

Performance Analysis of Corrugated Twisted Tape Inserts for Heat Transfer Augmentation

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1. Introduction

Enhancing heat transfer within a duct can be achieved through passive methods, including the use of various rib patterns, indented surfaces, and pin-like protrusions. These techniques are applied in combustion chamber linings, cooling internal turbine blades, solar air heaters, electronic cooling systems, medical equipment, and industrial heat exchangers. Dimpled surfaces are currently favored due to their ability to significantly increase heat transfer rates with minimal

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pressure impact. Researchers have explored combining these techniques to further enhance heat transfer efficiency. Extensive literature covers how different parameters of dimples affect heat transfer. The Russian Aerodynamic Society uses dimpled surfaces not only to reduce drag but also to enhance heat transfer. They utilize configurations such as regular arrays of dimples, staggered arrays in annular passages, flow through converging and diverging ducts with a single hemispherical dimple, and narrow ducts with spherical dimples variably positioned on opposing walls. Some studies report up to 150% higher heat transfer compared to flat plates, with a relatively minor pressure increase. Recent research shows heat transfer improvements up to 2.5 times greater than smooth plates across various Reynolds numbers, with a pressure penalty roughly half that of ribbed turbulators. Kurhade *et al.,* [1-4] discussed material selections and computational fluid dynamics (CFD) approaches for thermal cooling, while Patil *et al.,* [5], and Waware *et al.,* [6] provided critical reviews on heat transfer enhancement in heat exchangers. Khot Rahul *et al.,* [7-11] investigated laser welding parameters on the strength of TRIP steel. The present study focuses on enhancing heat transfer using wavy corrugated twisted tape inserts. Luo *et al.,* [12] used three methods—air bubble injection, perforated wavy strip turbulator (PWST), and nanofluids—to enhance thermal performance in a double pipe heat exchanger. Results indicated heat transfer increases of 56% with nanofluids, 53% with PWST, and 14.1% with bubble injection. Combining all three methods boosted heat transfer and exergy losses by 2.15 and 1.82 times, respectively, compared to a plain pipe. Kumar *et al.,* [13] presented experimental analyses on a heat exchanger tube using a newly designed perforated conical ring combined with twisted tape inserts. Aldawi [14] explored the use of twisted tapes in spiral tubes to address significant research gaps, employing a validated mathematical model to understand geometric parameters' effects on heat transfer and exergy efficiency in such configurations. Ahmad *et al.,* [15] found that corrugated geometries exhibit a performance evaluation criterion (PEC) greater than unity, surpassing smooth pipes. Experiments by Afanasyev *et al.,* [16] analyzed friction and heat transfer on surfaces with spherical cavities exposed to turbulent flow, using an aerodynamic test bed to study boundary layer conditions. Bunker and Donnellan [17] demonstrated that heat transfer in circular passages with dimpled surfaces can be enhanced by factors exceeding 2 when the dimple depth is greater than 0.3 and the array density is 0.5 or higher, resulting in friction factor multipliers between 4 and 6. This research provides initial insights into the effects of different concave arrays on heat transfer and friction in turbulent flows. Chyu *et al.,* [18] showed that concave configurations enhance heat transfer approximately 2.5 times more than smooth surfaces for Reynolds numbers between 10,000 and 50,000, comparable to continuous ribbed turbulators, with significantly lower pressure losses, nearly half of those caused by protruding elements. Isaev *et al.,* [19] demonstrated that altering the separation flow structure from symmetric to a single vortex significantly boosts heat transfer, increasing approximately 60% in the region of the spherical dimple and about 45% in its wake. Ligrani *et al.,* [20] presented flow structure characteristics for a channel with a dimpled surface on one wall, both with and without protrusions on the opposite wall. Moon *et al.,* [21] showed that heat transfer enhancement and pressure penalties remain consistent across a wide range of Reynolds numbers and duct heights. Mahmood *et al.,* [22] examined mechanisms for enhancing heat transfer on plain duct surfaces with dimples on one wall, where the duct height was 50% of the dimple print diameter. Syred *et al.,* [23] studied turbulent heat transfer and hydrodynamics in concavely and convexly curved dimples with Reynolds numbers ranging from 1.3 x 10⁵ to 3.1 x 10⁵. Mohadjer *et al.,* [24] showed that the PEC value was increased by only 6.3 %, some of the turbulators reduced this parameter by up to 11.8 %, which is more severe. The worst performance was observed with the Case C (three-bladed) turbulator at a PR value of 11, which reduced the PEC by 11.8 %. Abed *et al.,* [25] suggest that by incorporating bubble injection, adopting the

magnetic turbulator, and simultaneously utilizing both methods, there is a significant improvement in heat transfer. Kumar *et al.,* [26] examines the efficiency of a solar thermal air collector called a jet impingement solar thermal air collector (JISTAC) that is fitted with discrete multi-arc-shaped ribs (DMASRs) utilizing soft computing techniques. Ng and Alzakri [27] numerically investigate the thermal performance of laminar flow inside a pipe with a newly designed small twisted tape insert, showing a Nusselt number increase of approximately 0.07-42.7% for the three-small tapes design and 4.7-48.0% for the five-small tapes design compared to a plain twisted tape insert.

Engineers are looking for new ways to improve heat transfer in machines using magnets, like in car engines and refrigerators. Even though there's been a lot of research on improving heat transfer in double pipe heat exchangers with different methods, scientists haven't looked much at how wavy corrugated twisted tape inserts specifically affect how well heat transfers. Most studies focus on plain twisted tapes or other inserts that make the flow more turbulent. So, we don't really understand how the wavy bumps and twists of these special tapes affect heat transfer and pressure changes in turbulent flow. This research aims to fill this gap by thoroughly examining how these inserts perform.

2. Experimental Investigations

2.1 Set Up

Figure 1 and its inset illustrate the layout of the experiment, including the measuring tools used. The key component was a heat exchanger with a copper inner tube and a mild steel outer tube. We used thermocouples to track temperature changes in both the hot and cold water entering and exiting the exchanger. Four thermocouples were used in total: one for each inlet and outlet of both hot and cold water streams. Rotameters measured the flow rate of the water entering the hot and cold sides. Two pumps kept the water circulating, and separate tanks stored the hot and cold water. The hot water tank had a 1500-watt electric heater. A U-shaped manometer measured the pressure difference between the hot water inlet and outlet, while a current meter measured the flow velocity inside the test section. Control valves and bypass valves allowed for adjusting the flow at the inlet of each rotameter. An airflow meter with a restriction (orifice meter) is used to measure how much air is passing through. A valve allows researchers to control the flow rate. They used two temperature sensors (thermocouples) to measure the incoming air temperature and three to measure the outgoing air temperature.

2.2 Method

The experiment began by filling the tank with cold water and heating it to 80°C using a heater. Then, a pump and a valve were used to turn on the flow of hot water through a rotameter and into the inner pipe of the heat exchanger. At the same time, cold water from a separate tank was pumped and controlled by a valve to flow through a rotameter and into the outer pipe of the heat exchanger. The cold water flow rate was set to 100 liters per hour (LPH) and held constant throughout the experiment. The hot water flow rate was set to 350 LPH at first. Once the system reached a stable state (steady state), researchers recorded the inlet and outlet temperatures of both the hot and cold water. They also measured the pressure difference across the test section for a plain tube without any inserts. This process was then repeated using three different wavy twisted tapes inserted into the tube. Each tape had a different twist ratio (TR) of 5.2, 4.2, or 3.2 as shown in Table 1. The hot water flow rate was also varied during these tests, ranging from 350 LPH to 850 LPH.

The instruments used, provide accurate measurements within specified ranges, crucial for detailed performance analysis of heat exchangers with corrugated twisted tape inserts as shown in Table 2.

Table 2

Instruments used with accuracy and range

Sr. No.	Parameter	Measuring Instrument	Accuracy	Range
01	Temperature of Hot Fluid	Thermocouple	$\pm 0.5^{\circ}$ C	-50° C to 500° C
02	Temperature of Cold Fluid	Thermocouple	$\pm 0.5^{\circ}$ C	-50° C to 500° C
03	Flow Rate of Hot Fluid	Flow Meter	±1% of full scale	0.1 to 1000 m ³ /h
04	Flow Rate of Cold Fluid	Flow Meter	±1% of full scale	0.1 to 1000 m ³ /h
05	Electric Current	Energy Meter	±2%	0 to 100 kW

3. Data Reduction

The bulk mean temperature,

$$
T_{bh} = \frac{T_{h1} + T_{h2}}{2} \text{ and } T_{ch} = \frac{T_{c1} + T_{c2}}{2} \tag{1}
$$

Heat transfer for hot water and cold water

$$
Q_h = m_h C_{ph} (T_{h1} - T_{h2}) \text{ and } Q_c = m_c C_{pc} (T_{c1} - T_{c2})
$$
\n(2)

Table 3

Experimental Nusselt Number

$$
N_{ui} = \frac{h_i.d_i}{K} \tag{3}
$$

Experimental Friction Factor

$$
f = \frac{2g \, dih}{L U_i^2} \tag{4}
$$

4. Uncertainty Analysis

The Kline and McClintock's [28] method is used to estimate the uncertainty in their measurements. This method considers the errors associated with each instrument used to collect data. Table 3 shows the largest possible margins of error for the calculated Reynolds number (Re), Nusselt number (Nu), and friction factor (f). These uncertainties are based on the accuracies of the instruments used to measure the original data and the properties of the materials involved.

5. Results and Discussion

After analyzing the experiment data, we calculated Nusselt numbers and friction factors for both plain tubes and tubes with wavy inserts. We compared these results to established correlations: the Dittus-Boelter correlation for Nusselt number and the using Blasius's correlation for friction factor [29,30].

$$
N_{u} = 0.023 (R_e)^{0.8} \cdot (P_r)^{1/3}
$$
 (5)

$$
f = 0.0791 \, (\text{R}_e)^{-0.25} \tag{6}
$$

Figure 2 shows the relationship between Nusselt number and Reynolds number for the plain tube. The graph reveals a linear trend, indicating that Nusselt number is influenced by Reynolds number. It shows how the Nusselt number (indicating heat transfer rate) changes with Reynolds number (fluid flow rate) for twisted tapes with different twist ratios (TR). The results show that the Nusselt number increases as Reynolds number increases, which means a higher flow rate leads to a greater heat transfer rate. Interestingly, for a specific flow rate (Reynolds number), the twisted tape with the lowest twist ratio (TR=3.2) has the highest Nusselt number. In other words, the lowest twist ratio tape achieved the best heat transfer performance at that flow rate.

Fig. 2. Nusselt number vs Reynolds number

Figure 3 illustrates the friction factor versus Reynolds number for the plain tube. Here, we see an inverse relationship, meaning that friction factor decreases as Reynolds number increases. The graph shows how the friction factor changes with the flow rate (represented by Reynolds number) for different wavy twisted tape inserts. It reveals that friction factor increases as the twist ratio of the insert goes down. In other words, tapes with lower twist ratios create more friction. Specifically, the insert with the lowest twist ratio (3.2) has the highest friction factor, nearly two times greater than a plain tube. As the twist ratio increases (3.2, 4.2 and 5.2), the friction factor decreases, approaching values closer to a plain tube (1.98, 1.36 and 0.247 times that of a plain tube, respectively). These findings on heat transfer and heat transfer coefficients in a basic tubular heat exchanger are validate with those reported by Waware *et al.,* [31]. This comparison showed a close agreement, with a difference of less than 3% between the two studies, which helps to validate the current experiment's results.

6. Conclusion

Researchers and engineers can effectively leverage the benefits of wavy twisted tape inserts to enhance heat transfer in heat exchangers while addressing practical challenges related to friction factors and operational conditions. Future research should delve deeper into corrugated twisted tape inserts by exploring a wider range of geometries (corrugation pitch and height) and operating conditions to identify the optimal configuration for maximizing heat transfer. Additionally, investigating how these inserts synergize with other enhancement techniques like surface roughening or flow inducers could lead to even greater efficiency gains. Rigorous experiments are crucial to validate computational models and confirm real-world effectiveness. Finally, considering practicalities like ease of installation, maintenance, and long-term durability, alongside fostering collaboration between researchers, engineers, and industry, will accelerate the development of innovative heat transfer augmentation technologies through the combined expertise of diverse stakeholders.

Based on the experimental investigation, the following conclusions can be drawn

- i. Wavy (corrugated) twisted tape inserts significantly enhance heat transfer, particularly with a twist ratio of 3.2.
- ii. Compared to a plain tube, all tested wavy twisted tape inserts showed substantial heat transfer improvements.
- iii. Increasing the twist ratio further boosted heat transfer rates while reducing friction factors.
- iv. For Reynolds numbers between 4000 and 18000, Nusselt number increases were 77.75% for a twist ratio of 5.2, 167% for 4.2, and 185% for 3.2.
- v. The friction factor rose by approximately 10.42% for a twist ratio of 5.2, 32.54% for 4.2, and 36.33% for 3.2.

This design offers a substantial increase in heat transfer compared to plain tubes. While higher twist ratios further enhance heat transfer, also come with a slight increase in friction. Overall, these inserts provide a good balance between improved heat transfer and manageable friction factor.

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