]						
	Property			70 °C	90 °C	110 °C	
	Chemical formula			$C_{48}H_{90}O_6$	$C_{48}H_{90}O_6$	C ₄₈ H ₉₀ O ₆	
	MW (kg/kmol)			744.38	744.38	744.38	
	Density (kg/m³)		865.4	856.1	847.1		
	Cp (j/kg·K)		1988	2049	2113		
	Thermal cond. (w/m·k)			0.1683	0.1668	0.1653	
Viscosity (kg/m·s)		0.01275	0.008087	0.005709			

2.4 Experimental Setup

An experimental set up as shown in Figure 3. The fuel supply system is included of main tank for feeding fuel via a rotameter to control fuel flow rate. Then, heater with temperature controller is used to preheat palm oil 70, 90 and 110 °C. The air supply system consisted of air compressor, pressure regulator and an air rotameter to provide air with pressure 20, 40 and 60 psi. Palm oil and air enter a combustion chamber through 2-mm diameter nozzle. Pilot flame is used for initial ignition of the fuel-air mixture during start-up of combustion reaction. Flue gas analyzer, TESTO 350, is used to measure exhaust gas components in this experiment as shown in table 5.



Fig. 3. An Experimental set up

Table 5						
TESTO350 exhaust gas measurement [20]						
Param	eter	Accuracy				
O ₂	(0 to 25 vol.%)	± 0.8 vol.%				
CO_2	(0 to 50 vol.%)	± 0.3 vol.%				
CO	(0 to 10,000 ppm)	± 10 ppm				
NO	(0 - 4 <i>,</i> 000 ppm)	± 5 ppm				
NO_2	(0 - 500 ppm)	± 5 ppm				
SO ₂	(0 - 5,000 ppm)	± 5 ppm				

3. Results

3.1 Flame Characteristics

Figure 4 shows the largest flame size was at preheat temperature 110 °C and pressure 60 psi. The higher preheat temperature and pressure can accelerate combustion reactions.



Fig. 4. Flame characteristics (experimental results)

Figure 5 shows the highest temperature was at preheat temperature 110 °C and pressure 60 psi. High temperature areas of the flame of CFD results (Figure 5) were similar to the flame size of experimental results (Figure 4). The higher preheat temperature and pressure led to high temperature, large flame size and long penetration of flame.



Fig. 5. Flame characteristics (CFD results)

3.2 Temperature Graph

The temperature along chamber length from an inlet increases rapidly and then begins to drop to the end of the chamber (185 cm). Figure 6(a) constant preheat temperature with varied pressure, the temperature start dropping at 60 cm. The highest temperature is at 60 psi and followed by 40 and 20 psi respectively. Figure 6(b) the highest temperature is at a chamber length 80, 90 and 100 cm for pressure condition 20, 40 and 60 psi respectively.



Fig. 6. Temperature graph along a combustion chamber length (a) constant preheat temperature, varied pressure, (b) constant pressure, varied preheat temperature (CFD results)

3.3 Palm Oil Graph

Considering Figure 7, palm oil is a reactant that used in combustion reaction. Therefore, palm oil mass fraction decreases rapidly and become 0 at a chamber length 100-120 cm. The higher preheat

1.00 1.00 Const. preheat temp. 70 °C Const. pressure 20 psi 0.80 0.60 0.40 0.40 0.20 0.80 0.80 C48H90O6 Mass Fraction 0.60 20 psi 70 °C 0.40 **-** 40 psi - 90 °C ••••• 110 °C ••••• 60 psi 0.20 0.20 0.00 0.00 0 20 40 60 80 100 120 140 160 180 0 20 40 60 80 100 120 140 160 180 X (cm) X (cm) 1.00 1.00 Const. pressure 40 psi Const. preheat temp. 90 °C 0.80 0.80 C48H90O6 Mass Fraction C48H90O6 Mass Fraction 0.60 0.60 •70 °C 20 psi 0.40 0.40 - 90 °C **-** 40 psi •••• 60 psi •• 110 °C 0.20 0.20 0.00 0.00 0 20 40 60 80 100 120 140 160 180 0 20 40 60 80 100 120 140 160 180 X (cm) X (cm) 1.00 1.00 Const. preheat temp. 110 °C Const. pressure 60 psi 0.80 **C⁴⁸H³⁰O**⁶ Wass Fraction 0.40 0.40 0.80 C48H90O6 Mass Fraction 0.60

temperature, the faster palm oil mass fraction decreases as shown in Figure 7(a). For constant pressure varied preheat temperature, all the conditions show similar results as shown in Figure 7(b).

(a) (b) Fig. 7. Palm oil mass fraction along a combustion chamber length (a) constant preheat temperature varied pressure, (b) constant pressure varied preheat temperature (CFD results)

180

0.20

0.00 0

20

40

60

80

100

X (cm)

120

140

20 psi

– 40 psi •••• 60 ps

160

140

3.4 O₂ Graph

0.40

0.20

0.00

0

20

40

60

80

100

X (cm)

120

Considering Figure 8, O₂ is also a reactant that used in combustion reaction. When combustion reaction occurs, O₂ mass fraction increases slightly due to excess air in a chamber. Then, O₂ mass fraction rises rapidly at a chamber length 100-120 cm because there is not enough palm oil. So, air that enters a chamber is excess air.

70 °C

- 90 °C

•• 110 °C

160

180



Fig. 8. O₂ mass fraction along a combustion chamber length (a) constant preheat temperature varied pressure, (b) constant pressure varied preheat temperature (CFD results)

3.5 CO₂ Graph

Considering Figure 9, CO_2 mass fraction increases rapidly at a chamber length from an inlet to 40 cm because C is converted into CO_2 and CO, an increase in CO_2 showed better combustion and lower in CO. Then, CO_2 mass fraction keeps increasing slightly and starts to fall at a chamber length 100-120 cm due to no combustion reaction. Referring to Figure 7 palm oil mass fraction becomes 0 at 100-120 cm. So, there is no reactant to continue combustion reaction.

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Fig. 9. CO₂ mass fraction along a combustion chamber length (a) constant preheat temperature varied pressure, (b) constant pressure varied preheat temperature (CFD results)

4. Conclusion

This study focused on Palm oil-air combustion with species transport and compared with experimental results. The flam characteristics of simulation results were similar to the experimental results. The higher preheat temperature and pressure led to high temperature, large size and long penetration of flame. Moreover, the simulation results shown that the higher preheat temperature and pressure can accelerate combustion reaction. Temperature along a chamber length become higher and palm oil mass fraction decreases faster when palm oil-air combustion in high preheat temperature and pressure and pressure condition.

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